

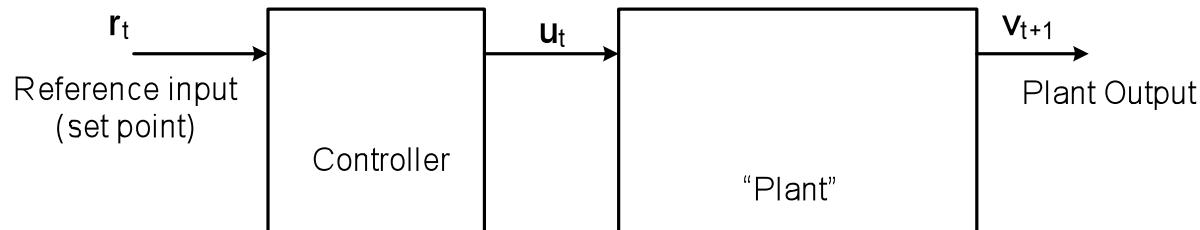
# Lecture 9 – Implementing PID Controllers

CSE P567

# Control Systems

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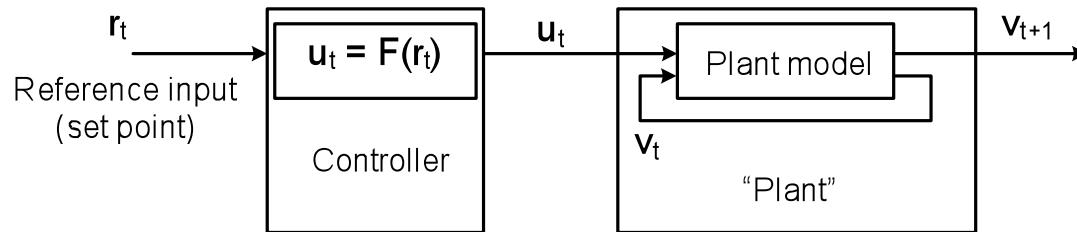
- ▶ We want to control some system
  - ▶ called a “Plant”
- ▶ There is an output value we want the system to achieve
- ▶ To be equal to a given goal value: set point
- ▶ Using a control input to the Plant



# Control Systems

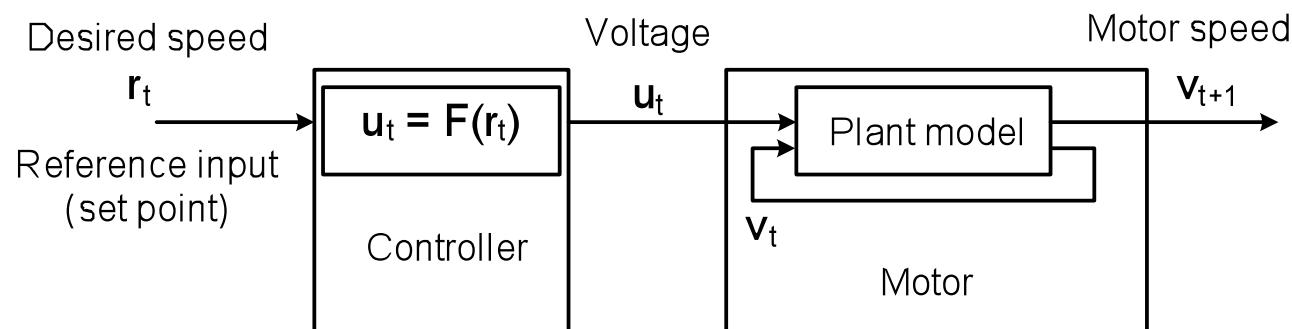
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- ▶ If we have a good model of the Plant
- ▶ We can predict the output from the input
- ▶ Andthus we can compute the input needed to achieve a given output
  - ▶  $u_t = F(r_t)$
- ▶ In this case we can use an Open Loop Controller



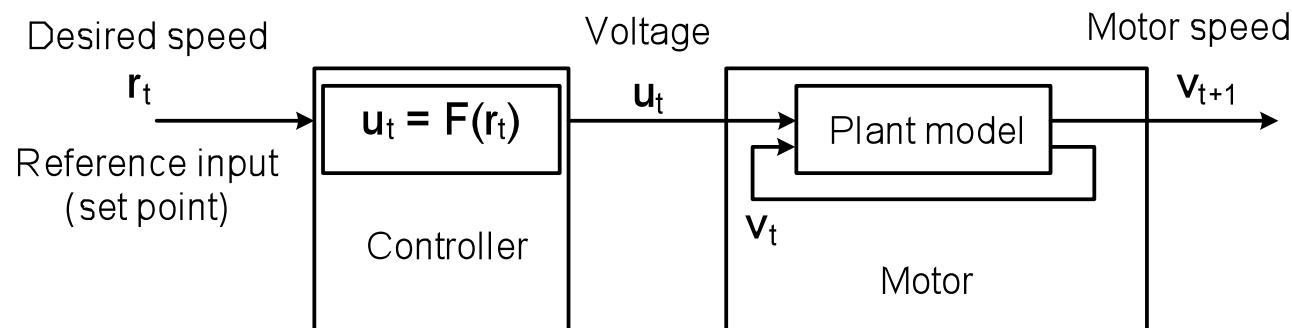
# Example Open Loop System

- ▶ Motor example
- ▶ Motor model:  $v_{t+1} = 0.7v_t + 0.5u_t + d_t$ 
  - ▶  $d_t$  is any disturbance in the plant
- ▶ Control:  $F(r_t) = P r_t$ 
  - ▶ Linear function



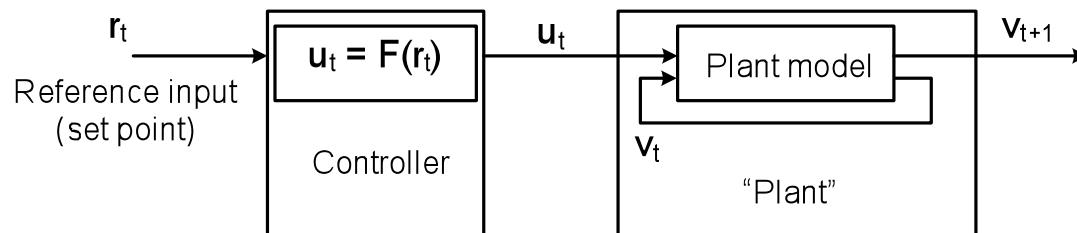
# Example Open Loop System

- ▶ Control:  $F(r_t) = P r_t$
- ▶ What should  $P$  be?
- ▶ In steady state:
  - ▶  $v_{ss} = 0.7v_{ss} + 0.5P r_t$
  - ▶  $0.3v_{ss} = 0.5P r_t$
  - ▶  $v_{ss} = 1.667P r_t$
  - ▶  $P = 0.6$  (steady state speed = set point)



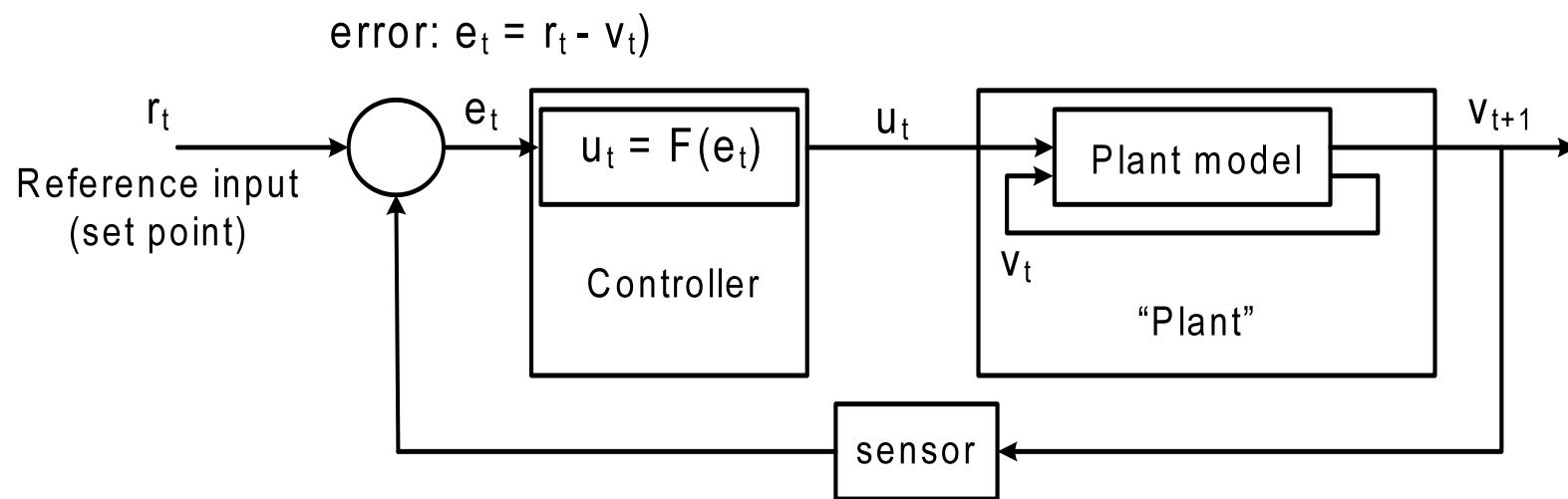
# Problems with Open Loop Systems

- ▶ They fly “blind”
  - ▶ Dead reckoning
- ▶ Cannot respond to disturbances
  - ▶ Extra friction/load, wearout, etc.
- ▶ Cannot adjust to different Plants (motors)
  - ▶ Each has its own model
- ▶ Models may be difficult or impossible to derive



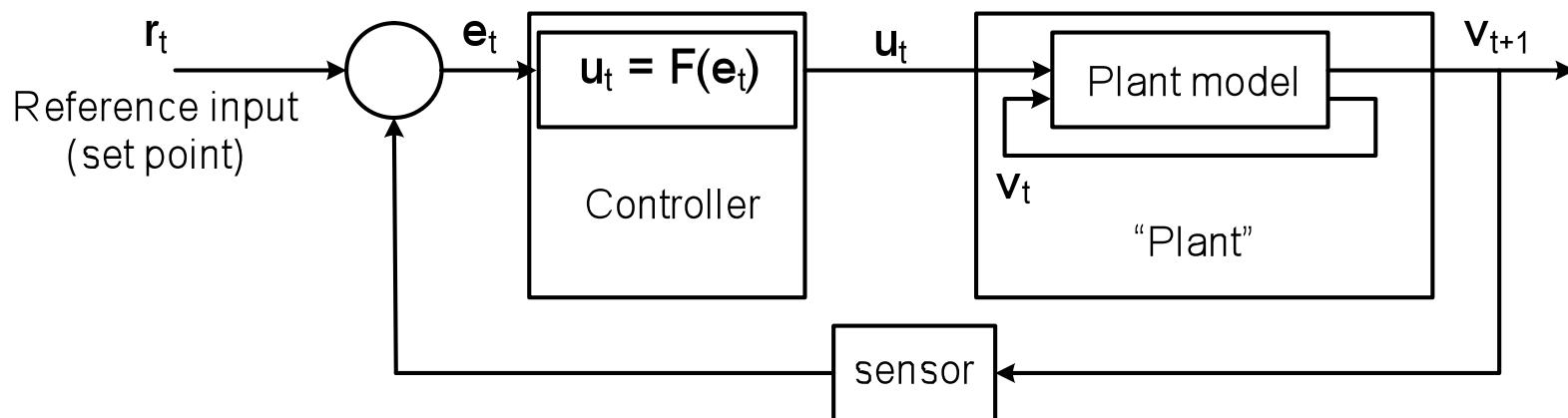
# Closed Loop Systems

- ▶ Add feedback so controller knows results of actions
- ▶ We now know the difference between the set point and the output
  - ▶ And we try to make this zero



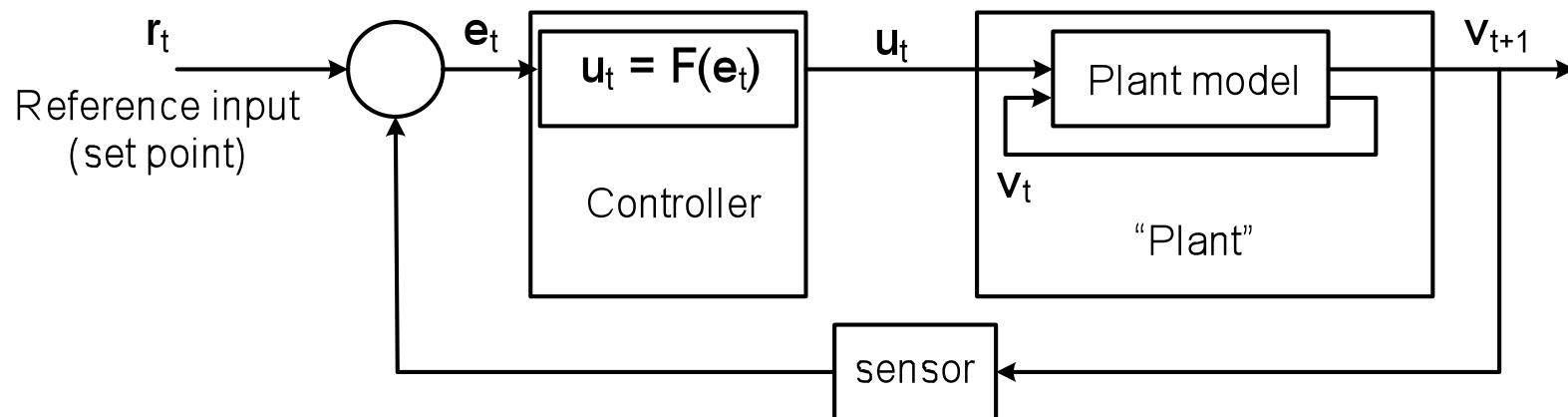
# Proportional Controller

- ▶ Simplest controller
- ▶  $F(e_t) = K_p(e_t)$
- ▶  $v_{t+1} = 0.7v_t + 0.5 K_p (r_t - v_t) + d_t$
- ▶  $v_{t+1} = (0.7 - 0.5 K_p) v_t + 0.5 K_p r_t + d_t$
- ▶  $\alpha = 0.7 - 0.5 K_p$  determines whether  $v$  stays within bounds
- ▶ if  $| \alpha | > 1$ , then  $v_t$  grows without bound



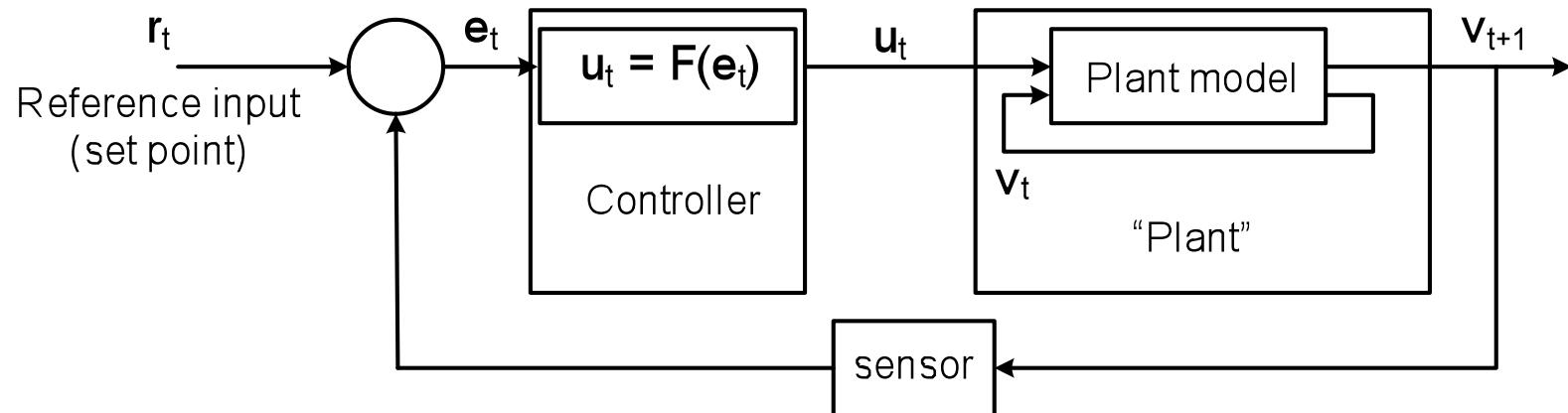
# Proportional Controller

- ▶  $| \alpha = 0.7 - 0.5 K_p | < 1$
- ▶  $K_p > -0.6$
- ▶  $K_p < 1.4$
- ▶ The best convergence rate is for  $K_p = 1.4$
- ▶ But for  $K_p \leq 1.4$ , we cannot reach the set point in steady state without oscillation



# Adding a Integral Term

- ▶ How do we solve the problem where the output never reaches the goal?
- ▶ If we sum the total error over time, the output must reach the set point
  - ▶ with some overcompensation
- ▶  $F(e_t) = K_p(e_t) + K_i(e_0 + e_1 + e_2 + \dots + e_{t-1})$
- ▶ The Integral term allows the output to reach goal



# Integral “Windup”

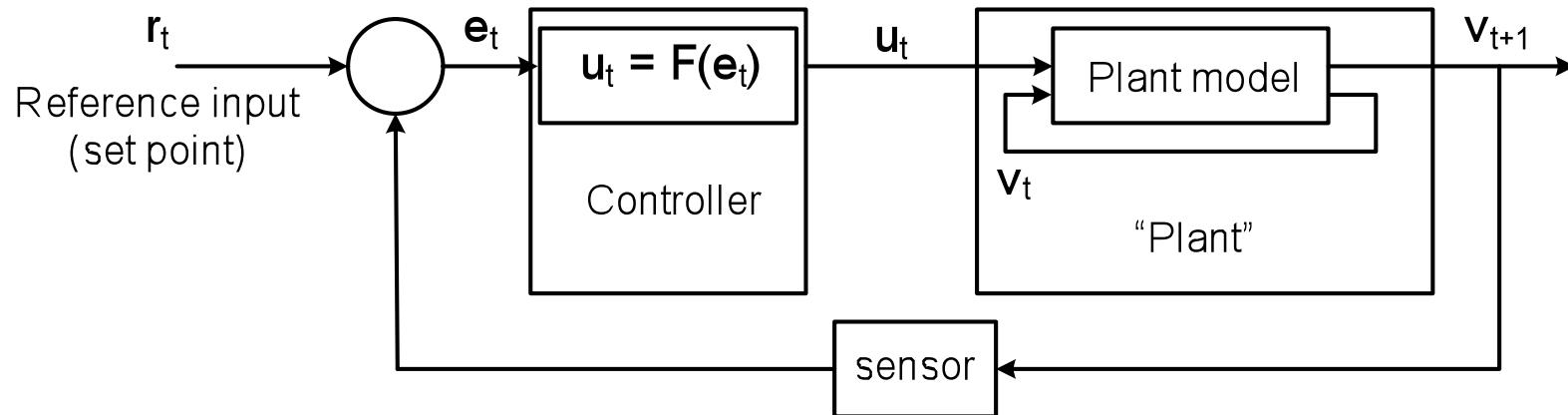
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- ▶ The integral term increases while the output is ramping up
- ▶ This causes overshoot
  - ▶ while the term “winds down”
- ▶ Can become oscillation
- ▶ Solution is to limit integral term
  - ▶ or cause it to die out
  - ▶  $I = 0.99I + e_t$



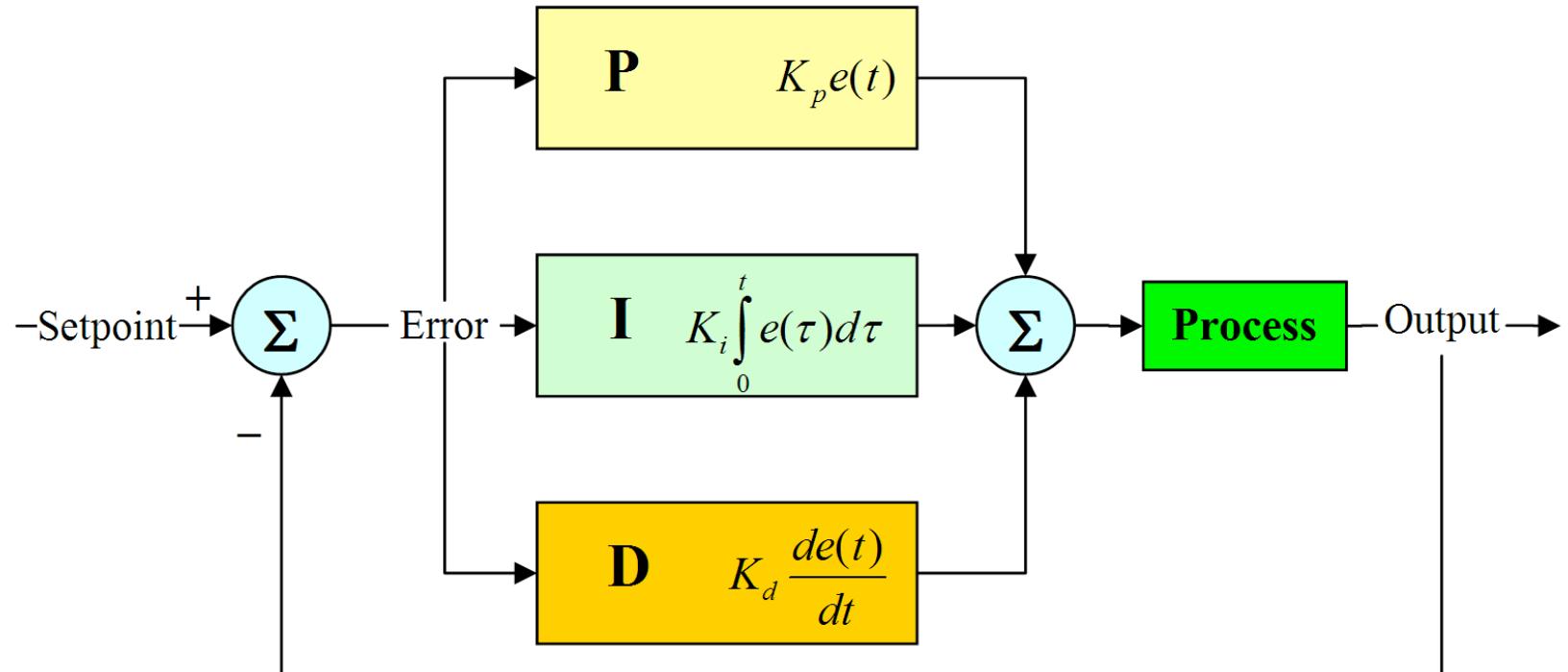
# Adding a Derivative Term

- ▶ We look at rate of change of output:
  - ▶ If too slow, increase the control input
  - ▶ If too fast, decrease the control input
- ▶  $F(e_t) = K_p(e_t) + K_D(e_t - e_{t-1})$
- ▶ The Derivative term decreases oscillation
  - ▶ especially caused by disturbances



# Summary of PID Controller

- ▶ We can build a PID controller that works well in practice in most situations without knowing control theory



# Controller Performance

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- ▶ Stability: The error variable should converge to a small number, preferably 0
  - ▶ i.e. little oscillation even with disturbances
- ▶ Performance:
  - ▶ Rise time/Response: e.g. 10% to 90% of final value
  - ▶ Peak time: Time to reach first peak
  - ▶ Overshoot: Amount in excess of final value
  - ▶ Settling time: Time before output settles to 1% of final value
- ▶ Disturbance rejection
- ▶ Robustness: Stability and performance should not be greatly compromised by small differences in plant or operating conditions



# Tuning a PID Controller

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- ▶ A search in 3 dimensions over all conditions
- ▶ If possible, use a large step function in the set point
  - ▶ e.g. 0 – 100%
- ▶ Heuristic procedure #1:
  - ▶ Set  $K_p$  to small value,  $K_D$  and  $K_I$  to 0
  - ▶ Increase  $K_D$  until oscillation, then decrease by factor of 2-4
  - ▶ Increase  $K_p$  until oscillation or overshoot, decrease by factor of 2-4
  - ▶ Increase  $K_I$  until oscillation or overshoot
  - ▶ Iterate



# Tuning a PID Controller

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- ▶ Heuristic procedure #2:
  - ▶ Set  $K_D$  and  $K_I$  to 0
  - ▶ Increase  $K_p$  until oscillation, then decrease by factor of 2-4
  - ▶ Increase  $K_I$  until loss of stability, then back off
  - ▶ Increase  $K_D$  to increase performance in response to disturbance
  - ▶ Iterate



# Tuning a PID Controller

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- ▶ Heuristic procedure #3:
  - ▶ Set  $K_D$  and  $K_I$  to 0
  - ▶ Increase  $K_p$  until oscillation:
    - ▶  $K_c = K_p, P_c = \text{period of oscillation}$
  - ▶ Set  $K_p = 0.5 K_c$
  - ▶ Set  $K_D = K_p P_c / 8$
  - ▶ Set  $K_I = 2K_p / P_c$



# Implementing a PID Controller

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- ▶ Can be done with analog components
- ▶ Microcontroller is much more flexible
- ▶ Pick a good sampling time:  $1/10$  to  $1/100$  of settling time
  - ▶ Should be relatively precise, within 1% – use a timer interrupt
  - ▶ Not too fast – variance in delta t
  - ▶ Not too slow – too much lag time
  - ▶ Sampling time changes relative effect of P, I and D
- ▶ Use interactive commands to set  $K_p$ ,  $K_i$ ,  $K_d$
- ▶ Possible to program an adaptive PID controller
  - ▶ Perform a careful, automatic search
  - ▶ Must be able to control Plant offline
  - ▶ Complex

