## Industrial Plastics, Inc.

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## MATERIAL DESCRIPTION

## POLYVINYLS

PVC (POLYVINYL CHLORIDE) has a relatively high tensile strength and modulus of elasticity and therefore is stronger and more rigid than most other thermoplastics. The maximum service temperature is $140^{\circ} \mathrm{F}$ for Type 1. PVC has excellent chemical resistance to a wide range of corrosive fluids, but may be damaged by ketones, aromatics, and some chlorinated hydrocarbons. It has proved an excellent material for process piping (liquids and slurries), water service, and industrial and laboratory chemical waste drainage. Joining methods are solvent welding, threading (Schedule 80 only), or flanging.

CPVC (CHLORINATED POLYVINYL CHLORIDE) is particularly useful for handling corrosive fluids at temperatures up to $210^{\circ} \mathrm{F}$. In chemical resistance, it is comparable to PVC. It weighs about one-sixth as much as copper, will not sustain combustion (self-extinguishing), and has low thermal conductivity. Suggested uses include process piping for hot, corrosive liquids; hot and cold water lines in office buildings and residences; and similar applications above the temperature range of PVC. CPVC pipe may be joined by solvent welding, threading, or flanging.

## POLYOLEFINS

POLYPROPYLENE (HOMOPOLYMER) is the lightest thermoplastic piping material, yet it has considerable strength, outstanding chemical resistance, and may be used at temperatures up to $180^{\circ} \mathrm{F}$ in drainage applications. Polypropylene is an excellent material for laboratory and industrial drainage piping where mixtures of acids, bases, and solvents are involved. It has found wide application in the petroleum industry where its resistance to sulfur-bearing compounds is particularly useful in salt water disposal line, chill water loops, and demineralized water. Joining methods are coil fusion and socket heat welding.

COPOLYMER POLYPROPYLENE is a copolymer of propylene and polybutylene. It is made of high molecular weight copolymer polypropylene and possesses excellent dielectric and insulating properties because of its structure as a nonpolar hydrocarbon polymer. It combines high chemical resistance with toughness and strength at operating temperatures from freezing to $200^{\circ} \mathrm{F}$. It has excellent abrasion resistance and good elasticity, and is joined by butt and socket fusion.

POLYETHYLENE, although its mechanical strength is comparatively low, polyethylene exhibits very good chemical resistance and is generally satisfactory when used at temperatures below $120^{\circ} \mathrm{F}$. Types I and II (low and medium density) polyethylene are used frequently in tanks, tubing, and piping. Polyethylene is excellent for abrasive slurries. It is generally joined by butt fusion.

## FLUOROPOLYMERS

PVDF (POLYVINYLIDENE FLUORIDE) is a strong, tough, and abrasion-resistant fluoroplastic material. It resists distortion and retains most of its strength to $280^{\circ} \mathrm{F}$. As well as being ideally suited to handle wet and dry chlorine,
bromine, and other halogens, it also withstands most acids, bases, and organic solvents. PVDF is not recommended for strong caustics. It is most widely recognized as the material of choice for high purity piping such as deionized water. PVDF is joined by thermal butt, socket, or electrofusion.

HALAR is a durable copolymer of ethylene and chlorofluoroethylene with excellent resistance to a wide variety of strong acids, chlorine, solvents, and aqueous caustics. Halar has excellent abrasion resistance, electric properties, low permeability, temperature capabilities from cryogenic to $340^{\circ} \mathrm{F}$, and radiation resistance. Halar has excellent application for high purity hydrogen peroxide and is joined by thermal butt fusion.

## TEFLON

There are three members of the Teflon family of resins. PTFE TEFLON is the original Teflon resin developed by DuPont in 1938. This fluoropolymer offers the most unique and useful characteristics of all plastic materials. Products made from this resin handle liquids or gases up to $500^{\circ} \mathrm{F}$. The unique properties of this resin prohibit extrusion or injection molding by conventional methods. When melted PTFE does not flow like other thermoplastics and it must be shaped initially by techniques similar to powder metallurgy. Normally PTFE is an opaque white material. Once sintered it is machined to the desired part.

FEP TEFLON was also invented by DuPont and became a commercial product in 1960. FEP is a true thermoplastic that can be melt-extruded and fabricated by conventional methods. This allows for more flexibility in manufacturing. The dielectric properties and chemical resistance are similar to other Teflons, but the temperature limits are $-65^{\circ} \mathrm{F}$ to a maximum of $300^{\circ} \mathrm{F}$. FEP has a glossy surface and is transparent in thin sections. It eventually becomes translucent as thickness increases. FEP Teflon is the most transparent of the three Teflons. It is widely used for its high ultraviolet light transmitting ability.

Caution: While the Teflon resin family has great mechanical properties and excellent temperature resistance, care must be taken when selecting the proper method of connections for your piping system. Generally, Teflon threaded connections will handle pressures to 120 PSIG. Loose ferrule connections are limited to 60 PSIG at ambient temperatures. Teflon loses it's ability to bear a load at elevated temperatures quicker than other thermoplastics. When working with the PTFE products shown in this catalog external ambient temperatures ranging from $-60^{\circ} \mathrm{F}$ to $250^{\circ} \mathrm{F}\left(-51^{\circ} \mathrm{C}\right.$ to $\left.121^{\circ} \mathrm{C}\right)$ may be handled safely. Fluid or gas temperatures inside the product should be limited to -60 to $400^{\circ} \mathrm{F}\left(-51^{\circ} \mathrm{C}\right.$ to $\left.204^{\circ} \mathrm{C}\right)$ unless otherwise noted. Always use extreme care when working with chemicals at elevated temperatures.

## MATERIAL DESCRIPTION

PFA TEFLON, a close cousin of PTFE, was introduced in 1972. It has excellent melt-processability and properties rivaling or exceeding those of PTFE Teflon. PFA permits conventional thermoplastic molding and extrusion processing at high rates and also has higher mechanical strength at elevated temperatures to $500^{\circ}$ F. Premium grade PFA Teflon offers superior stress and crack resistance with good flex-life in tubing. It is generally not as permeable as PTFE.

## DURAPLUS

ABS (ACRYLONITRILE-BUTADIENE-STYRENE)
There are many possibilities for polymer properties by combining these resins. For our purposes we will limit it to two products. One is the less expensive ABS resin used in drain, waste, and vent applications. The other resin for more stringent industrial applications has a different combination of the three polymers that make up the copolymer. The Duraplus product is made from this copolymer and has outstanding impact resistance even at low temperatures. The product is very tough and abrasion resistant. Temperature range is $40^{\circ} \mathrm{F}$ to $176^{\circ} \mathrm{F}$.

RYTON (PPS) POLYPHENYLENE SULFIDE remains quite stable during both long and short term exposure to high temperatures. The high tensile strength and flexural modulus typical of PPS compounds, decrease with an increase in temperature. PPS is also highly resistant to chemical attack. Relatively few chemicals react to this material even at high temperatures. Its broad range of chemical resistance is second only to that of Teflon (PTFE). Ryton is used primarily for precision pump parts.

## ELASTOMERS

VITON (FLUOROCARBON) is inherently compatible with a broad spectrum of chemicals. Because of this extensive chemical compatibility which spans considerable concentration and temperature ranges, Viton has gained wide acceptance as a sealing for valves, pumps, and instrumentation. Viton can be used in most applications involving mineral acids, salt solutions, chlorinated hydrocarbons, and petroleum oils.

EPDM (EPT) is a terpolymer elastomer made from ethylenepropylene diene monomer. EPDM has good abrasion and tear resistance and offers excellent chemical resistance to a variety of acids and alkalies. It is susceptible to attack by oils and is not recommended for applications involving petroleum oils, strong acids, or strong alkalies.

HYTREL is a multipurpose polyester elastomer similar to vulcanized thermoset rubber. Its chemical resistance is comparable to Neoprene, Buna-N and EPDM; however, it is a tougher material and does not require fabric reinforcement as do the other three materials. Temperature limits are $-10^{\circ} \mathrm{F}$ minimum to $190^{\circ} \mathrm{F}$ maximum. This material is used primarily for pump diaphragms.

## THERMOSETS

FIBERGLASS REINFORCED PLASTICS (FRP) including epoxy, polyester, and vinylester have become a highly valuable process engineering material for process piping.

FRP has been accepted by many industries because it offers the following significant advantages:
(a) moderate initial cost and low maintenance; (b) broad range of chemical resistance; (c) high strength-to-weight ratio; (d) ease of fabrication and flexibility of design; and (e) good electrical insulation properties.

EPOXY pipe and fittings have been used extensively by a wide variety of industries since 1960. It has good chemical resistance and excellent temperatures to pressure properties (to $300^{\circ} \mathrm{F}$ ). Epoxy has been used extensively for fuel piping and steam condensate return lines.

POLYESTER pipe and fittings have been used by the industry since 1963. It has a proven resistance to most strong acids and oxidizing materials. It can be used in applications up to $200^{\circ} \mathrm{F}$. Polyester is noted for its strength in both piping and structural shapes.

VINYLESTER resin systems are recommended for most chlorinated mixtures as well as caustic and oxidizing acids up to $200^{\circ} \mathrm{F}$. Vinylester for most service has superior chemical resistance to epoxy or polyester.

NYLONS are synthetic polymers that contain an amide group. Their key characteristics are: (a) excellent resistance and low permeation to fuels, oils, and organic solvent, including aliphatic, aromatic, and halogenated hydrocarbons, esters, and ketones; (b) outstanding resistance to fatigue and repeated impact; and (c) wide temperature range from $-30^{\circ} \mathrm{F}$ to $250^{\circ} \mathrm{F}$.

Caution: Acids will cause softening, loss of strength, rigidity, and eventual failure.

## POLYURETHANES

There are essentially two types of polyurethanes: polyester based and polyether based. Both are used for tubing applications.

POLYESTER based is the toughest of the two, having greater resistance to oil and chemicals. It does not harden when used with most oils, gasoline, and solvents. Polyurethane is extremely resistant to abrasives making it ideal for slurries, solids and granular material transfer. Temperature limit is $170^{\circ} \mathrm{F}$.

Caution: Polyester based polyurethanes may be subject to hydrolysis under certain conditions, high relative humidity at elevated temperatures, aerated water, fungi, and bacteria. Where these potentials exist, we recommend polyether-based polyurethane.

POLYETHER-based polyurethane possesses better low temperature properties, resilience and resistance to hydrolytic degradation than the polyester previously discussed.

## MATERIAL DESCRIPTION

Accelerated testing indicates that polyether-based polyurethanes have superior hydrolytic stability as compared to polyester based material. Made with no plasticizers and with a low level of extractables, polyether is ideal for high purity work. It will not contaminate laboratory samples and is totally non-toxic to cell cultures. Compared with PVC tubing, polyurethanes have superior chemical resistance to fuels, oils, and some solvents. Its excellent tensile strength and toughness make it suitable for full vacuums. This tubing can withstand temperatures from $-94^{\circ} \mathrm{F}$ to $200^{\circ} \mathrm{F}$.

## PTBP

Polybutylene terephthalate is a little known specialty material belonging to the polyimide group; It has excellent mechanical properties and good mechanical stress properties under corrosive environments. PTBP is used mainly for valve actuators, and bonnet assemblies.


## INDUSTRY STANDARDS

The standards referenced herein, like all other standards, are of necessity minimum requirements. It should be recognized that two different plastic resin materials of the same kind, type, and grade will not exhibit identical physical and chemical properties. Therefore, the plastic pipe purchaser is advised to obtain specific values or requirements from the resin supplier to assure the best application of the material not covered by industry specifications; this suggestion assumes paramount importance.

## ANSI

American National Standards Institute, Inc.
655 15th St. N.W.
300 Metropolitan Square
Washington, DC 20005
Phone (202) 639-4090

## ANSI PRESSURE CLASSES

ANSI Class 125 means 175 PSIG at $100^{\circ} \mathrm{F}$
ANSI Class 150 means 285 PSIG at $100^{\circ} \mathrm{F}$
ANSI Class 300 means 740 PSIG at $100^{\circ} \mathrm{F}$
ANSI A119.2-1963
ANSI B72.2-1967
ANSI B31.8-1968
ANSI Z21.30-1969
The following ASTM standards have been accepted by ANSI and assigned the following designations.

Table 1

| ANSI <br> Designation | ASTM <br> Designation | ANSI <br> Designation | ASTM Designation |
| :---: | :---: | :---: | :---: |
| B72.1 | D 2239 | B 72.11 | D 2412 |
| B72.2 | D 2241 | B 72.12 | D 2446 |
| B72.3 | D 2282 | B 72.13 | D 2447 |
| B72.4 | D 1503 | B 72.16 | D 2564 |
| B72.5 | D 1527 | B 72.17 | D 2657 |
| B72.6 | D 1598 | B 72.18 | D 2661 |
| B72.7 | D 1785 | B 72.19 | D 2662 |
| B72.8 | D 2104 | B 72.20 | D 2672 |
| B72.9 | D 2152 | B 72.22 | D 2740 |
| B72.10 | D 2153 | B 72.23 | D 2235 |

## ASTM

## American Society of Testing and Materials 1916 Race Street <br> Philadelphia, Pennsylvania 19103

Plastic Pipe Specifications:

| D | 1785 | Polyvinyl chloride (PVC) plastic pipe, <br> schedules 40, 80, and 120 <br> Chlorinated poly (vinyl chloride)(CPVC) <br> plastic pipe, schedules 40 and 80 |
| :--- | :--- | :--- |
| F | 441 | Polyvinyl chloride (PVC) plastic pipe |
| D | 2241 | (SD - PR) |
| D | 2513 | Thermoplastic gas pressure pipe, tubing <br> and fittings |
| D | 2665 | PVC plastic drain, waste, and vent pipe <br> and fittings |
| D | 2672 | Bell-ended PVC pipe |


| D | 2729 |
| :--- | :--- |
| D | 2846 |
| D | 2949 |
| D | 3034 |

PVC sewer pipe and fittings Chlorinated (CPVC) plastic hot water distribution system 3" thin wall PVC plastic drain, waste, and vent pipe and fittings Type PSM PVC sewer pipe and fittings

Plastic Pipe Fittings Specifications:

| D | 2464 | Threaded PVC plastic pipe fittings, <br> Schedule 80 |
| :--- | :--- | :--- |
| F | 437 | Threaded chlorinated polyvinyl chloride <br> (CPVC) plastic pipe fittings, Schedule 80 |
| D | 2466 | Socket-type PVC plastic type fittings, |
| D | 2467 | Schedule 40 <br> Socket-type PVC plastic type fittings, <br> Schedule 80 |
| F | 439 | Socket-type chlorinated polyvinyl <br> chloride (CPVC) plastic pipe fittings |
| D | 3036 | Schedule 80 <br> PVC plastic pipe lined couplings, socket <br> type |

Plastic Pipe Solvent Cement Specifications
D $2564 \quad$ Solvent cements for PVC plastic pipe and fittings
F $493 \quad$ CPVC solvent cement
Plastic Lined Steel Piping Specifications:
ASTM A-587 Standard specification for electric-welded low carbon steel pipe for the chemical industry

ASTM A-53

ASTM A-105

ASTM A-125 Standard specification for steel springs, helical, heat-treated

ASTM A-126

ASTM A-395

ASTM A-216

ASTM A-234

ANSI B-16.1 Cast iron pipe flanges and flanged fittings Class 25, 125, 150, 250 and 800

ANSI B-16.42 Ductile iron pipe flanges and flanged fittings Class 150 and 300

## INDUSTRY STANDARDS



ANSI B-16.5 Steel pipe flanges and flanged fittings Class 150, 300, 400, 600, 900, 1500 and Standard specification for electric-welded low carbon steel pipe for the chemical industry

Standard specification for pipe, steel black and hot-dipped, zinc-coated, welded and Standard specification for forgings, carsteel, for piping components

Standard specification for steel springs, helical, heat-treated

Standard specification for gray iron cast-

Standard specification for ferritic ductile iron pressure retaining castings for use at elevated temperatures

Standard specification for carbon steel castings suitable for fusion welding for high temperature service

## Methods of Test Specifications:

D 256 Test for impact resistance of plastics and electrical insulating materials reagents
$\begin{array}{lll}\text { D } & 570 & \text { Test for water absorption of plastics } \\ \text { D } & 618 & \text { Conditioning plastics and electrical insul- }\end{array}$ ating materials for testing load

Test for flammability of self-supporting plastics

Test for tensile properties of plastics
Test for deflection temperature of plastics under load

Tests for repeated flexural stress of plastics

Test for flammability of plastics, selfextinguishing type

Test for flexural properties of plastics
Nomenclature relating to plastics

D 1180
Test for bursting strength of round, rigid plastic tubing

D 1598
Test for time to failure of plastic pipe under long-term hydrostatic pressure

Test for short-time rupture strength of plastic pipe, tubing and fittings

D 2122 Determining dimensions of thermoplastic pipe and fittings

D 2152
Test for quality of extruded PVC pipe by acetone immersion

Test for external loading properties of plastic pipe by parallel-plate loading

D 2444
Test for impact resistance of thermoplastic pipe and fittings by means of a tup (falling weight)

D 2837
Obtaining hydrostatic design basis thermoplastic pipe materials

Test for external pressure resistance of plastic pipe

## RECOMMENDED PRACTICES

D $2153 \quad$ Calculating stress in plastic pipe under internal pressure

D 2321 Underground installation of flexible thermoplastic sewer pipe

D 2657 Heat joining of thermoplastic pipe and fittings

D 2749 Standard definitions of terms relating to plastic pipe fittings

D 2774 Underground installation of thermoplastic pressure pipe

D 2855 Making solvent cemented joints with PVC pipe and fittings

## ASTM STANDARDS FOR PLASTIC MATERIALS REFERENCED IN PLASTIC PIPE, FITTINGS, AND CEMENT STANDARDS

D 1784 PVC compounds and CPVC compounds
BOCA

## Building Officials Conference of America <br> 1313 East 60th Street Chicago, Illinois 60637

BOCA Basic Plumbing Code

Table 2

| Group | Commercial Standard <br> or Product Standard | ASTM Standard or <br> Tentative Specification |
| :---: | :---: | :---: |
| A | PS10 | D2104 |
| B | PS11 | D2238 |
| C | PS12 | D2447 |
| D | PS18 | D1527 |
| E | PS19 | D2282 |
| F | PS21 | D1785 |
| G | PS22 | D2241 |
| H | CS228 | D2852 |
| I | CS270 | D2661 |
| J | CS272 | D2665 |

## COMMERCIAL AND PRODUCT STANDARDS

## Supt. of Documents

U.S. Government Printing Office

Washington, DC 20402

CS 272
PVC-DWV pipe and fittings
PS 21 PVC plastic pipe (Schedules 40, 80, 120) supersedes CS 207-60

PS 22
PVC plastic pipe (SDR) supersedes CS 256

CSA
Canadian Standards Association
178 Rexdale Boulevard
Rexdale, Ontario, Canada
B $\quad 137.0 \quad$ Defines general requirements and methods of testing for thermoplastic pressure pipe
B $\quad 137.3$ Rigid polyvinyl chloride (PVC) pipe for pressure applications
B $\quad$ 137.4 Thermoplastic piping systems for gas service

B $\quad 137.14$ Recommended practice for the installation of thermoplastic piping for gas service

B $\quad 181.2$ Polyvinyl chloride drain, waste, and vent pipe and pipe fittings
B $\quad 181.12$ Recommended practice for the installation of PVC drain, waste, and vent pipe fittings

B $\quad 182.1 \quad$ Plastic drain and sewer pipe and pipe fittings for use underground

B
182.11 Recommended practice for the installation of plastic drain and sewer pipe and pipe fittings

DEPARTMENT OF AGRICULTURE
U.S. Department of Agriculture

Soil Conservation Service
Washington, DC 20250
SCS National Engineering Handbook, Section 2, Part 1, Engineering Practice Standards

SCS432-D
High pressure underground plastic irrigation pipelines

SCS432-E Low head underground plastic irrigation pipelines

## DEPARTMENT OF DEFENSE MILITARY STANDARDS Commanding Officer <br> Naval Publications and Forms Center <br> 5108 Tabor Avenue <br> Philadelphia, Pennsylvania 19120

MIL-A-22010A(1) Adhesive solvent-type, polyvinyl chloride amendment

MIL-C-23571A(YD) Conduit and conduit fittings, plastic, rigid
MIL-P-14529B Pipe, extruded, thermoplastic
MIL-P-19119B(1) Pipe, plastic, rigid, unplasticized, high impact, polyvinyl chloride

MIL-P-22011A
Pipe fittings, plastic, rigid, high impact, polyvinyl chloride, (PVC) and poly 1, 2 dichlorethylene

MIL-P-28584A

MIL-P-29206
Pipe and pipe fittings, glass fiber reinforced plastic for condensate return lines

Pipe and pipe fittings glass fiber reinforced plastic for liquid petroleum lines

## DOT - OTS

Department of Transportation, Hazardous Materials Regulation Board, Office of Pipeline Safety, Title 49, Docket OPS-3 and amendments, Part 192. Transportation of Natural Gas and Other Gas by Pipeline: Minimum Federal Safety Standards, Federal Register, Vol, 35, No. 161, Wednesday, August 19, 1980. Amendments to date are 1921, Vol. 35, No. 205, Wednesday, October 21, 1970; 19-2, Vol. 35, No. 220, Wednesday, November 11, 1970; and 192-3, Vol. 35, No. 223, Tuesday, November 17, 1970.

## FEDERAL SPECIFICATIONS

## Specifications Activity

Printed Materials Supply Division Building 197, Naval Weapons Plant Washington, DC 20407

L-P-320a

L-P-1036(1)

Pipe and fittings, plastic (PVC, drain, waste, and vent)

Plastic rod, solid, plastic tubes and tubing, heavy walled; polyvinyl chloride

## INDUSTRY STANDARDS

## FHA <br> Architectural Standards Division Federal Housing Administration <br> Washington, DC 20412

FHA UM-41 PVC plastic pipe and fittings for domestic water service

FHA UM-49 ABS and PVC plastic drainage and vent pipe and fittings, FHA 4550.49

FHA UM-53a Polyvinyl chloride plastic drainage, waste and vent pipe and fittings

FHA MR-562 Rigid chlorinated polyvinyl chloride (CPVC) hi/temp water pipe and fittings

FHA MR-563 PVC plastic drainage and vent pipe and fittings

FHA Minimum Property standards interim revision No. 31
IAPMO
International Association of Plumbing and
Mechanical Officials
5032 Alhambra Avenue
Los Angeles, California 90032
Uniform Plumbing Code
IAPMO IS8 Solvent cemented PVC pipe for water service and yard piping

IAPMO IS9 PVC drain, waste, and vent pipe and fittings

IAPMO IS10 Polyvinyl chloride (PVC) natural gas yard piping

IAPMO PS27 Supplemental standard to ASTM D2665; polyvinyl chloride (PVC) plastic drain, waste, and vent pipe and fittings
(NOTE: IS = installation standard; PS = property standard)
NSF
National Sanitation Foundation
School of Public Health
University of Michigan
Ann Arbor, Michigan 48106
NSF
Standard No. 14: Thermoplastic Materials, Pipe, Fittings, Valves, Traps, and Joining Materials

NSF
Seal of Approval: Listing of Plastic Materials, Pipe, Fittings, and Appurtenances for Potable Water and Waste Water (NSF Testing Laboratory).

NSPI
National Swimming Pool Institute
2000 K Street, N.W.
Washington, DC 20006
T.R.-19 The Role of Corrosion-Resistant Materials in Swimming Pools, Part D, The Role of Plastics in Swimming Pools.

PHCC
National Association of Plumbing-Heating-Cooling Contractors
1016 20th Street, N.W.
Washington, DC 20036
National Standard Plumbing Code

## SBCC

Southern Building Code Congress
1166 Brown-Marx Building
Birmingham, Alabama 35203
SBCC Southern Standard Plumbing Code
SIA
Sprinkler Irrigation Association
1028 Connecticut Avenue, N.W.
Washington, DC 20036
Minimum Standards for Irrigation Equipment

## WUC

Western Underground Committee, W.H. Foote
Los Angeles Department of Water and Power
P.O. Box 111

Los Angeles, California 90054
Interim Specification 3.1: Plastic Conduit and Fittings
UL
Underwriters Laboratories, Inc.
207 East Ohio Street
Chicago, Illinois 60611
UL 651 Rigid Nonmetallic Conduit (September 1968)
UL 514 Outlet Boxes and Fittings (March 1951 with Amendments of 22-228-67)


## INDUSTRY STANDARDS

NEMA
National Electrical Manufacturers' Association 2101 "L" St. N.W.
Washington, DC 20037
Type 1 General Purpose - Indoor: This enclosure is intended for use indoors, primarily to prevent accidental contact of personnel with the enclosed equipment in areas where unusual service conditions do not exist. In addition, they provide protection against falling dirt.

Type 2 Dripproof - Indoor: Type 2 dripproof enclosures are for use indoors to protect the enclosed equipment against falling noncorrosive liquids and dirt. These enclosures are suitable for applications where condensation may be severe such as encountered in cooling rooms and laundries.

Type 3 Dusttight, Raintight, Sleet (Ice) Resistant Outdoor: Type 3 enclosures are intended for use outdoors to protect the enclosed equipment against windblown dust and water. They are not sleet (ice) proof.

Type 3R Rainproof and Sleet (Ice) Resistant Outdoor: Type 3R enclosures are intended for use outdoors to protect the enclosed equipment against rain and meet the requirements of Underwriters Laboratories Inc., Publication No. UL 508, applying to "Rainproof Enclosures." They are not dust, snow, or sleet (ice) proof.

Type 3S Dusttight, Raintight, and Sleet (Ice) ProofOutdoor: Type 3S enclosures are intended for use outdoors to protect the enclosed equipment against windblown dust and water and to provide for its operation when the enclosure is covered by external ice or sleet. These enclosures do not protect the enclosed equipment against malfunction resulting from internal icing.

Type 4 Watertight and Dusttight - Indoor and Outdoor: This type is for use indoors or outdoors to protect the enclosed equipment against splashing and seepage of water or streams of water from any direction. It is sleet-resistant but not sleetproof.

Type 4 X Watertight, Dusttight and CorrosionResistant - Indoor and Outdoor: This type has same provisions as Type 4 and, in addition, is corrosion-resistant.

Type 5

Type 6

Type 7
Class I, Group A, B, C, and D-Indoor Hazardous Locations - Air-Break Equipment: Type 7 enclosures are intended for use indoors, in the atmospheres and locations defined as Class 1 and Group A, B, C or D in the National Electrical Code. Enclosures must be designed as specified in Underwriters' Laboratories, Inc. "Industrial Control Equipment for Use in Hazardous locations," UL 698. Class I locations are those in which flammable gases or vapors may be present in explosive or ignitable amounts. The group letters A, $B, C$, and $D$ designate the content of the hazardous atmosphere under Class 1 as follows:

Group A
Atmospheres containing acetylene.
Group B
Atmospheres containing hydrogen or gases or vapors of equivalent hazards such as manufactured gas.

Group C
Atmospheres containing ethyl ether vapors, ethylene, or cyclopropane.

Group D
Atmospheres containing gasoline, hexane, naphtha, benzene, butane, propane, alcohols, acetone, lacquer solvent vapors and natural gas.

## INDUSTRY STANDARDS

Type 8
Class I, Group A, B, C or D - Indoor Hazardous Locations Oil-immersed Equipment: These enclosures are intended for indoor use under the same class and group designations as Type 7, but are also subject to immersion in oil.

Type 9 Class II, Group E, F and G - Indoor Hazardous Locations - Air-Break Equipment: Type 9 enclosures are intended for use indoors in the atmospheres defined as Class II and Group E, F, or G in the National Electrical Code. These enclosures shall prevent the ingress of explosive amounts of hazardous dust. If gaskets are used, they shall be mechanically attached and of a non-combustible, nondeteriorating, verminproof material. These enclosures shall be designed in accordance with the requirements of Underwriters' Laboratories, Inc. Publication No. UL 698. Class II locations are those in which combustible dust may be present in explosive or ignitable amounts. The group letter E,F, and G designate the content of the hazardous atmosphere as follows:

Group E
Atmosphere containing metal dusts, including aluminum, magnesium, and their commercial alloys.

Group F
Atmospheres containing carbon black, coal, or coke dust.

Group G
Atmospheres containing flour, starch, and grain dust.

Type $10 \quad$ Bureau of Mines: Enclosures under Type 10 must meet requirements of Schedule 2G (1968) of the Bureau of Mines, U.S. Department of the Interior, for equipment to be used in mines with atmospheres containing methane or natural gas, with or without coal dust.

Type 11 Corrosion-Resistant and Dripproof-OilImmersed - Indoor: Type 11 enclosures are corrosion-resistant and are intended for use indoors to protect the enclosed equipment against dripping, seepage, and external condensation of corrosive liquids. In addition, they protect the enclosed equipment against the corrosive effects of fumes and gases by providing for immersion of the equipment in oil.
Type 12 Industrial Use - Dusttight and Driptight Indoor: Type 12 enclosures are intended for use indoors to protect the enclosed equipment against fibers, flyings, lint, dust and dirt, and light splashing, seepage, dripping and external condensation of non-corrosive liquids.

Type 13
Oiltight and Dusttight - Indoor: Type 13 enclosures are intended for use indoors primarily to house pilot devices such as limit switches, foot switches, pushbuttons, selector switches, pilot lights, etc., and to protect these devices against lint and dust, seepage, external condensation, and spraying of water, oil or coolant. They have oil-resistant gaskets.

## HAZARDOUS (CLASSIFIED) LOCATIONS IN ACCORDANCE WITH FACTORY MUTUAL ENGINEERING CORP.

The National Electrical Code and the Canadian Electrical Code divide hazardous locations into three "classes" according to the nature of the hazard: Class I, Class II, and Class III. The locations in each of these classes are further divided by "divisions" according to the degree of the hazard.

Class I, Division 1 locations are those in which flammable gases or vapors are or may be present in sufficient quantities to produce an ignitable mixture (continuously, intermittently, or periodically).

Class I, Division 2 locations are those in which hazardous mixtures may frequently exist due to leakage or maintenance repair.

Class I, Division 3 are those in which the breakdown of equipment may release concentration of flammable gases or vapors which could cause simultaneous failure of electrical equipment.

For purposes of testing, classification and approval of electrical equipment atmospheric mixtures are classified in seven groups (A through G) depending on the kind of material involved.

Class II locations are classified as hazardous because of the presence of combustible dusts.

Class III locations are hazardous because of the presence of combustible fibers or flyings in textile processes.

There are similar divisions and groups for Class II and Class III as those described for Class I. For specifics or further details contact Harrington's Technical Services department.

## INDUSTRY STANDARDS

HAZARDOUS MATERIAL SIGNALS

Hazardous Material Signals based on the National Fire Protection Association Code number 704M and Federal Standard 313. This system provides for identification of hazards to employees and to outside emergency personnel. The numerical and symboled system shown here are the
standards used for the purpose of safeguarding the lives of those who are concerned with fires occurring in an industrial plant or storage location where the fire hazards of material may not be readily apparent.


Figure 1. For use where specified color background is used with numerals of contrasting colors.

FLAMMABILITY


Figure 2. For use where a white background is necessary.

WHITE PAINTED BACKGROUND, WHITE PAPER OR CARD STOCK


Figure 3. For use where a white background is used with painted numerals, or for use when the signal is in the form of sign or placard.

## Table 4 - ARRANGEMENT AND

ORDER OF SIGNALS - OPTIONAL
FORM OF APPLICATION

| DISTANCE AT <br> WHICH SIGNALS <br> MUST BE LEGIBLE | MINIMUM SIZE <br> OF SIGNALS <br> REQUIRED |
| :---: | :---: |
| 50 FEET | $1 "$ |
| 75 FEET | $2 "$ |
| 100 FEET | $3 "$ |
| 200 FEET | $4 "$ |
| 300 FEET | $6 "$ |

## NOTE:

This shows the correct spatial arrangement and order of signals used for identification of materials by hazard.


Figure 4. Storage Tank

This is a system for the identification of hazards to life and health of people in the prevention and control of fires and explosions in the manufacture and storage of materials.

The basis for identification are the physical properties and characteristics of materials that are known or can be determined by standard methods. Technical terms, expressions, trade names, etc., are purposely avoided as this system is concerned only with the identification of the involved hazard from the standpoint of safety.

The explanatory material on this page is to assist users of these standards, particularly the person who assigns the degree of hazard in each category.

## Table 5 IDENTIFICATION OF THE FIRE AND HEALTH HAZARDS OF MATERIALS

| IDENTIFICATION OF HEALTH HAZARDS COLOR CODE: BLUE |  | identification of flammability COLOR CODE: RED |  | IDENTIFICATION OF REACTIVITY COLOR CODE: YELLOW |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
| SIGNAL | TYPE OF POSSIBLE INJURY | SIGNAL | SUSCEPTIBILITY OF MATERIALS TO BURNING | SIGNAL | SUSCEPTIBILITY TO RELEASE OF ENERGY |
| $4$ | Materials which on very short exposure could cause death or major residual injury even though prompt medical treatment were given. | $4$ | Materials which will rapidly or completely vaporize at atmospheric pressure and normal ambient temperature, or which are readily dispersed in air and which will burn readily. | $4$ | Materials which in themselves are readily capable of detonation or of explosive decomposition or reaction at normal temperatures and pressures. |
| 3 | Materials which on short exposure could cause serious, temporary or residual injury even though prompt medical treatment were given. | $3$ | Liquids and solids that can be ignited under almost all ambient temperature conditions. | $3$ | Materials which in themselves are capable of detonation or of explosive reaction but require a strong initiating source or which must be heated under confinement before initiation or which react explosively with water. |
| $2$ | Material which on intense or continued exposure could cause temporary incapacitation or possible residual injury unless prompt medical treatment is given. | $2$ | Materials that must be moderately heated or exposed to relatively high ambient temperatures before ignition can occur. | $2$ | Materials which in themselves are normally unstable and readily undergo violent chemical change but do not detonate. Also materials which may react violently with water or which may form potentially explosive mixtures with water. |
| 1 | Materials which on exposure would cause irritation but only minor residual injury, even if no treatment is given. |  | Materials that must be preheated before ignition can occur. | $1$ | Materials which, in themselves, are normally stable, but which can become unstable at elevated temperatures and pressures or which may react with water with some release of energy but not violently. |
|  | Materials which on exposure under fire conditions would offer no hazard beyond that of ordinary combustible material. | $0$ | Materials that will not burn. | $0$ | Materials, which in themselves are normally stable, even under fire exposure conditions, and which are not reactive with water. |



# INDUSTRY STANDARDS <br> Government regulatory agencies 

## DEPARTMENT OF COMMERCE

National Institute
of Standards and Technology
Public and Business Affairs Div.
Building 101, Room A903
Gaithersburg, MD 20889
Ph\#: 301/975-2762
Fax: 301/926-1630
The National Institute of Standards and Technology (NIST) focuses on tasks vital to the country's technology infrastructure that neither industry nor the government can do separately.

NIST works to promote U.S. economic growth by working with industry to develop and apply technology, measurements, and standards.

Part of the Commerce Department's Technology Administration, NIST has four major programs that reflect U.S. industry's diversity and multiple needs. These programs include the Advanced Technology Program; Manufacturing Extension Partnership; Laboratory Research and Services; and the Baldrige National Quality Program.

## DEPARTMENT OF ENERGY

Consumer Affairs
1000 Independence Avenue SW
Washington, DC 20585
Ph\#: 202/586-5373
Fax: 202/586-0539
The Department of Energy is entrusted to contribute to the welfare of the nation by providing the technical information and scientific and educational foundation for technology, policy, and institutional leadership necessary to achieve efficiency in energy used, diversity in energy sources, a more productive and competitive economy, improved environmental quality, and a secure national defense.

## DEPARTMENT OF THE INTERIOR

1849 C Street NW
Washington, DC 20240
Ph\#: 202/208-3100
Fax: 202/208-6950
As the nation's principal conservation agency, the Department of the Interior's responsibilities include: encouraging and providing appropriate management, preservation and operation of the nation's public lands and natural resources; developing and using resources in an environmentally sound manner; carrying out related scientific research and investigations in support of these objectives; and carrying out trust responsibilities of the U.S. government with respect to American Indians and Alaska Natives.

It manages more than 440 million acres of federal lands.

## DEPARTMENT OF LABOR

Office of Information and Public Affairs
200 Constitution Avenue, NW
Washington, DC 20210
Ph\#: 202/219-7316
Fax: 202/219-8699
The Department of Labor's principal mission is to help working people and those seeking work.

The department's information and other services, particularly in job training and labor law enforcement, benefit and affect many other groups, including employers, business organizations, civil rights groups and government agencies at all levels as well as the academic community.

## DEPARTMENT OF TRANSPORTATION

Office of Public Affairs
400 Seventh Street SW, Room 10414
Washington, DC 20590
Ph\#: 202/366-4570
Fax: 202/366-6337
The Department of Transportation ensures the safety of all forms of transportation; protects the interests of consumers; conducts planning and research for the future; and helps cities and states meet their local transportation needs.

The Department of Transportation Is composed of 10 operating administrations, including the Federal Aviation Administration; the Federal Highway Administration; the Federal Railroad Administration; the Federal Transit Administration; the National Highway Traffic Safety Administration; the Maritime Administration; the St. Lawrence Seaway Development Corp.; the U.S. Coast Guard; the Research and Special Programs Administration; and the Bureau of Transportation Statistics.

## DEPARTMENT OF THE <br> TREASURY

Bureau of Alcohol, Tobacco and
Firearms
Liaison and Public Information
650 Massachusetts Avenue NW
Room 8290
Washington, DC 20226
Ph\#: 202/927-8500
Fax: 202/927-8112
The Bureau of Alcohol, Tobacco and Firearms (ATF) is an agency of the U.S. Department of the Treasury.

ATF's responsibilities are law enforcement; regulation of the alcohol, tobacco, firearms and explosives industries; and ensuring the collection of taxes on alcohol, tobacco, and firearms.

ATF's mission is to curb the illegal traffic in and criminal use of firearms; to assist federal, state and local law enforcement agencies in reducing crime and violence; to investigate violations of federal explosive laws; to regulate the alcohol, tobacco, firearms and explosives industries; to assure the collection of all alcohol, tobacco and firearm tax revenues; and to suppress commercial bribery, consumer deception, and other prohibited trade practices in the alcoholic beverage industry.

## ENVIRONMENTAL PROTECTION <br> AGENCY

Communication, Education and Public Affairs
401 M Street SW
Washington, DC 20460
Ph\#: 202/260-2090 Public Information Center
Mail Code 3404
Ph\#: 202/260-2080
Fax: 202/260-6257
Chemical Control
401 M St. SW
Washington DC 20460
Ph\#: 202/260-3749
Fax: 202/260-8168
Chemical Emergency Preparedness and Prevention 401 M St.
SW Washington, DC 20460 Ph\#: 202/ 260-8600 Fax: 202/260-7906
The Environmental Protection Agency (EPA) is an independent agency in the executive branch of the U.S. government. EPA controls pollution through a variety of activities, which includes research, monitoring, standards setting, and enforcement.

The Environmental Protection Agency supports research and antipollution efforts by state and local governments as well as by public service institutions and universities.

# INDUSTRY STANDARDS <br> Government regulatory agencies 

FEDERAL AVIATION
ADMINISTRATION
800 Independence Avenue, SW
Washington, DC 20591
Ph\#: 800/FAA-SURE
FAA Consumer Hotline
The Federal Aviation Administration (FAA) provides a safe, secure and efficient global aerospace system that contributes to national security and the promotion of U.S. aerospace.

As the leading authority in the international aerospace community, FAA is responsive to the dynamic nature of customer needs, economic conditions and environmental concerns.

FOOD AND DRUG ADMINISTRATION Office of Public Affairs Public Health Service Department of Health \& Human Services 5600 Fishers Lane (HFI-40)
Rockville, MD 20857
Ph\#: 301/443-3170
Consumer Affairs
The Food and Drug Administration (FDA) works to protect, promote, and enhance the health of the American people by ensuring that foods are safe, wholesome, and sanitary; human and veterinary drugs, biological products and medical devices are safe and effective; cosmetics are safe; electronic products that emit radiation are safe; regulated products are honestly, accurately, and informatively represented; these products are in compliance with the law and the FDA regulations; and non-compliance is identified and corrected and any unsafe and unlawful products are removed from the marketplace.

## NATIONAL AERONAUTICS

AND SPACE ADMINISTRATION
300 E Street SW
Washington, DC 20546
Ph\#: 202/358-0000
Fax: 202/358-3251
The National Aeronautics and Space Administration explores, uses and enables the development of space for human enterprise; advances scientific knowledge and understanding of the Earth, the solar system and universe; uses the environment of space for research; and researches, develops, verifies and transfers advanced aeronautics, space and related technologies.

## NATIONAL INSTITUTE FOR

OCCUPATIONAL SAFETY

## AND HEALTH

Public Affairs
200 Independence Avenue SW
Washington, DC 20201
Ph\#: 202/260-8519
Fax: 202/260-1898
The National Institute for Occupational Safety and Health (NIOSH) was established by the Occupational Safety and Health Act of 1970. NIOSH is part of the Centers for Disease Control and Prevention and is the federal institute responsible for conducting research and making recommendations for the prevention of work-related illnesses and injuries.

The Institute's responsibilities include: investigating potentially hazardous working conditions as requested by employers or employees; evaluating hazards in the workplace; creating and disseminating methods for preventing disease, injury, and disability; conducting research and providing scientifically valid recommendations for protecting workers; and providing education and training to individuals preparing for or actively working in the field of occupational safety and health.

NIOSH identifies the causes of work related diseases and injuries and the potential hazards of new work technologies and practices. It determines new ways to protect workers from chemicals, machinery, and hazardous working conditions.

## NATIONAL TRANSPORTATION

## SAFETY BOARD

490 L'Enfant Plaza SW
Washington, DC 20594
Ph\#: 202/382-6600
The National Transportation Safety Board is an independent federal accident investigation agency that also promotes transportation safety.

The board conducts safety studies; maintains official U.S. census of aviation accidents; evaluates the effectiveness of government agencies involved in transportation safety; evaluates the safeguards used in the transportation of hazardous materials; and evaluates the effectiveness of emergency responses to hazardous material accidents.

## NUCLEAR REGULATORY

COMMISSION
Office of Public Affairs
Washington, DC 20555
Ph\#: 301/415-8200
Fax: 301/415-2234
The Nuclear Regulatory Commission regulates the civilian uses of nuclear materials in the United States to protect the public health and safety, the environment, and the common defense and security.

The mission is accomplished through licensing of nuclear facilities and the possession, use and disposal of nuclear materials; the development and implementation of requirements governing licensed activities; and inspection and enforcement to assure compliance.

## OCCUPATIONAL SAFETY AND HEALTH ADMINISTRATION

Office of Information and Consumer Affairs
200 Constitution Avenue NW, Room N3647
Washington, DC 20210
Ph\#: 202/2198151
Fax: 202/219-5986
The Occupational Safety and Health Administration (OSHA) sets and enforces workplace safety and health standards with a goal of ensuring safe and healthful working conditions for all Americans.

OSHA issues standards and rules for safe and healthful working conditions, tools, equipment, facilities, and processes.

## OCCUPATIONAL SAFETY AND HEALTH REVIEW COMMISSION

Office of Public Information
One Lafayette Center
1120 20th Street, NW, Ninth Floor
Washington, DC 20036-3419
Ph\#: 202/606-5398
Fax: 202/606-5050
The Occupational Safety and Health Review Commission is an independent federal agency that serves as a court to provide decisions in workplace safety and health disputes arising between employers and the Occupational Safety and Health Administration in the department of labor.

## U.S. COAST GUARD

Hazard Materials Standards Branch 2100 Second Street SW
Washington, DC 20593-0001
Ph\#: 202/267-2970
Fax: 202/267-4816
The U.S. Coast Guard is the United States' primary maritime law enforcement agency as well as a federal regulatory agency and one of the armed forces.

The U.S. Coast Guard duties include aids to navigation; defense operations; maritime pollution preparedness and response; domestic and international ice breaking operations in support of commerce and science; maritime law enforcement; marine inspection and licensing; port safety and security; and search and rescue.

# INDUSTRY STANDARDS <br> Chemical Industry Trade Associations 

ADHESIVES MANUFACTURERS ASSOCIATION
1200 19th Street NW, Suite 300
Washington, DC 20036
Ph\#: 202/857-1127
Fax: 202/857-1115
The Adhesives Manufacturers Association (AMA) is a national organization comprised of major U.S. companies engaged in the manufacturing, marketing, and selling of formulated adhesives or formulated adhesives coatings to the industrial marketplace. Associate members supply raw materials to the industry.

## AIR \& WASTE MANAGEMENT

ASSOCIATION
1 Gateway Center, 3rd Floor
Pittsburgh, PA 15222
Ph\#: 412/232-3444
Fax: 412/232-3450
Membership Department
The Air \& Waste Management Association is a non-profit, technical and educational organization with 17,000 members in 58 countries. Founded in 1907, the association provides a neutral forum in which all viewpoints of an environmental issue (technical, scientific, economic, social, political, and health-related) receive equal consideration. The association serves its members and the public by promoting environmental responsibility and providing technical and managerial leadership in the fields of air and waste management.

## AMERICAN ACADEMY OF ENVIRONMENTAL ENGINEERS

 (AAEE)130 Holiday Court, Suite 100
Indianapolis, MD 21401
Ph\#: 301/261-8958 (Washington, DC)
This organization certifies environmental engineers.

## AMERICAN BOILER

MANUFACTURERS ASSOCIATION
950 N. Glebe Road, Suite 160
Arlington, VA 22203
Ph\#: 703/522-7350
Fax: 703/522-2665
The mission of the American Boiler Manufacturers Association is to improve services to the public; to be proactive with government in matters affecting the industry; to promote safe, economical, and environmentally friendly services of the industry; and to carry out other activities recognized as lawful for such organizations.

## THE AMERICAN CERAMIC SOCIETY

P.O. Box 6136

Westerville, OH 43086-6136
Ph\#: 614/890-4700
Fax: 614/899-6109
Customer Service: 614/794-5890
The American Ceramic Society is the headquarters for the professional organization for ceramic engineers.

## AMERICAN CHEMICAL SOCIETY

(ACS)
1155 Sixteenth Street NW
Washington, DC 20036
Ph\#: 202/872-4600
Fax: 202/872-6337
ACS has 149,000 members. The members are chemists, chemical engineers, or people who have degrees in related fields.

## AMERICAN COKE AND COAL

CHEMICALS INSTITUTE
1255 23rd Street NW
Washington, DC 20037
Ph\#: 202/452-1140
Fax: 202/466-4949
The ACCl's mission is to represent the interests of the coke and coal chemicals industry by communicating positions to legislative and regulatory officials, cooperating with all government agencies having jurisdiction over the industry, providing a forum for the exchange of information, and discussion of problems and promoting the use of coke and its byproducts in the marketplace.

AMERICAN CONFERENCE OF GOVERNMENTAL INDUSTRIAL HYGIENISTS (ACGIH)
Kemper Woods Center
1330 Kemper Meadow Drive, Suite 600
Cincinnati, OH 45240
Ph\#: 513/742-2020
Fax 513/742-3355
The ACGIH is an organization of more than 5,500 industrial hygienists and occupational health and safety professionals devoted to the technical and administrative aspects of worker health and safety.

## AMERICAN CROP PROTECTION ASSOCIATION

1156 15th Street NW, Suite 400
Washington, DC 20005
Ph\#: 202/872-3869
Fax: 202/463-0474
ACPA is the trade association for the manufacturers and formulators/distributors representing virtually all of the active ingredients manufactured, distributed, and sold in the United States for agricultural uses, including herbicides, insecticides, and fungicides.

AMERICAN INSTITUTE OF MINING, METALLURGICAL AND PETROLEUM ENGINEERS (AIME)
345 E. 47th Street
New York, NY 10017
Ph\#: 212/705-7695
Fax: 212/371-9622
AIME serves as the unifying forum for the Member Societies, which include the Society for Mining, Metallurgy and Exploration; The Minerals, Metals \& Materials Society; Iron and Steel Society; Society of Petroleum Engineers; and the AIME Institute Headquarters.

AMERICAN NATIONAL STANDARDS INSTITUTE, INC.
(ANSI) 11 W. 42nd Street, 13th Floor
New York, NY 10036
Ph\#: 212/642-4900
Fax: 212/302-1286
The Sales Department
ANSI is an approval entity in the United States for the voluntary standards effort.

## AMERICAN PETROLEUM INSTITUTE (API)

1220 L Street NW
Washington, DC 20005
Ph\#: 202/682-8000
Fax: 202/682-8232
The American Petroleum Institute (API) is the U.S. petroleum industry's primary trade association. API provides public policy development and advocacy, research, and technical services to enhance the ability of the petroleum industry to meet its mission.

AMERICAN SOCIETY OF BREWING CHEMISTS
3340 Pilot Knob Road
St. Paul, MN 55121
Ph\#: 612/454-7250
Fax: 612/454-0766
Member Services Representative
A non-profit organization that publishes scientific books and journals.

AMERICAN SOCIETY OF HEATING, REFRIGERATING AND AIR CONDITIONING ENGINEERS (ASHRAE)
1791 Tullie Circle NE
Atlanta, GA 30329
Ph\#: 404/636-8400
Fax: 404/ 321-5478
Customer Service: 800/527-4723
ASHRAE is an engineering society whose members are engineers specializing in heating, refrigerating, and air conditioning. It serves members through meetings and publications.

# INDUSTRY STANDARDS <br> Chemical Industry Trade Associations 

## AMERICAN SOCIETY OF MECHANICAL ENGINEERS (ASME)

345 E 47th Street
New York, NY 10017-2392
Ph\#: 212/705-7722
Fax: 212/705-7674
Member Services
This organization provides classes and networking, and also serves its members by providing information about technology and solutions to the problems of an increasingly technological society.

## AMERICAN SOCIETY FOR NONDESTRUCTIVE TESTING

 (ASNT)1711 Arlingate Lane
P.O. Box 28518

Columbus, OH 43228-0518
Ph\#: 614/274-6003
Fax: 614/274-6899
A non-profit organization that has 10,000 members worldwide. It sells technical books as well as providing testing for certification for non-destructive testing. This organization also publishes a monthly magazine.

## AMERICAN SOCIETY FOR QUALITY CONTROL (ASQC)

P.O. Box 3005

Milwaukee, WI 53201-3005
Ph\#: 414/272-8575
Fax: 414/272-1734
Customer Service: 800/ 248-1946
This organization facilitates continuous improvement and increased customer service by identifying, communicating, and promoting the use of quality concepts and technology. The ASQC carries out a variety of professional, educational, and informational programs.

## AMERICAN SOCIETY OF SAFETY ENGINEERS

1800 E. Oakton
Des Plaines, IL 60018-2187
Ph\#: 847/699-2929
Membership Department, extensions 231, 228, or 254
Fax: 847/296-3769
This is the oldest and largest organization servicing safety engineers. It has more than 32,000 members and 139 local chapters. The society provides safety education seminars, technical publications, and a monthly magazine among other services.

## AMERICAN SOCIETY FOR TESTING

## \& MATERIALS (ASTM)

100 Barr Harbor Drive
W. Conshohocken, PA 19428

Ph\#: 610/832-9500
Fax: 610/832-9555
Membership Department
This non-profit organization deals with 132 different committees, and provides materials and tests different standards.

## CHEMICAL MANUFACTURERS

ASSOCIATION (CMA)
1300 Wilson Boulevard
Arlington, VA 22209
Ph\#: 703/741-5000
Fax: 703/741-6095
CMA is one of the oldest trade associations in North America. The CMA is also the focal point for the chemical industry's collective action on legislative, regulatory, and legal matters at the international, national, state and local levels.

## CHLORINE INSTITUTE

2001 L Street NW \#506
Washington, DC 20036
Ph\#: 202/775-2790
Fax: 202/223-7225
This organization supports the chloralkaline industry and serves as a public service for safety and health.

## COMPOSITES FABRICATORS ASSOCIATION

8201 Greensboro Drive, Suite 300
McLean, VA 22102
Ph\#: 703/610-9000
Fax: 703/610-9005
The Composites Fabricators Association provides educational services including seminars, video training tapes, publications, a monthly technical magazine, and an annual convention. It offers free technical, government, and regulatory service to its members.

COSMETIC, TOILETRY AND FRAGRANCE ASSOCIATION
1101 17th Street NW, Suite 300
Washington, DC 200364702
Ph\#: 202/331-1770
Fax: 202/331-1969
The Cosmetic, Toiletry and Fragrance Association is the leading trade association for the personal care product industry, representing the majority of U.S. personal care product sales. The industry trade association was founded in 1894.

## FEDERATION OF SOCIETIES FOR COATINGS TECHNOLOGY

492 Norristown Road
Blue Bell, PA 19422
Ph\#: 610/940-0291
Fax: 610/940-0292
This is a trade association for the paint industry.

## HAZARDOUS MATERIALS ADVISORY COUNCIL

1101 Vermont Avenue NW, Suite 301
Washington, DC 20005-3521
Ph\#: 202/289-4550
Fax: 202/289-4074
Incorporated in 1978, the Hazardous Materials Advisory Council (HMAC) is an international, non-profit organization devoted to promoting regulatory compliance and safety in the transportation of hazardous materials, substances, and wastes.

ISA
P.O. Box 12277

67 Alexander Drive
Research Triangle Park, NC 27709
Ph\#: 919/549-8411
Fax: 919/549-8288
Brian Duckett, Meetings Manager
ISA develops standards for the instrumentation and control field.

## METAL FINISHING SUPPLIERS' ASSOCIATION

801 N. Cass Avenue, Suite 300
Westmont, IL 60559
Ph\#: 708/887-0797
Fax: 708/887-0799
MFSA is an organization representing 175 member companies who are suppliers of equipment, chemicals, and services to the metal finishing industry.

## NACE INTERNATIONAL

National Association of Corrosion Engineers
P.O. Box 218340

Houston, TX 77218-8340
Ph\#: 713/492-0535
Fax: 713/492-8254
This organization provides a number of services to its members: the selling of books, publications, magazines, classes, seminars and symposiums are among some of those services.

NATIONAL ASSOCIATION OF CHEMICAL RECYCLERS
1900 M. Street NW, Suite 750
Washington, DC 20036
Ph\#: 202/296-1725
Fax: 202/296-2530

# INDUSTRY STANDARDS <br> Chemical Industry Trade Associations 

## NATIONAL ASSOCIATION OF

PRINTING INK MANUFACTURERS, INC.
(NAPIM)
Heights Plaza, 777 Terrace Avenue
Hasbrouck Heights, NJ 07604
Ph\#: 201/288-9454
Fax: 201/288-9453
The National Association of Printing Ink Manufacturers is a trade association whose purpose it is to represent the printing ink industry in the United States and to provide direction to management in the areas of environmental issues, business management, government regulations, and regulatory compliance.

## NATIONAL FIRE PROTECTION

## ASSOCIATION (NFPA)

1 Batterymarch Park
Quincy, MA 02269-9101
Ph\#: 617/770-3000
Fax: 617/770-0700
Member Services
Fire protection standards and manuals. Services and interpretation of standards are available to members only

## PHARMACEUTICAL RESEARCH AND MANUFACTURERS OF

 AMERICA1100 Fifteenth Street NW, Suite 900
Washington, DC 20005
Ph\#: 202/845-3400
Fax: 202/835-3414
The Pharmaceutical Research and Manufacturers of America (PhRMA) represents the country's largest research based pharmaceutical and biotechnology companies. Investing nearly $\$ 16$ billion a year in discovering and developing new medicines. PhRMA companies are the source of nearly all new drug discoveries worldwide.

## PROCESS EQUIPMENT

## MANUFACTURERS' ASSOCIATION

111 Park Place
Falls Church, VA 22046-4513
Ph\#: 703/538-1796
Fax: 703/241-5603
The Process Equipment Manufacturers' Association is an organization of firms and corporations engaged in the manufacture of process equipment such as agitators, mixers, crushing, grinding and screening equipment, vacuum and pressure filters, centrifuges, furnaces, kilns, dryers, sedimentation and classification devices, and waste treatment equipment.

## PULP CHEMICALS ASSOCIATION, INC

15 Technology Parkway South
Norcross, GA 30092
Ph\#: 770/446-1290
Fax: 770/446-1487
The Pulp Chemicals Association Inc. is an international trade association serving the common goals of its membership. Any person, firm or corporation who manufactures chemical products derived from the pulp and forest products industries is eligible for membership.

## RUBBER MANUFACTURERS ASSOCIATION

1400 K Street NW, Suite 900
Washington, DC 20005
Ph\#: 202/682-4800
Fax: 202/682-4854
The Rubber Manufacturers Association is a trade association representing the rubber and tire industry in North America.

SOAP AND DETERGENT ASSOCIATION 475 Park Avenue, S.
New York, NY 10016
Ph\#: 212/725-1262
Fax: 212/213-0685
This is a national, non-profit trade association that represents the manufacturers of soaps and detergents.

## SOCIETY FOR THE ADVANCEMENT

OF MATERIAL AND PROCESS ENGINEERING
(SAMPE)
P.O. Box 2459

Covina, CA 91722
Ph\#: 818/33-0616
Fax: 818/332-8929
SAMPE is a global, member-governed, volunteer, not-for-profit organization, which supplies information on advanced state-of-theart materials and process opportunities for career development within the materials and process industries.

## SOCIETY OF PLASTICS ENGINEERS

14 Fairfield Drive
Brookfield, CT 06804-0403
Ph\#: 203/775-0471
Fax: 203/775-8490
This society deals with education, holds seminars and conferences, and produces magazines and journals. Membership of 37,500 worldwide individuals in all areas of the plastics industry, in 70 countries.

## THE SOCIETY OF THE PLASTICS

INDUSTRY INC.
1275 K Street NW, Suite 400
Washington, DC 20005
Ph\#: 202/371-5200
Fax: 202/371-1022
VALVE MANUFACTURERS
ASSOCIATION OF AMERICA (VMA)
1050 17th Street NW, Suite 280
Washington, DC 20036
Ph\#: 202/331-8105
Fax: 202/296-0378

## WANER ENVIRONMENT

FEDERATION
601 Wythe Street
Alexandria, VA 22314-1994
Ph\#: 703/684-2400
Fax: 703/684-2450
Member Services


## CHEMICAL RESISTANCE GUIDE

The chemical resistance data provided here on the following pages has been assembled from a wide variety of sources in our industry. This information is based on practical field experience and actual laboratory testing conducted by the manufacturers of various plastic resins and finished products. Keep in mind that this information should only be used as a guideline for recommendations and not a guarantee of chemical resistance. Some performance variations may be noticed between homopolymers and copolymers as well as emulsion and suspension type resins of the same general type. In addition, actual service conditions including temperature, concentration, and contaminant's will affect variances in chemical resistance.

In assembling the chemical resistance data presented here, several sources were checked. When conflicts were uncovered, we took a conservative approach and used the lower of two or more ratings. In addition, special consideration was given to the material as supplied by a particular vendor; i.e., our polyethylene ratings are based on information provided by tank manufacturers rather than pipe suppliers. This was done primarily because of the volume of tanks supplied as compared to polyethylene pipe.

In an attempt to make the recommendations more meaningful, we have given the maximum recommended use temperature for each plastic and elastomer in the specific chemicals listed. Lacking complete data in many cases we did leave those in question as blanks. Where a material is unsuitable for a specific chemical an " $X$ " is used.

Metals are listed as:

A = Excellent
$B=$ Good, minor effect
C = Fair, needs further tests
X = Unsuitable

To the best of our knowledge, the information contained in this publication is accurate. However, we do not assume any liability whatsoever for the accuracy or completeness of such information. Moreover, there is a need to reduce human exposure to many materials to the lowest physical limits in view of possible long term adverse effects. To the extent that any hazards may have been mentioned in this publication, we neither suggest nor guarantee that such hazards are the only ones which exist. Final determination of the suitability of any information or product for the use contemplated by any user, the manner of that use and whether there is any infringement of patents, is the sole responsibility of the user. We recommend that anyone intending to rely on any recommendation or use any equipment, processing technique, or material mentioned in this publication should satisfy themselves as to such suitability, and that they meet all applicable safety and health standards. We strongly recommend the user seek and adhere to manufacturers' or suppliers' current instructions for handling each material they use.

## USE OF THE CHEMICAL RESISTANCE TABLES

The aggressive agents are classified alphabetically according to their most common designation. Further descriptions include trivial or common names as trade names.

If several concentrations are given for a particular material, the physical data, in general, relates to the pure product that is $100 \%$ concentration.

In listing the maximum use temperature for each plastic type in a given chemical, it can in general be assumed that the resistance will be no worse at lower temperatures.

## HOW TO SELECT THE CORRECT MATERIAL:

1. Locate the specific chemical in the system or found in the surrounding atmosphere using the alphabetical chart of chemicals.
2. Select the material with a maximum use temperature that matches or exceeds the need. The Harrington philosophy has always been to suggest the least costly material that will do the job.
3. Where a material or elastomer appears to be marginal compared to the requirements, we encourage a call to our technical service group.

## EXAMPLES:

1. Methylene chloride: in the tables PVDF, Halar, or Teflon are the only materials suitable. Carbon steel
works well and that would er reason to justify be our choice unless there was anoththe higher cost of the PVDF, Teflon or Halar.
2. Sodium hypochlorite, $15 \%$ at $100^{\circ} \mathrm{F}, \mathrm{PVC}$ is good to $140^{\circ} \mathrm{F}$ and is the least expensive of the materials available.
3. For nitric acid $40 \%$ ambient temperature, the tables recommend either CPVC or polypropylene at $73^{\circ} \mathrm{F}$. In most cases CPVC will be the economical choice. Note that PVDF is rated for higher temperature use.

NOTE: The ratings shown for carbon and ceramic pump seals are approximate. Please contact your local Harrington service center for a recommendation on your specific application.

## CHEMICAL RESISTANCE GUIDE

| CHEMIICAL |  |  | $\stackrel{0}{0}$ ${ }_{i}^{2}$ $\frac{1}{2}$ $\frac{2}{2}$ $\frac{1}{4}$ $\begin{aligned} & 3 \\ & 0 \\ & 0 \end{aligned}$ |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Acetaldehyde | $\mathrm{CH}_{3} \mathrm{CHO}$ | - | X | X | 100 | 120 | X | X | X | 200 |  |  | 350 | 150 | X | $\times$ | 100 | 200 | X | x | A |  |  | A | A |  |  | A |
| Acetaldehyde, Aqueous | - | 40 | X | X | 100 | 120 | X | X | - | 200 | - | - | 350 | 150 | X | X | 100 | 200 | X | X | A |  |  | A | A |  |  | A |
| Acetamide | $\mathrm{CH}_{3} \mathrm{CONH}_{2}$ | - - | - - | - | 100 | 73 | 150 | - | - | - | - | - | - | - | - | - | 200 | 200 | X | 100 |  |  |  | B | A |  |  | - |
| Acetate Solvents, Crude |  | - | X | X | - | 78 | - | - | X | - | - | - | 350 | - | - |  | X | X | X | x | A |  |  | B | A |  |  | B |
| Acetate Solvents, Pure |  | - - | X | X | - | X | - | - | X | - |  | - | 350 | - | - |  | X | X | X | X |  |  |  | B | A |  |  |  |
| Acetic Acid* | $\mathrm{CH}_{3} \mathrm{COOH}$ | 5 | 140 | 140 | 200 | 140 | X | 140 | 68 | 200 | 250 | - | 350 | 150 | 200 | - | X | 200 | 100 | - |  |  |  | A | A |  |  | A |
| Acetic Acid* | $\mathrm{CH}_{3} \mathrm{COOH}$ | 10 | 140 | 140 | 200 | 140 | X | 140 | 68 | 200 | 250 | - | 350 | 150 | 200 | - | 180 | 200 | X | x |  |  |  | A | A |  |  | A |
| Acetic Acid* | $\mathrm{CH}_{3} \mathrm{COOH}$ | 20 | 140 | 0140 | 200 | 140 | X | 140 | X | 200 | 250 | - | 350 | X | 200 | - | 180 | 200 | X | X |  |  |  | A | A |  |  | A |
| Acetic Acid* | $\mathrm{CH}_{3} \mathrm{COOH}$ | 30 | 140 | O 140 | 200 | 140 | X | 140 | X | 200 | 250 | - | 350 | - | 100 | - | 180 | 200 | - | - |  |  |  | A | A |  |  | A |
| Acetic Acid* | $\mathrm{CH}_{3} \mathrm{COOH}$ | 50 | 100 | 0100 | 200 | 100 | X | 140 | X | 200 | 250 | - | 350 | X | 100 | - | 180 | 200 | X | X |  |  |  | A | A |  |  | A |
| Acetic Acid* | $\mathrm{CH}_{3} \mathrm{COOH}$ | 60 | 73 | 73 | 150 | 100 | X | 140 | X | 200 | - | - | 350 | X | X | - | 180 | 100 | X | x | - |  |  | A | A |  |  | A |
| Acetic Acid* | $\mathrm{CH}_{3} \mathrm{COOH}$ | 80 | X | X | 140 | 73 | X | 70 | X | 200 | 212 | - | 350 | X | x | - | 180 | 100 | X | X | - |  |  | A | A |  |  | A |
| Acetic Acid*, Glacial | $\mathrm{CH}_{3} \mathrm{COOH}$ | 1001 | 1.0 | 10110 | 180 | 180 | X | 70 | X | 200 | 212 | 300 | 350 | X | x | - | X | 73 | X | x | A |  |  | A | A |  |  | A |
| Acetic Anhydride | $\left(\mathrm{CH}_{3} \mathrm{CO}\right)_{2} \mathrm{O}$ | - 5 | X | X | 73 | 90 | X | X | X | 200 | 73 | - | - | X | X | - | X | 200 | X | x | A |  |  |  |  |  |  | - |
| Acetic Ether (See Ethyl Acetate) | - | - - | - - | - | - | - | - | - | - | - | - | - | - | - | - |  | - | - | - | - |  |  |  | - |  |  |  | - |
| Acetol (Hydroxy 2 Propanone) | - | - - | - - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - |  |  |  | A | A |  |  | A |
| Acetone | $\mathrm{CH}_{3} \mathrm{COCH}_{3}$ | - | X | X | - | - | - | - | - | 200 | 150 | - | - | - | - |  | - | - | - | - |  |  |  | A | A |  |  | A |
| Acetonitrile (Methyl Cyanide) | $\mathrm{CH}_{3} \mathrm{CN}$ | - - | X | X | X | 150 | X | X | X | 200 | 212 | - | 400 | X | X | - | X | - | X | x |  |  |  | A | A |  |  | A |
| Acetophenone | $\mathrm{C}_{6} \mathrm{H}_{5} \mathrm{COCH}_{3}$ | 0 | 0.8 X | X | 150 | 200 | - | - | X | 200 | 121 | - | 400 | 120 | x | - | X | - |  | X | - |  |  | A | A |  |  | B |
| Acetyl Acetone | - | - - | - - | - | - | - | - | - | - | - |  | - | - | - | - | - | - | - | - | - |  |  |  | - |  |  |  |  |
| Acetyl Benzene | $\mathrm{C}_{6} \mathrm{H}_{5} \mathrm{COCH}_{3}$ | - - | X | X | 73 | 73 | - | - | X | - | - | - | - | X | X | - | X | - | X | x |  |  |  |  | A |  |  |  |
| Acetyl Bromide | - | 1. | 1.0 X | X | - | - | - | - | X | - | - | - | - | X | X | - | X | - | X | x | - |  |  | - | A |  |  | - |
| Acetyl Chloride (dry) | $\mathrm{C}_{6} \mathrm{H}_{5} \mathrm{COCH}_{3}$ | - 3 | 3 | - | - | 100 | X | X | X | 200 | 150 | - | - | X | X | - | - | X | - | - | - |  |  | - | A |  |  | - |
| Acetyl Oxide | $\mathrm{CH}_{3} \mathrm{COBr}$ | - | - - | - | - | - | - | - | X | - | - | - | - | - | - | - | - | - | - | - |  |  |  | - |  |  |  | - |
| Acetyl Propane | $\mathrm{CH}_{3} \mathrm{COCL}$ | - - | X | X | 130 | 100 | - | - | X | - | - | - | 200 | - | - | - | X | - | X | x | - |  |  | A | A |  |  | - |
| Acetylene | $\left(\mathrm{CH}_{3} \mathrm{CO}\right)_{2} \mathrm{O}$ | - | 100 | 0100 | - | 200 | - | - | - | 200 | 150 | - | - | - | - | - | - | - | - | - | A |  |  | - | A |  |  | B |
| Acetylene Dichloride | CLHC:CHLC | - - | X | X | - | X | - | - | x | - | - | - | 300 | - | - | - | 150 | - | - |  | - |  |  | - |  |  |  | - |
| Acetylene Tetrachloride | $\left(\mathrm{CHCL}_{2}\right)_{2}$ | - | - - | - | - | - | - | - | X | - | - | - | - | - | - |  |  | - | - | - |  |  |  |  |  |  |  |  |
| Acid Mine Water | - | - - | 100 | 0150 | 150 | 250 | - | - | - | 200 | - | - | 350 | - | - | - | - | - | - | - |  |  |  |  |  |  |  |  |
| Acrylic Acid | $\mathrm{CH}_{2} \mathrm{CHCOOH}$ | - - | X | X | X | 100 | X | X | X | - | 212 | - | 170 | X | X | - | - | - | - | - |  |  |  | - |  |  |  | - |
| Acrylic Emulsions* | - | - - | - - | - | - | - | X | 70 | - | - | - | - | - | - | - |  | X | X | X | X |  |  |  | A |  |  |  | A |
| Acrylonitrile | $\mathrm{H}_{2} \mathrm{CCHCN}$ | - | X | X | 73 | 100 | 140 | 140 | X | - | 73 | - | 350 | 100 | X | - | 250 | 200 | 160 | 180 | A |  |  | B |  |  |  | B |
| Adipic Acid Aqueous | - | - - | 140 | 0180 | 100 | 250 | 140 | 140 | - | - | 150 | - | 350 | - | - |  |  | - | - | - |  |  |  | A | A |  |  | A |
| Alcohol (See Ethyl Alcohol) | - | - - | - - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - |  |  |  | - |  |  |  | - |
| Alcohol, Allyl | - | - - | 80 | 80 | 140 | 200 | 100 | 140 | X | - | - | - | 250 | 200 | 100 | - | 200 | 70 | 100 | 180 |  |  |  | A |  |  |  | A |
| Alcohol, Amyl | $\mathrm{C}_{5} \mathrm{H}_{11} \mathrm{OH}$ | - - | 100 | 0100 | 170 | 250 | 140 | 140 | X | 200 | 250 | - | 400 | 200 | 100 | - | 190 | 200 | 140 | 140 |  |  |  | A |  |  |  | A |
| Alcohol, Benzyl | $\mathrm{C}_{6} \mathrm{H}_{5} \mathrm{CH}_{2} \mathrm{OH}$ | - - | X | X | 140 | 180 | - | ${ }^{-}$ | X | - | 250 | - | - | - | - | - | 140 | X | 140 | X | - |  |  | A |  |  |  | A |
| Alcohol, Butyl | - | - | 140 | 0180 | 180 | 240 | 140 | 140 | X | 200 | 250 | - | 250 | 200 | 100 |  | 100 | 180 | 140 | 140 | - |  |  | A |  |  |  | A |
| Alcohol, Diacetone | - | - | X | - | 73 | 73 | - | - | X | - | 150 | - | 350 | - | - |  | X | 70 | X |  | - |  |  | A |  |  |  | A |
| Alcohol, Ether | - | - - | - - | - | - | - | - | - | - | - | - | - | - | - |  |  | - | - | - | - | - |  |  | - |  |  |  | - |
| Alcohol, Ethyl | $\mathrm{C}_{2} \mathrm{H}_{5} \mathrm{OH}$ | - - | 140 | 0 * | 180 | 750 | 140 | 140 | X | - | 250 | - | 300 | 180 | - |  | 170 | 170 | 170 | 200 | A |  |  | A |  |  |  | A |
| Alcohol, Hexyl | - | - - | 100 | - 70 | 70 | - | - | - | X | - | 73 | - | - | - | - | - | 160 | X | 70 | 70 | A |  |  | A |  |  |  | A |
| Alcohol, Isobutyl | $\left(\mathrm{CH}_{3}\right)_{2} \mathrm{CHCH}_{2} \mathrm{OH}$ | - | - - | - | - | 250 | - | - | X | - | - | - | 300 | 180 | 100 |  | 140 | 140 | 70 | 70 | A |  |  | A |  |  |  | A |
| Alcohol, Isopropyl | $\left(\mathrm{CH}_{3}\right)_{2} \mathrm{CHOH}$ | - - | 140 | 0 | 150 | 230 | 140 | 140 | X | - | 250 | - | 300 | 180 | 100 |  | 200 | 140 | 70 | 200 | A |  |  | A |  |  |  | - |
| Alcohol, Methyl | $\mathrm{CH}_{3} \mathrm{OH}$ | - - | 140 | 150 | 150 | 230 | 140 | 140 | X | - | 250 | - | 300 | 150 | - | - | 100 | 100 | 140 | 140 | A |  |  | A |  |  |  | A |
| Alcohol, Octyl | - | - - | - - | - | - | - | - | - | - | - | - | - | - | - | - |  | - | - | - |  | A |  |  | - |  |  |  | - |
| Alcohol, Polyvinyl | - | - | 140 | 180 | 180 | 250 | - | - | 68 | - | - | - | 280 | 150 | 100 | - | 210 | 100 | - | - | A |  |  | A |  |  |  | - |
| Alcohol, Propargyl | - | - - | - - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | A |  |  | - |  |  |  | - |
| Alkanes | - | - - | 140 | 100 | 100 | 250 | - | - | - | - | - | - | 300 | - | - | - | 210 | X | X | X |  |  |  | A |  |  |  | - |
| Alkazene | - | - - | - - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - |  |  | - |  |  |  | - |
| Allyl Aldehyde | - | - - | - - | - | - | - | - | - | X | - | - | - | - | - | - | - | - | - | - | - | - |  |  | - |  |  |  | - |
| Allyl Bromide | $\mathrm{C}_{3} \mathrm{H}_{5} \mathrm{Br}$ | - - | X | - | - | - | - | - | X | - | - | - | - | - | - | - | - | - | - | - | - |  |  | - |  |  |  | - |
| Allyl Chloride | $\mathrm{C}_{3} \mathrm{H}_{5} \mathrm{CL}$ | - | X | X | 100 | 200 | 100 | - | X | - | 250 | - | 350 | - | - | - | 100 | X | X | X |  |  |  | A |  |  |  | - |
| Alum (See Aluminum Sulfate) | $\mathrm{AL}_{2}\left(\mathrm{SO}_{4}\right)_{3}$ |  | - - | - | - | - | - | - | - | - | - | - | - | - | - |  | - | - | - | - | - |  | - | - |  |  | , | - |

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## CHEMICAL RESISTANCE GUIDE



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| CHEMIICAL | FORMULAS |  |  |  |  |  |  |  |  | I |  | $A S$ |  |  |  |  |  |  |  | TAL |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Calcium Nitrate | $\mathrm{Ca}\left(\mathrm{NO}_{3}\right)_{2}$ | 1.82 | . 82140 | 180 | 180 | 250 |  | 140 | 140 | 200 | 250 | - |  |  | 200 | - | 210 | 180 |  |  |  |  |  | A |  | - |  |
| Calcium Oxide | CaO | - - | 140 | 180 | 180 | 250 | 140 | - | 150 | - | 250 | - | 400 | - | - | - | - | 210 | 160 | 180 |  |  |  | A |  |  |  |
| Calcium Phosphate | $\mathrm{CaH}_{4}\left(\mathrm{PO}_{4}\right)_{2}$ |  | 2.3 | - | - | - | 140 | 140 | - | - | - | - | - | 150 | - |  |  |  |  | - |  |  |  |  |  |  |  |
| Calcium Sulfate | $\mathrm{CaSO}_{4}$ | 2.9 | 2.9140 | 180 | 180 | 210 | 140 | 140 | 150 | 200 | 250 | - | 400 | 250 | 200 | - | 200 | 210 | 150 | 180 | A |  |  | A | A | A | B |
| Calcium Sulfide | CaS | - - | 140 | 140 | 180 | 180 | 140 | 140 | - | - | - | - | 400 | 200 | 200 | - | 200 | 150 | 100 | 150 |  |  |  |  |  |  |  |
| Calcium Thiosulfate | $\mathrm{CaS}_{2} \mathrm{O}_{3}$ | 1.87 | . 87 | - | - | - | 140 | 140 | - | - | - | - | - | - | - |  | - | - | - | - |  |  |  |  |  |  |  |
| Calgon (Sodium | - |  | - - | - | - | - | - | - |  | - | - | - | - | - | - |  | - | - |  |  |  |  |  |  |  |  |  |
| Hexametaphosphate) | - | - | - - | - | - | - |  | 140 | - | - | - | - | - | - | - | - | - | - |  | - | A |  |  |  |  |  | - |
| Cane Sugar Liquors | - | - - | 140 | 180 | 140 | 250 | 140 | - | 150 | - | 150 | - | 350 | - | - | - | 200 | 250 | 150 | 150 | A |  |  | A | A | - | A |
| Caprylic Acid (Octanic Acid) | $\mathrm{CH}_{3}\left(\mathrm{CH}_{2}\right)_{6} \mathrm{COOH}$ | - - | 140 | 180 | 150 | 220 | - | - | X | - | 150 | - | 350 | X | 200 | - | - | - | - | - | A |  |  |  |  |  |  |
| Carbinol (See Alcohol, Methyl) | - |  | - - | - | - | - | - | - | - | - | - | - | - | - | - |  | - | - |  |  |  |  |  |  |  |  |  |
| Carbolic Acid (see Phenol) | - | - - | - - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - |  | - |  |  |  |  |  |  |  |
| Carbon Bisulfide (see | - |  | - - | - | - | - | - | - | X | - | - | - | - | - | - | - | - | - | - | - |  |  |  |  |  |  |  |
| Carbon Disulfide) | $\mathrm{CS}_{2}$ |  | - - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - |  |  |  |  |  |  | A |
| Carbon Dioxide (wet or dry) | $\mathrm{CO}_{2}$ | - - | 140 | 180 | 180 | 250 | 140 | 140 | 90 | - | 250 | - | 350 | 200 | 200 | - | 210 | 170 | 150 | 180 |  |  |  | A | A | A | A |
| Carbon Disulfide | $\mathrm{CS}_{2}$ | - - | X | X | X | 68 | X | X | X | 200 | 73 | - | 400 | 73 | X | - | 180 | X | X | X | A |  |  | A | A | - | A |
| Carbon Monoxide | CO | - - | 140 | 180 | 180 | 250 | 140 | 140 | 140 | - | 150 | - | 400 | 200 | 200 | - | 180 | - | 200 | 180 | A |  |  | A | A | - |  |
| Carbon Tetrachloride | $\mathrm{CCL}_{4}$ | 1.6 | . 6 X | X | X | 140 | X | X | X | - | 250 | - | 350 | 150 | - | - | 190 | X | X | X | A |  |  | A | C | A | A |
| Carbonic Acid | $\mathrm{H}_{2} \mathrm{CO}_{3}$ | - - | 140 | 210 | 210 | 250 | 140 | 140 | - | - | 250 | - | 350 | 180 | 140 | - | 200 | 210 | 70 | 180 | A |  |  | A | A | - | A |
| Casein | - | - - | - - | - | - | 50 | - | - | - | - | - | - | 250 | - | - | - | 180 | 180 | - | - |  |  |  | - |  |  | - |
| Castor Oil | - | 0.95 | 0.95140 |  | 150 | 250 | 140 | 140 | 140 | - | 250 | - | 350 | 220 | 200 | - | 140 | 140 | 100 | 140 |  |  |  | A | A | - | A |
| Catsup | - | - - | - - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - |  |  |  | A | A |  | A |
| Caustic Lime -Calcium Hydroxide | $\mathrm{Ca}(\mathrm{OH})_{2}$ | - - | 140 | 180 | 200 | 250 | - | - | 176 | - | 250 | - | 250 | 100 | 180 | - | 210 | 210 | 70 | 140 | A |  |  | A |  |  | A |
| Caustic Potash (Potassium | - | - - | - - | - | - | - | - | - | 176 | - | 250 | - | - | - | - | - | - | - | - | - |  |  |  | - |  |  |  |
| Hydroxide) | KOH | 2.04 | . 04140 | 180 | 200 | 140 | - | - | - | - | - | - | 200 | 180 | 150 | - | X | 200 | 150 | 70 |  |  |  | A | - | - | - |
| Caustic Soda (Sodium | - | - - | - - | - | - | - | - | - | 176 | - | 250 | - | - | - | - | - | - | - | - | - |  |  |  | - | - | - | - |
| Hydroxide) | NaOH | 2.13 | 13140 | 180 | 200 | 100 | X | 140 | - | - | - | - | 250 | 120 | 100 | - | X | 200 | 140 | 180 |  |  |  | A | - | - |  |
| Cellosolve (See Butyl Cellosolve) | - |  | - - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - |  |  |  | - | - | - | - |
| Cetyl Alcohol | $\mathrm{C}_{16} \mathrm{H}_{33} \mathrm{OH}$ | - - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - |  |  |  | - | - | - | - |
| Chloral Hydrate (knockout drops) | $\mathrm{CCL}_{3} \mathrm{CH}(\mathrm{OH})_{2}$ | 1.9 | 1.9140 | 160 | X | 200 | - | - | - | - | 121 | - | 200 | - | - | - | X | - | - | X |  |  |  | - | C | - | - |
| Chloroacetic Acid | $\mathrm{CH}_{2} \mathrm{CLCOOH}$ | X | - - | X | - | - | X | X | X | - | 212 | - | 300 | 100 | 200 | - | X | - | X | X |  |  |  | C | C | - | - |
| Chloric Acid | $\mathrm{HClO}_{3}$ | 20 | 140 | 180 | 140 | - | - | - | - | - | - | - | 140 | - | - | - | 100 | - | - | - |  |  |  | C | X | - | A |
| Chloric Acid | $\mathrm{HClO}_{3}$ | - - | - - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - |  |  |  | X | - |  | - |
| Chlorinated Glue | - | - - | - - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - |  |  |  |  | - |  | - |
| Chlorine Dioxide | $\mathrm{CLO}_{2}$ | 15 | 73 | 73 | X | 200 | - | - | X | - | 150 | - | 140 | X | 150 | - | 140 | X | X | X |  |  |  |  | X |  | - |
| Chlorine Gas Dry | $\mathrm{CL}_{2}$ | - - | X | X | X | 250 | X | X | X | - | 212 | - | 350 | X | 150 | - | 140 | X | X | X | A |  |  | - | - | - | - |
| Chlorine Gas Wet | - | - - | X | X | X | - | X | X | X | - | 212 | - | - | X | 200 | - | 140 | X | X | X |  |  |  | A | - | - | A |
| Chlorine Liquid | - | - - | X | X | X | 200 | X | X | X | - | 212 | - | 400 | - | - | - | 140 | - | - | X | - |  |  | C | - | - | A |
| Chlorine Water | - | - - | 140 | 180 | - | 250 | - | - | - | - | 212 | - | 400 | - | 200 | - | 180 | 73 | X | X | C |  |  | - | - | - | - |
| Chlorosulfonic Acid | $\mathrm{CLSO}_{2} \mathrm{OH}$ | 61.77 | .77 X | X | X | X | X | X | - | X | 73 | - | 180 | - | X | - | X | X | X | X | - |  |  | X | - | - | - |
| Chlorox Bleach | $\mathrm{NaOCL}: \mathrm{H}_{2} \mathrm{O}$ | 5.5 | 140 | 140 | 140 | 140 | 140 | 140 | - | - | 212 | - | 350 | X | 150 | - | 140 | 100 | 73 | 73 |  |  |  | X | B | X | - |
| Chocolate Syrup | - | - - | - - | - | 100 | - | - | - | - | - | - | - | - | - | - | - | 100 | - | 100 | - |  |  |  | - | A | - | B |
| Chrome Alum (Chr. Potass. Sulf.) | $\mathrm{CrK}\left(\mathrm{SO}_{4}\right)_{2}$ | - - | 73 | 73 | 140 | 200 | 140 | 140 | 176 | - | - | - | 210 | 200 | 200 | - | 210 | 140 | 160 | 150 | - |  |  | A | - | - | - |
| Chromic Acid | $\mathrm{H}_{2} \mathrm{CrO}_{4}$ | 58.8 | 2.8140 | 180 | 140 | 250 | 140 | 140 | X | 200 | 250 | - | 400 | X | 200 | - | 180 | 73 | X | - | X |  |  | B | A | - | - |
| Chromic Acid | $\mathrm{H}_{2} \mathrm{CrO}_{4}$ | 10 | 140 | 180 | 140 | 250 | 140 | 140 | X | 200 | 212 | - | 400 | X | 100 | - | 180 | 73 | X | - | X |  |  | A | - | - | A |
| Chromic Acid | $\mathrm{H}_{2} \mathrm{CrO}_{4}$ | 20 | 140 | 180 | X | 250 | 140 | 140 | X | 200 | 212 | - | 400 | X | 100 | - | 140 | 73 | X | - | X |  |  | B | B | - | A |
| Chromic Acid | $\mathrm{H}_{2} \mathrm{CrO}_{4}$ | 30 | 100 | 180 | X | 200 | 100 | 140 | X | 200 | 212 | - | 400 | X | X | - | 300 | - | - | 140 | X |  |  | B | - | - | A |
| Chromic Acid | $\mathrm{H}_{2} \mathrm{CrO}_{4}$ | 50 | X | 73 | - | 180 | 100 | 140 | X | 200 | 212 | - | 350 | X | X | - | 300 | - | - | 140 | X |  |  | C | B | A | B |
| Chromium Alum. | - | - - | - - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - |  |  |  | - | - | - | - |
| Citric Acid | - | 1.5 | . 54140 | 180 | 180 | 240 | 140 | 140 | 176 | 200 | 250 | - | 200 | 250 | 200 | - | 200 | 200 | 200 | 200 | - |  |  | - | - | - | - |
| Citric Oils | - | - - | - - | - | - | - | - | - | - | 200 | - | - | - | - | - | - | - | - | - | - | A |  |  | - | - | - | - |
| Cobalt Chloride | $\mathrm{CoCL}_{2}$ | 3.35 | . 35 | - | 100 | - | - | - | 176 | - | - | - | - | - | - | - | - | X | - | - |  |  |  | - | - | - | - |
| Coconut Oil | - | - - | - - | - | 100 | 250 | 140 | 140 | - | 200 | 250 | - | 250 | - | - | - | 340 | - | - | 200 |  |  |  | - | - | - | - |
| Cod Liver Oil | - | - - | - - | - | - | - | - | - | - | 200 | - | - | - | - | - | - | - | - | - | - | - |  |  | - | - | - | - |

## CHEMICAL RESISTANCE GUIDE



## CHEMICAL RESISTANCE GUIDE

| CHEMICAL | FORMULAS |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  | EA |  |  | TAL <br> 7 |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Dichlorobenzene | $\mathrm{C}_{6} \mathrm{H}_{4} \mathrm{CL}_{2}$ | - - | X | X | 100 | 140 | - | - | X | - | 121 |  | 350 | 120 | X |  | 150 | X | X | X |  |  |  |  |  |  |  |
| Dichlorethylene | CLHC:CHCL | 1.25 | 5 X | X | X | 120 | - | - | X | - | 73 | - | 350 | - | - | - | 190 | X | X | X |  |  |  |  |  |  |  |
| Dichloroisopropyl (Ether) | - | - - | X | X | X | 100 | - | - | X | - | - | - |  |  | - |  | - |  |  | - |  |  |  |  |  |  |  |
| Dichloromethane | $\mathrm{CH}_{2} \mathrm{CL}_{2}$ | - - | X | X | X | 100 | - | - | X | - | - | - | - | - | - | - | - | X | X | X | A | A |  |  |  |  |  |
| Diesel Fuel | - | - - | 72 | 72 | 100 | 250 | - | 70 | X | 200 | 250 | - | 400 | 250 | 150 | - | 190 | X | X | 100 | A | A |  |  |  |  |  |
| Diethanolamine | - | 1.1 | X | X | - | - | - | 1 | 104 | - | - | - | 100 | X | X |  | - | - | - | 70 |  |  |  |  |  |  |  |
| Diethyl Cellosolve | - | - - | - | - | 80 | 280 | - | - | X | - | 250 | - | - | - | - |  | 200 | X | 100 | 140 |  |  |  |  |  |  |  |
| Diethylether (Ether) | $\left(\mathrm{C}_{2} \mathrm{H}_{5}\right)_{2} \mathrm{O}$ | - - | X | X | 100 | 100 | 73 | - | X | - | 73 | - | 400 | 100 | X | - | X | X | X | X |  |  |  |  |  |  |  |
| Diethyl Ketone | $\mathrm{C}_{2} \mathrm{H}_{5} \mathrm{COC}_{2} \mathrm{H}_{5}$ | - - | X | X | - | - | - | - | X | - | - |  | - | - | X | - | X | - | X | 200 |  |  |  |  |  |  |  |
| Diethyl Oxide (Ether) | $\left(\mathrm{C}_{2} \mathrm{H}_{5}\right)_{2} \mathrm{O}$ | - - | - | - | - | - | - | - | X | - | 73 |  | - | - | - |  | X | X | X | X |  |  |  |  |  |  |  |
| Diethylamine | $\left(\mathrm{C}_{2} \mathrm{H}_{5}\right)_{2} \mathrm{NH}$ | - - | X | X | 100 | 100 | - | - | X | - | 73 | - | 400 | - | - |  | X | 120 | X | X | - |  |  |  |  |  |  |
| Diethylbenzene | $\mathrm{C}_{6} \mathrm{H}_{4}\left(\mathrm{C}_{2} \mathrm{H}_{5}\right)_{2}$ | - - | X | X | X | - | - | - | X | - | - | - | - | - | - |  | 150 | X | X | X | - |  |  |  |  |  |  |
| Diethylene Glycol | - | - - | 140 | 0200 | 180 | 280 | - | - | X | - | - | - | 350 | 200 | 180 | - | 200 | - | 150 | 140 | A | A |  |  |  |  |  |
| Diethylenetriamine | - | - - | - | - | 80 | 100 | - | - | - | - | - | - | 400 | X | X |  | - | - | - | - |  |  |  |  |  |  |  |
| Diglycolic Acid | $\mathrm{O}\left(\mathrm{CH}_{2} \mathrm{COOH}\right)_{2}$ | - - | 140 | 0190 | 100 | 80 | - | - | - | - | 73 | - | 400 | - | - | - | - | - | - | - |  |  |  |  |  |  |  |
| Dimethyl Phthalate | - | - - | X | X | X | 68 | - | - | X | - | 212 | - | - | 100 | 100 | - | 200 | - |  | - |  |  |  |  |  |  |  |
| Disobutyl Ketone | - | - - | X | X | - | 140 | - | - | X | - | - | - | - | - | - | - | X | X | - | 70 |  |  |  |  |  |  |  |
| Diisobutylene | $\mathrm{C}_{8} \mathrm{H}_{16}$ | - | - | - | - | 180 | - | - | - 20 | 200 | - |  | 250 | - | - |  | 140 | X |  | - |  |  |  |  |  |  |  |
| Diisooctyl Phthalate | - | - - | - | - | - | - | - | - | X | 200 | - |  | - | - | - | - | - | - | - | - | - |  |  |  |  |  |  |
| Diisopropyl Ketone | - | - - | - | - | - | 68 | - | - | - | - | 73 |  | 70 | - | - |  | X | 70 | - | - | - |  |  |  |  |  |  |
| Dimethylbenzene | $\mathrm{C}_{6} \mathrm{H}_{4}\left(\mathrm{CH}_{3}\right)_{2}$ | - - | X | X | X | 140 | - | - | X | - | - | - | 250 | - | - | - | 100 | X | X | X |  |  |  |  |  |  |  |
| Dimethyl Ether | $\mathrm{CH}_{3} \mathrm{OCH}_{3}$ | 0.66 | 6 X | X | - | - | - | - | X | - | - |  | - | - | - | - | - | - | X | - |  |  |  |  |  |  |  |
| Dimethylformamide | $\mathrm{HCON}\left(\mathrm{CH}_{3}\right)_{2}$ | 100.95 | 5 X | X | 120 | X | 100 | - | X | - | - |  | 140 | - | - |  | X | - | - | - |  |  |  |  |  |  |  |
| Dimethyl Ketone (see Acetone) | $\mathrm{CH}_{3} \mathrm{COCH}_{3}$ | - - | X | X | - | - | - | - | X | - | - | - | - | - | - | - | X | - | X | X |  |  |  |  |  |  |  |
| Dimethyl Phthalate | $\mathrm{C}_{6} \mathrm{H}_{4}\left(\mathrm{COOCH}_{3}\right)_{2}$ | - - | X | X | 100 | 100 | - | - | X | - | 73 | - | 350 | 100 | 100 | - | 200 | - | X | X | - |  |  |  |  |  |  |
| Dimethylamine | $\left(\mathrm{CH}_{3}\right)_{2} \mathrm{NH}$ | - - | X | X | - | - | - | - | X | - | 73 | - | - | X | X | - | X | X | - | - | - |  |  |  |  |  |  |
| Dioctyl Phthalate | - | - - | X | X | X | 73 | X | X | X | 200 | 73 | - | - | - | - | - | - | - | X | X |  |  |  |  |  |  |  |
| Dioxane | - | - - | X | X X | 73 | X | 73 | - | X |  | 150 | - | 350 | - | - |  | X | - | X | X | - |  |  |  |  | A | A |
| Dioxolane |  | 1.07 | 7 | - | - | - |  | - | - | - | - | - | - | - | - |  | X | X | - | - | - |  |  |  |  | - |  |
| Diphenyl (Dowtherm) | - | 1 | - | - | - | - | - | - | X | 200 | - | - | 350 | 120 | 120 |  | 300 | X | 150 | x | - |  |  |  |  |  |  |
| Diphenyl Ether (See Diphenyl Oxide) | - | - - | - | - | - | - | - | - | - | - | - |  | - | - |  |  |  | - |  | - | - |  |  |  |  |  |  |
| Diphenyl Oxide | $\left(\mathrm{C}_{6} \mathrm{H}_{5}\right)_{2} \mathrm{O}$ | - - | - | - | - | - | - | - | X | - | - | - | - | 120 | - |  | 100 | X | X | X | A |  |  |  |  |  |  |
| Dipropylene Glycol | - | 1.25 | 25140 | 10180 | 120 | 280 | - | - | X | - | - |  | - | 200 | 150 |  | 250 | 210 | 160 | 180 | A |  |  |  |  | - |  |
| Disodium Methylarsonate | - | - | - | - | - | - | - | - | - | - | - | - | - | - |  |  | - | - | - | - | - |  |  |  |  | - |  |
| Disodium Phosphate | - | - - | 140 | 10 180 | 180 | 180 | 140 | 140 | - | - | 300 | - | 350 | - | - |  | 80 | 210 | 80 | 100 | - |  |  |  |  | - |  |
| Distilled Water | HOH | - - | 140 | 10210 | 180 | 250 | 140 | 140 | 176 | - | 300 | - | 350 | 250 | 200 |  | - | 250 | 250 | 180 | - |  |  |  |  | - | - |
| Divinylbenzene | - | - - | X | X X | X | X | - | - | X | - | 73 | - | - | - | - |  | - | - | - | - | - |  |  |  |  | - |  |
| Dolomite | $\mathrm{CaMg}\left(\mathrm{CO}_{3}\right)_{2}$ | - - | - | - | - | - | - | - | - | - | - | - | - | - | - |  | - | - | - | - | - |  |  |  |  | - |  |
| Dowtherm (See Diphenyl) | - | - - | - | - | - | - | - | - | - | - | - | - | - | - | - |  | - | - | - | - | - |  |  |  |  | - | - |
| Dry Cleaning Solvents | - | - - | X | X X | 73 | 250 | X | X | - | - | - | - | 350 | 120 | X |  | 200 | X | X | x | - |  |  |  |  | A | - |
| Epichlorohydrin | - | - - | X | X X | 80 | 220 | - | - | X | 200 | - | - | 350 | - | - |  | X | X | - | x | - |  |  |  |  | A | - |
| Epsom Salts | $\mathrm{MgSO}_{4}$ | - - | 140 | 10200 | 180 | 280 | 140 | 140 | 176 | - | 250 | - | 300 | 270 | 200 | - | 200 | 180 | 160 | 180 | 140 |  |  |  |  | - | - |
| Esters (General) | ${ }^{-}$ | - - | X | X | X | 100 | - | - | - | - | - | - | 350 | 100 | - |  | - | - | - | - | - |  |  |  |  | - | - |
| Ethane | $\mathrm{C}_{2} \mathrm{H}_{6}$ | - - | 73 | 373 | X | 280 | - | - | - | - | - | - | 350 | - | - |  | - | X | - | - | - |  |  |  |  | - | - |
| Ethanol (see Alcohol, Ethyl) | $\mathrm{C}_{2} \mathrm{H}_{5} \mathrm{OH}$ | - - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - |  |  |  |  | - | - |
| Ethanolamine | - | 1.02 | $2 \times$ | X X | X | X | - | - | - | 200 | - | - | 100 | - | - | - | - | 100 | - | 68 | - |  |  |  |  | - | - |
| Ethers | ${ }^{-}$ | - - | X | X X | X | 100 | - | - | - 2 | 200 | - | - | 350 | - | - | - | X | X | X | X | - |  |  |  | A | - | - |
| Ethyl Acetate | $\mathrm{CH}_{3} \mathrm{COOL}_{2} \mathrm{H}_{5}$ | - - | X | X | 100 | 100 | X | X | X | 200 | 121 | - | 350 | 150 | X | - | X | 70 | X | X | A |  |  |  | A | - | - |
| Ethyl Acetoacetate | - | - - | X | X | - | 120 | - | - | X | - | 73 | - | 350 | - | - |  | X | - | - | X | - |  |  |  |  | - | - |
| Ethyl Acrylate | - | - - | X | X X | 73 | 120 | - | - | X | - | 121 | - | 350 | - | - | - | X | - | X | X | - |  |  |  | C | - | - |
| Ethyl Alcohol | $\mathrm{C}_{2} \mathrm{H}_{5} \mathrm{OH}$ | 0.8 | 8140 | 140180 | 180 | 250 | 120 | 140 | X | - | 250 | - | 300 | 180 | 80 |  | 180 | 170 | 70 | 180 | - |  |  |  | A | - | - |
| Ethylbenzene | $\mathrm{C}_{6} \mathrm{H}_{5} \mathrm{C}_{2} \mathrm{H}_{5}$ | - - | X | X | X | 140 | - | - | X | - | - |  | 300 | - | - |  | 70 | X | X | X | - |  |  |  |  | - | - |
| Ethyl Bromide | $\mathrm{C}_{2} \mathrm{H}_{5} \mathrm{BR}$ | - - | X | X X | X | 180 | X | X | X | - | - | - | 350 | - | - | - | - | 70 | 70 | - | - |  |  |  | - | - | - |
| Ethyl Butyrate | $\mathrm{C}_{3} \mathrm{H}_{7} \mathrm{CO}_{2} \mathrm{C}_{2} \mathrm{H}_{5}$ | - - | X | X X | - | - | - | - | X | - | - | - | - | - | - | - | - | - | - | - | - |  |  |  | - | - |  |

## CHEMICAL RESISTANCE GUIDE



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FOR SERVICE, PLEASE CALL 1-800-877-HIPCO

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| CHEMIICAL |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  | TAL <br> ${ }^{\circ}$ $\frac{0}{7}$ 忽 |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Potassium Chromate | $\mathrm{K}_{2} \mathrm{CrO}_{4}$ | 2.7 | 7140 | 180 | 180 | 250 | - | - | - | - | 250 | - | - | - | - | - | 100 | 170 | 70 | 140 | A |  |  |  |  |  |
| Potassium Copper | - | - | - - | - | - | - | - | - |  | - | 250 | - | - |  |  | - | - | - | - | - | - |  |  |  |  |  |
| Cyanide | KCuCN | - - | 140 | 180 | 200 | 250 | - | - | - | - | - |  | 350 | - | - | - | 200 | 140 | - | 140 |  |  |  |  |  |  |
| Potassium Cyanide | KCN | 1.5 | 5140 | 180 | 180 | 250 | - | - | 176 | - | - |  | 350 | 2301 | 180 | - | 190 | 140 | 160 | 180 | C | A |  |  |  |  |
| Potassium Dichromate | $\mathrm{K}_{2} \mathrm{Cr}_{2} \mathrm{O}_{7}$ | 102.7 | 7140 | 180 | 180 | 250 | - | - | 176 | - | 250 | - | 350 | 200 | 200 | - | 180 | 170 | 160 | 180 |  |  |  |  |  |  |
| Potassium Ferricyanide | $\mathrm{K}_{3} \mathrm{Fe}(\mathrm{CN})_{6}$ | - - | 140 | 180 | 140 | 250 | - | - | 176 | - | 250 | - | 350 | 2202 | 200 | - | 140 | 140 | 150 | 70 | - |  |  |  |  |  |
| Potassium Ferrocyanide | $\mathrm{K}_{4} \mathrm{Fe}(\mathrm{CN})_{6}$ | 1.9 | 9140 | 180 | 140 | 250 | - | - | 176 | - | 250 | - | 350 | 220 | 200 | - | 180 | 140 | 200 | 180 | - |  |  |  |  |  |
| Potassium Fluoride | KF | 2.5 | 5140 | 180 | 180 | 250 | - | - | 176 | - | 250 | - | 350 | - | - | - | 180 | 140 | - | 180 |  |  |  |  |  |  |
| Potassium Hydroxide | KOH | 2.0 | 0 | - | - | - | - | - | 176 | - | - | - | - | - | - | - | - | 200 | 160 | 70 | - |  |  |  |  |  |
| (Caustic Potash) | - | - - | - | - | - | - | - | - | - | - | 250 | - | - | - |  | - | - | - | - | - | - |  |  |  |  |  |
| Potassium Hydroxide | KOH | 25 | 140 | 180 | 180 | 140 | - | - | 176 | 200 | - | - | 350 | 1001 | 120 | - | - | 200 | 160 | 100 |  |  |  |  |  |  |
| Potassium Hydroxide | KOH | 10 | 140 | 180 | 100 | X | - | - | 176 | 200 | 250 | - | 350 | - | - | - | - | 200 | 160 | 70 |  |  |  |  |  |  |
| Potassium Hypochlorite | KHOCL | - - | 140 | 180 | 73 | 250 | X | - | - | - | 250 | - | 300 | - | - | - | 100 | 70 | X | X | - |  |  |  |  |  |
| Potassium lodide | KI | 3.12 | 12140 | 180 | 180 | 48 | - | - | 176 | - | - |  | 350 | - | - | - | 100 | 140 | 160 | 80 | - |  |  |  |  |  |
| Potassium Nitrate (Salt Peter) | $\mathrm{KNO}_{3}$ | 2.1 | 1140 | 180 | 150 | 250 | - | - | 176 | - | - | - | 350 | 270 | 200 | - | 180 | 210 | 200 | 180 | - |  |  |  |  |  |
| Potassium Perbotate | - | - - | 140 | 180 | 180 | 250 | - | - | - | - | - | - | 350 | - | - | - | - | - | 70 | 70 | - |  |  |  |  |  |
| Potassium Perchlorate | $\mathrm{KCLO}_{4}$ | 2.5 | 5140 | 180 | 180 | 250 | - | - | - | - | - | - | 350 | - | - | - | 150 | 140 | X | X | - |  |  |  |  | - |
| Potassium Permanganate | $\mathrm{KMNO}_{4}$ | 202.7 | 7140 |  | 120 | 250 | - | - | - | 200 | 73 | - | 350 | X | 150 | - | 150 | 210 | 100 | X | A | A |  |  |  | B |
| Potassium Persulfate | $\mathrm{K}_{2} \mathrm{~S}_{2} \mathrm{O}_{8}$ | 2.5 | 5140 | 180 | 120 | 250 | - | - | - | - | 300 | - | 400 | - 1 | 180 | - | 200 | 210 | 140 | X | A | A |  |  |  |  |
| Potassium Phosphate | $\mathrm{K}_{2} \mathrm{HPO}_{4}$ | - - | - | 180 | - | - | - | - | - | - | 121 | - | 400 | 1801 | 100 | - | 140 | 100 | 100 | 100 | - |  |  |  |  |  |
| Potassium Salts | - | - - | - | - | - | - | - | - | - | - | - |  | - | - | - | - | - | - | - | - | - |  |  |  |  |  |
| Potassium Sulfate | $\mathrm{K}_{2} \mathrm{SO}_{4}$ | 2.7 | 7140 | 180 | 180 | 250 | - | - | 176 | - | - | - | 400 | 250 | 180 | - | 200 | 180 | 140 | 140 | A | A |  |  |  |  |
| Potassium Sulfide | $\mathrm{K}_{2} \mathrm{~S}$ | 1.8 | 8100 | 120 | - | 250 | - | - | - | - | 250 | - | 300 | - | - | - | 100 | - | 70 | 100 | - |  |  |  |  | - |
| Potassium Thiosulfate | $\mathrm{K}_{2} \mathrm{~S}_{2} \mathrm{O}_{3}$ |  | - | - | - | - | - | - | 176 | - | - | - | - | - | - | - | - | - | - |  | - |  |  |  |  |  |
| Propane (Dimethyl- Methane) | $\mathrm{C}_{3} \mathrm{H}_{8}$ | - - | 72 | 72 | 73 | 250 | - | - | X | - | - | - | 300 | 1501 | 100 | - | 300 | X | 70 | 100 | - |  |  |  |  | - |
| Propanol (see Alcohol, Propyl) | - | - - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - |  |  |  |  |  |
| Propargyl Alcohol | $\mathrm{HC}: \mathrm{CCH}_{2} \mathrm{OH}$ | - - | 72 | 72 | 120 | 150 | - | - | - | - | - | - | 350 | - | - | - | 140 | - | X | X | - |  |  |  |  |  |
| Propyl Acetate | $\mathrm{C}_{3} \mathrm{H}_{7} \mathrm{OOCCH}_{3}$ | 0.89 | 9 | - | - | 100 | - | - | X | - | 73 | - | 140 | - | - | - | X | 70 | X | 100 | - |  |  |  |  |  |
| Propyl Alcohol | $\mathrm{CH}_{3} \mathrm{CH}_{2} \mathrm{CH}_{2} \mathrm{OH}$ | 0.8 | 8120 | 160 | 150 | 150 | - | - | X | 2 | 250 | - | 400 | - | - | - | 200 | 140 | 200 | - | - |  |  |  |  |  |
| Propylene | $\mathrm{CH}_{3} \mathrm{CH}: \mathrm{CH}_{2}$ | 0.51 | 51 | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | X | - |  |  |  |  |  |
| Propylene Dichloride | $\mathrm{CH}_{3} \mathrm{CHCLCH}_{2} \mathrm{CL}$ | 1.58 | 8 X | X | X | 150 | - | - | X | - | - | - | 400 | - | - | - | 70 | X | X | 100 | - |  |  |  |  | - |
| Propylene Glycol | $\mathrm{CH}_{3} \mathrm{CHOHCH}_{2} \mathrm{OH}$ | 1.0 | 0 | - | - | 250 | X | 140 | - | - | - | - | 400 | 200 | - | - | 200 | - | 100 | X | - |  |  |  |  |  |
| Pyridine | $\mathrm{N}(\mathrm{CH})_{4} \mathrm{CH}$ | 1.0 | X | X | 73 | X | - | - | X | 200 | - | - | 350 | - | - | - | X | 70 | X | 80 | - |  |  |  |  | - |
| Pyrogallic Acid (Pyrogallol) | $\mathrm{C}_{6} \mathrm{H}_{3}(\mathrm{OH})_{3}$ | 1.47 | 773 | - | - | 150 | - | - | - | - 1 | 121 | - | 350 | - | - | - | 80 | - | 200 | - | - |  |  |  |  |  |
| Quaternary Ammonium | - | - - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - |  |  |  |  |  |
| Salts | - | - - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | A | A |  |  |  | - |
| Rayon Coagulating Bath | - | - - | 140 | 180 | 73 | 73 | X | 140 | - | - | - | - | - | - | - | - | - | - | - | X | - |  |  |  |  | - |
| Rhodan Salts (Thiocyanates) | - | - - | 140 | 140 | 140 | 250 | - | - | - | - | - | - | - | - | - | - | 180 | - | - | - | - |  |  |  |  | - |
| Rosins | - | - - | - | - | - | - | - | - | - | - | - | - | 350 | - | - | - | - | - | - | - | - |  |  |  |  | - |
| Rum | - | - - | 100 | 100 | 100 | - | - | - | - | - | - | - | - | - | - | - | 70 | - | - | - | - |  |  |  |  | - |
| Rust Inhibitors | - | - - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - |  |  |  | - |
| Salad Dressings | - | - - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | A | A |  |  |  | - |
| Salicylaldehyde | $\mathrm{C}_{6} \mathrm{H}_{4} \mathrm{OHCHO}$ | - 1.17 | 7 X | X | - | 140 | - | - | - | - | 73 | - | 200 | - | - | - | - | - | - | - | - |  |  |  |  | - |
| Salicylic Acid | $\mathrm{C}_{6} \mathrm{H}_{4}(\mathrm{OH})(\mathrm{COOH})$ | 1.44 | 4 | - | - | 210 | - | - | - | - | - | - | 250 | - | - | - | 200 | - | - | 68 | A | A |  |  |  | - |
| Saline Solutions (Brine) | - | - - | 140 | 190 | 180 | 250 | 140 | 140 | - | 2 | 250 | - | 400 | 200 | - | - | 280 | 250 | 160 | 180 | - | - |  |  |  | - |
| Salt Brine | - | - - | 140 | 190 | 180 | 250 | 140 | 140 | - | 2 | 250 | - | 400 | 200 | - | - | 280 | 250 | 160 | 180 | A | A |  |  |  | B |
| Sea Water | - | - - | 140 | 190 | 180 | 250 | 140 | 140 | 176 | 2 | 250 | - | 400 | 200 | - | - | 280 | 250 | 160 | 180 | A | A |  |  |  | A |
| Salenic Acid | $\mathrm{H}_{2} \mathrm{SeO}_{4}$ | - 22.6 | . 140 | 190 | 73 | 70 | 70 | 70 | - | - | - | - | 350 | - | - | - | - | - | - | - | - | - |  |  |  | A |
| Sewage | - | - - | 140 | 180 | 180 | 250 | - | - | - | - | - | - | 350 | - | - | - | 180 | 140 | 140 | 150 | A | A |  |  |  |  |
| Shellac Bleached | - | - - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - |  |  |  |  | - |
| Shellac Orange | - | - - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - | - |  |  |  | - |
| Salicic Acid | $\mathrm{SiO}_{2} \mathrm{H}_{2} \mathrm{O}$ | - - | 140 | 180 | 180 | 250 | 140 | 140 | - | - | - | - | 250 | - | - | - | 200 | 140 | 140 | 180 | - | - |  |  |  | - |
| Silicone Oil | - | - - | 140 | 150 | 150 | 250 | - | - | - | - | 73 | - | 350 | - | - | - | 190 | 140 | 70 | 140 | A | A |  |  |  | - |
| Silver Bromide | AgBr | - 6.47 | 7 | - | - | - | 140 | 140 | - | - | - | - | - | - | - | - | - | - | - | - | A | - |  |  | - | - |

## CHEMICAL RESISTANCE GUIDE



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* Caution: Further testing needed, suspect with certain stress levels.

The Teflon included in the tables is PFA or PTFE which are similar in chemical resistance and temperature. For data on FEP Teflon, please call Harrington's technical service department.
NOTE: Recent studies have shown that surfactants and detergents even in trace quantities can adversely affect the performance of certain thermoplastics in applications like sodium hydroxide, e.g. cross-linked polyethylene and CPVC.

MIXED CHEMICALS
Table 6

| CHEMICALS | CONCENTRATION (\%) | PVC* | CPVC* | PP* | PVDF* | TEFLON* | VITON* | EPT ${ }^{*}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Sulfuric Add <br> Chromic Add <br> Sodium Silicon- <br> fluoride | $\begin{aligned} & 0.7 \\ & 250 \mathrm{~g} / \mathrm{l} \end{aligned}$ $1$ | 140 | 176 | - | 248 | 248 | - | - |
| Sulfuric Add Hydrofluoric Acid | $\begin{aligned} & 20 \\ & 10 \end{aligned}$ | 140 | 140 | - | 248 | 248 | 104 | 104 |
| Sulfuric Acid Hydrofluoric Add | $\begin{aligned} & 25 \\ & 15 \end{aligned}$ | 140 | 140 | - | 248 | 248 | - | - |
| Sulfuric Add <br> Nitric Acid <br> Chlorine Gas | $\begin{aligned} & 75 \\ & 5 \\ & \text { Little } \end{aligned}$ | 140 | 176 | 104 | 176 | 248 | - | - |
| Sulfuric Acid Sulfurous Acid | $\begin{aligned} & 75 \\ & 4 \end{aligned}$ | 140 | 176 | 176 | 248 | 248 | 104 | 140 |
| Sulfuric Acid <br> Spelter <br> Manganese Sulfate | $\begin{aligned} & 150 \mathrm{~g} / \mathrm{l} \\ & 80 \\ & 2 \end{aligned}$ | 140 | 176 | 176 | 248 | 248 | 176 | 176 |
| Sodium Sulfide Sulfuric Acid Formaldehyde | $\begin{aligned} & 225 \mathrm{~g} / \mathrm{l} \\ & 225 \mathrm{~g} / \mathrm{l} \\ & 50 \end{aligned}$ | 104 | 176 | 176 | 212 | 212 | 212 | 140 |

Table 6 (cont'd)

| CHEMICALS | CONCENTRATION (\%) | PVC* | CPVC* | PP* | PVDF* | TEFLON* | VITON* | EPT* |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Hydrochloric Acid <br> Allyl Chloride | $36$ <br> 12 PPM | 104 | 104 | 140 | 248 | 248 | 176 | 104 |
| Hydrochloric Acid <br> Benzene | $36$ <br> 54 PPM | 140 | 176 | 176 | 248 | 248 | 140 | 68 |
| Hydrochloric Acid <br> Chlorobenzene | $\begin{gathered} 18 \\ 490 \text { PPM } \end{gathered}$ | 140 | 176 | 176 | 248 | 248 | 140 | 68 |
| Hydrochloric Acid <br> Chlorobenzene | $\begin{gathered} 36 \\ 890 \text { PPM } \end{gathered}$ | 104 | -- | 104 | 212 | 248 | 104 | -- |
| Hydrofluoric Acid Chromium Sulfate Sodium Silicofluoride | $\begin{aligned} & 220 \mathrm{~g} / \mathrm{l} \\ & 1 \mathrm{~g} / \mathrm{l} \\ & 12 \mathrm{~g} / \mathrm{l} \end{aligned}$ | 140 | 176 | -- | 248 | 248 | -- | - |
| Hydrofluoric Acid <br> Sodium Silico- <br> fluoride <br> Oxalic Acid | $350 \mathrm{~g} / \mathrm{l}$ <br> $17 \mathrm{~g} / \mathrm{l}$ <br> $1 \mathrm{~g} / \mathrm{l}$ | 104 | 104 | -- | 248 | 248 | -- | - |
| Hydrochloric Acid <br> Ferrous Chloride | $\begin{aligned} & 35 \\ & 28 \end{aligned}$ | - | -- | - | 248 | 248 | -- | 176 |
| Hydrochloric Acid <br> Hydrofluoric Acid | $\begin{aligned} & 10 \\ & 15 \end{aligned}$ | 140 | 140 | - | 248 | 248 | -- | -- |
| Hydrochloric Acid <br> Hydrofluoric Acid | $\begin{aligned} & 18 \\ & 20 \end{aligned}$ | 140 | 176 | - | 248 | 248 | -- | -- |
| Hydrochloric Acid <br> Nitric Acid | $\begin{aligned} & 20 \\ & 50 \end{aligned}$ | 140 | 140 | -- | 68 | 248 | 248 | -- |
| Hydrochloric Acid <br> Ortho-chlorophenal | $\begin{gathered} 36 \\ 170 \text { PPM } \end{gathered}$ | 140 | 140 | 140 | 248 | 248 | 176 | 104 |
| Hydrochloric Acid <br> Sulfuric Acid | $\begin{aligned} & 36 \mathrm{~g} / \mathrm{l} \\ & 98 \mathrm{~g} / \mathrm{l} \end{aligned}$ | 68 | 68 | - | 176 | 248 | -- | -- |
| Hydrochloric Acid <br> Sulfuric Acid | $20$ $5$ | 140 | 176 | 176 | 248 | 248 | 176 | 176 |
| Hydrochloric Acid <br> Sulfuric Acid | $\begin{aligned} & 36 \\ & 98 \end{aligned}$ | 140 | 176 | 176 | 248 | 248 | -- | -- |
| Hydrofluoric Acid Ammonium Fluoride | $250 \mathrm{~g} / \mathrm{l}$ <br> $8 \mathrm{~g} / \mathrm{l}$ | 140 | 140 | -- | 248 | 248 | -- | -- |

NOTE: * Temperature at ${ }^{\circ} \mathrm{F}$

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MIXED CHEMICALS
Table 6 (cont'd)

| CHEMICALS | CONCENTRATION <br> (\%) | PVC* | CPVC* | PP* | PVDF* | TEFLON* | VITON* | EPT* |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Hydrochloric Acid <br> Ferric Chloride | $\begin{aligned} & 25 \\ & 28 \end{aligned}$ | 140 | 212 | 212 | 248 | 248 | 176 | 176 |
| Hydrochloric Acid <br> Ferrous Chloride | $\begin{aligned} & 20 \\ & 28 \end{aligned}$ | - | - | - | 248 | 248 | 176 | 176 |
| Nitric Acid <br> Hydrofluoric Acid | $15$ $3$ | 140 | 140 | 140 | 248 | 248 | - | -- |
| Nitric Acid <br> Hydrofluoric Acid | $\begin{gathered} 15 \\ 5 \end{gathered}$ | 140 | 104 | 104 | 248 | 248 | 176 | 104 |
| Nitric Acid <br> Hydrofluoric Acid | $\begin{aligned} & 15 \\ & 10 \end{aligned}$ | 140 | 68 | 104 | 248 | 248 | - | - |
| Nitric Acid <br> Hydrofluoric Acid | $15$ $15$ | 140 | 68 | 104 | 248 | 248 | -- | - |
| Nitric Acid <br> Hydrofluoric Acid | $\begin{gathered} 5 \\ 20 \end{gathered}$ | 140 | 176 | - | 248 | 248 | - | - |
| Nitric Acid <br> Sulfuric Acid | $\begin{gathered} 50 \\ 100 \mathrm{~g} \\ 50 \\ 100 \mathrm{~g} \\ \hline \end{gathered}$ | 68 | 68 | 68 | 248 | 248 | - | -- |
| Sulfuric Acid <br> Chromic Acid | $\begin{aligned} & 2 \\ & 1 \end{aligned}$ | 140 | 176 | 68 | 248 | 248 | 104 | 68 |
| Sulfuric Acid <br> Chromic Acid | $\begin{aligned} & 10 \\ & 10 \end{aligned}$ | 104 | 104 | -- | 248 | 248 | 104 | 68 |
| Sulfuric Acid <br> Chromic Acid | $\begin{array}{r} 10 \\ 25 \end{array}$ | 104 | 104 | -- | 248 | 248 | 68 | - |
| Sulfuric Acid <br> Chromic Acid | $\begin{gathered} 4 \mathrm{~g} / \mathrm{l} \\ 400 \mathrm{~g} / \mathrm{l} \end{gathered}$ | 140 | 140 | -- | 248 | 248 | - | - |
| Sulfuric Acid <br> Chromic Acid <br> Phosphoric Acid | 15 <br> 5 <br> 80 | 140 | 176 | -- | 248 | 248 | 140 | 104 |
| Sulfuric Acid <br> Chromic Acid <br> Water | $\begin{gathered} 2 \\ 10 \\ 80 \end{gathered}$ | 140 | 176 | - | 248 | 248 | 104 | - |

NOTE: *Temperature at ${ }^{\circ} \mathrm{F}$

## TABLE 7

Table 7

| MATERIAL |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| STEEL Gr. B | 7.86 | -- | 60,000 | 290 | - | 32 | -- | . 33 |
| ALUMINUM 3003 | 2.73 | -- | 16,000 | 100 | -- | 20 | -- | . 33 |
| COPPER | 8.94 | -- | 30,000 | 170 | -- | 43 | -- | -- |
| (PVC) POLYVINYL CHLORIDE TYPE 1 | 1.38 | . 05 | 7,940 | 4.2 | 14,500 | . 65 | 9,600 | . $35-38$ |
| (CPVC) CHLORINATED POLYVINYL CHLORIDE | 1.55 | . 05 | 8,400 | 4.2 | 15,800 | 3.0 | $\begin{aligned} & 9,000- \\ & 22,000 \end{aligned}$ | . $35-38$ |
| (PP) POLYPROPYLENE NON PPFR | . 905 | . 02 | 5,000 | 1.7-2.5 | 7,000 | 1.3 |  | . $38-.40$ |
| (PPFR) POLYPROPYLENE FLAME RETARDANT |  |  |  |  | 7,000 |  | $8,000$ |  |
| (PROLINE) POLYPROPYLENE/ POLYBUTYLENE COPOLYMER | . 905 | . 02 | 5,800 | 1.1 | 2,900 | 4.7 | 7,000 | .34-4.0 |
| (RYTON) POLYPHYLENE SULFIDE 40\% GLASS FIBER REINFORCED | 1.6 | . 05 | 19,500 | 1.6 | 29,000 | 1.4 | 21,000 | -- |
| (PVDF) POLYVINYLIDENE FLUORIDE | $\begin{aligned} & 1.75- \\ & 1.78 \end{aligned}$ | . 04 | $\begin{aligned} & 5,000- \\ & 7,000 \end{aligned}$ | 2.13 | 12,180 | 2.8 | 10,500 | . 38 |
| POLYETHYLENE <br> LD PE - LOW DENSITY | . 925 | . 01 | 2,300 | .14-38 | - | 9.0 | - | -- |
| HALAR | 1.69 | . 04 | 4,500 | 2.40 | --- | No Break | --- | 0.3-0.4 |
| DURAPLUS (ABS) | 1.06 | --- | 5,500 | 2.40 | --- | 8.5 | 6,150 | --- |
| HD PE - HIGH DENSITY | . 965 | . 01 | 4,500 | .6-1.8 | 7,000 | 4.0 | 3,600 | -- |
| XL PE - CROSS LINK PE | 1.28 | . 02 | 3,000 | - | 5,000 | 2.0 | 4,000 | -- |
| TEFLON (PTFE) POLYTETRAFLUORETHYLENE | 2.14 | . 02 | 2,600 | 1.0 | 81,000 | No Break | 3,500 | -- |
| TEFLON (PFA) PERFLUOROALKOXY | 2.2 | 0.0 | $\begin{aligned} & 2,000- \\ & 5,000 \end{aligned}$ | . 58 | - | 3.0 | 1,700 | - |
| TEFLON (FEP) FLUORINATED ETHYLENE PROPYLENE | 2.1 | 0.0 | $\begin{aligned} & 2,700- \\ & 3,100 \end{aligned}$ | . 50 | - | No Break | 2,200 | -- |
| EPOXY FIBERGLASS | 1.6 | .05-. 20 | 10,000 | 1.35 | 10,000 | 1.0 | 25,000 | - |
| VINYLESTER FIBERGLASS | 1.6 | . 02 | 10,500 | 1.4 | 15,600 | 2.5 | 18,000 | - |
| POLYSULFONE | 1.24 | 0.3 | 10,200 | 3.6 | 15,400 | 1.3 | - | -- |

## RELATIVE PROPERTIES

TABLE 8

Table 8

| MATERIAL | ๗̛ <br> 岳 <br> Ȯㅡㄴ <br> 둥 <br> 3 O |  |  |  |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| STEEL Gr. B | 20,000 | . 06 | 1/16" | $750^{\circ}$ | -- | -- | 290 | -- | - | - |  | $\begin{aligned} & \hline \boldsymbol{山} \\ & \mathbf{O} \\ & \sum_{\infty}^{0} \end{aligned}$ |
| ALUMINUM 3003 | - | -- | 5/32" | $400^{\circ}$ | -- | - | 1450 | -- | - | - |  |  |
| COPPER | - | - | 1/8" | $400^{\circ}$ | -- | - | 2610 | - | - | - |  |  |
| (PVC) POLYVINYL CHLORIDE TYPE 1 | 2,000 | 3.0 | $1 / 3^{\prime \prime}$ | $140^{\circ}$ | 173 | 160 | 1.2 | * | 43 | V-0 | 15 | 850 |
| (CPVC) CHLORINATED POLYVINYL CHLORIDE | 2,000 | 3.8 | 1/2" | $210^{\circ}$ | 238 | 221 | . 95 | * | 60 | V-0 | 10 | 295 |
| (PP) POLYPROPYLENE NON PPFR | 725-800 | 5.0 | 5/8" | $180^{\circ}$ | 220 | 125-140 | 1.2 |  | 17 | V-2 | 119 | 791 |
| (PPFR) POLYPROPYLENE FLAME RETARDANT |  |  |  |  |  |  |  | Slow |  |  | 115 | 412 |
| (PROLINE) POLYPROPYLENE/ POLYBUTYLENE COPOLYMER | 800 | 8.33 | 1" | $200^{\circ}$ | -- | - | 1.2 | Slow | -- | V-2 | 110 | 515 |
| (RYTON) POLYPHYLENE SULFIDE 40\% GLASS FIBER REINFORCED | - | - | 1/2" | $200^{\circ}$ | - | 485 | 1.5-0.91 | * | - | V-0 | - | - |
| (PVDF) POLYVINYLIDENE FLUORIDE | 2,300 | 6.6-8.7 | 1" | $280^{\circ}$ | 284 | 195 | 1.32 | * | 44 | V-0 | - | - |
| POLYETHYLENE LD PE - LOW DENSITY | -- | $\begin{aligned} & 10.0- \\ & 22.0 \end{aligned}$ | 1-1/4" | $140^{\circ}$ | 100-121 | 90-105 | 2.3 | Very Slow | - | V-1 | - | - |
| HD PE - HIGH DENSITY | -- | 7.2 | 7/8" | $160^{\circ}$ | 175-196 | 110-130 | 3.5 | VerySlow | 226 | V-1 | -- | - |
| XL PE - CROSS LINK PE | -- | -- | -- | $180^{\circ}$ | 180 | 120 | - | Slow | - | V-1 | - | - |
| TEFLON (PTFE) POLYTETRAFLUORETHYLENE | -- | 10.0 | 2/3" | $500^{\circ}$ | 250 | -- | 6.0 | * | 95 | V-0 | - | - |
| (PFA) PERFLUOROALKOXY | -- | 7.6 | 0.9" | $500^{\circ}$ | -- | - | 1.3 | * | 95 | V-0 | - | - |
| TEFLON (FEP) FLUORINATED ETHYLENE PROPYLENE | -- | 8.3-10.5 | 1/3" | $300^{\circ}$ | 158 | -- | 6.0 | * | 95 | V-0 | - | - |
| EPOXY FIBERGLASS | -- | 4.0-10.0 | 1/10" | $300^{\circ}$ | -- | 300 | 1.7 |  | -- | V-0 | - | -- |
| VINYLESTER FIBERGLASS | -- | -- | 1/10" | $200^{\circ}$ | -- | 200 | 2.0 | * | - | V-0 | - | - |
| POLYSULFONE | - | 3.1 | - | $300^{\circ}$ | - | 345 | 1.8 |  | 33 | V-0 | - | - |
| HALAR | -- | 4.4-9.2 | 1" | $300^{\circ}$ | 195 | 151 | 1.07 | * | 60 | V-O | - | - |
| DURAPLUS (ABS) | - | 5.6 | 5/8" | $176{ }^{\circ}$ | 194 | 223 | 1.7 | * | - |  |  |  |

* Self-Extinguishing


## SYSTEMS ENGINEERING DATA FOR THERMOPLASTIC PIPING

## INTRODUCTION

In the engineering of thermoplastic piping systems to comply with the Uniform Building Code, Uniform Fire Code, Uniform Mechanical Code, and Uniform Plumbing Code, it is necessary to have not only a working knowledge of piping design, but also an awareness of the unique properties of thermoplastics. The selection of the proper piping material is based upon $\underline{\mathbf{S}} \mathbf{T} \underline{\mathbf{A}} \underline{\mathrm{P}}$ :

1. Size
2. Temperature
3. Application
4. Media
5. Pressure

Size of piping is determined by carrying capacity of the piping selected. Carrying capacity and friction loss are discussed on pages 50-58.

Temperature refers to the temperature of the liquid being piped and is the most critical factor in selecting plastic piping. Refer to the Continuous Resistance To Heat column in the Relative Properties tables on pages 40-41 to select an appropriate plastic material. Temperature of media must not exceed continuous resistance to heat. Temperature also refers to the maximum and minimum media or climactic conditions which the piping will experience. These maximum and minimum temperatures directly affect chemical resistance, expansion and contraction, support spacing, pressure rating, and most other physical properties of the piping material. These different considerations are discussed separately later.

Application asks what the pipe is being designed to do. Above or below ground, in a building or outside, drainage or pumped, in a floor trench or in a ceiling, high purity, short-/or long-term application, FDA requirement, flame and smoke spread required, and double containment required are all questions which should be answered.

Media is the liquid being contained and its concentration. Specific gravity, percent of suspended solids, and crystallization should be determined. Consult with the chemical resistance chart on pages 18-38 to make a selection based on liquid, concentration, and temperature.

Pressure is the pressure within the piping. Pressure is directly affected by temperature, wall thickness, diameter, and method of joining being employed. Refer to the Temperature-Pressure charts on pages 44-48 to conform the desired installation. Pressure inside the pipe may be less than the surrounding soil or atmospheres such as in vacuum or deep burial applications, and collapse pressure of piping must be determined from tables on page 49.

If more than one material meets the STAMP criteria, cost of material, personal preferences, and additional safety considerations are used to determine the right material for the service.

After piping, fitting, valve, and gasket materials are chosen for the service being considered, engineering the piping system begins with calculations for:

1. Pressure Ratings
2. Water Hammer
3. Temperature-Pressure Relationships
4. Flow Rate and Friction Loss Characteristics
5. Dimensional and Weight Data

It must be noted that storage, handling, and use of gaseous, liquid, and solid hazardous production material (HPM), as defined and discussed in the Uniform Building Code and Uniform Fire Code, requires very careful consideration and compliance to provide piping systems that comply with the law and are safe to man and the environment.

## PRESSURE RATINGS OF THERMOPLASTICS

## DETERMINING PRESSURE-STRESS-PIPE RELATIONSHIPS

## ISO EQUATION

Circumferential stress is the largest stress present in any pressurized piping system. It is this factor that determines the pressure that a section of pipe can withstand. The relationship of stress, pressure, and pipe dimensions is described by the ISO (International Standardization Organization) equation. In various forms this equation is:

$$
\begin{aligned}
& P=\frac{2 S}{R-1}=\frac{2 S t}{D_{0}-t} \quad \frac{2 S}{P}=\frac{D_{0}}{t}-1 \\
& \frac{2 S}{P}=R-1 \quad S=\frac{P(R-1)}{2}
\end{aligned}
$$

Where:
P = Internal Pressure, psi
S = Circumferential Stress, psi
$\mathrm{t}=$ Wall Thickness, in.
$D_{0}=$ Outside Pipe Diameter, in.
$R=D_{0} / t$

## LONG-TERM STRENGTH

To determine the long-term strength of thermoplastic pipe, lengths of pipe are capped at both ends (see Figure 5) and subjected to various internal pressure, to produce circumferential stresses that will produce failure in from 10 to 10,000 hours. The test is run according to ASTM D-1598 - Standard Test for Time-to-Failure of Plastic Pipe Under Long-Term Hydrostatic Pressure.

The resulting failure points are used in a statistical analysis (outlined in ASTM D-2837, see page 6) to determine the characteristics of the regression curve that represents the stress/time-to-failure relationship for the particular thermoplastic pipe compound under test.

## SYSTEMS ENGINEERING DATA FOR THERMOPLASTIC PIPING

This curve is represented by the equation:

$$
\log =a+b \log S
$$

## Where:

a and b are constants describing the slope and intercept of the curve, and T and S are time-to-failure and stress, respectively.

The regression curve may be plotted on a log-log paper, as shown in Figure 6, and extrapolated from 10,000 to 100,000 hours (11.4 years). The stress at 100,000 hours is known as the Long-Term Hydrostatic Strength (LTHS) for that particular thermoplastic compound. From this (LTHS) the Hydrostatic Design Stress (HDS) is determined by applying the service factor multiplier, as described below.

FIGURE 5

LONG-TERM STRENGTH TEST PER ASTM D1598


Pipe test specimen per ASTM D1598 for "Time-to-Failure of Plastic Pipe Under Long-Term Hydrostatic Pressure"

FIGURE 6

REGRESSION CURVE - STRESS/TIME-TO-FAILURE FOR PVC TYPE 1


## SERVICE FACTOR

The Hydrostatic Stress Committee of the Plastics Pipe Institure (PPI) has determined that a service (design) factor of one-half the hydrostatic design basis would provide an adequate safety margin for use with water to ensure useful plastic-pipe service for a long period of time. While not stated in the standards, it is generally understood within the industry that this "long period of time" is a minimum of 50 years.


## SYSTEMS ENGINEERING DATA FOR THERMOPLASTIC PIPING

The standards for plastic pipe, using the 0.5 service factor, require that the pressure rating of the pipe be based upon this hydrostatic design stress, again calculated with the ISO equation.

While early experience indicated that this service factor, or multiplier, of 0.5 provided adequate safety for many if not most uses, some experts felt that a more conservative service factor of 0.4 would better compensate for water hammer pressure surges, as well as for slight manufacturing variations and damage suffered during installation.

The PPI has issued a policy statement officially recommending this 0.4 service factor. This is equivalent to recommending that the pressure rating of the pipe should equal 1.25 times the system design pressure for any particular installation. Based upon this policy, many thousands of miles of thermoplastic pipe have been installed in the United States without failure.

It is best to consider the actual surge conditions, as outlined later in this section. In addition, substantial reductions in working pressure are advisable when handling aggressive chemical solutions and in high-temperature service.

Numerical relationships for service factors and design stresses of PVC are shown in Table 9.

## Table 9

SERVICE FACTORS AND HYDROSTATIC DESIGN STRESS
(Hydrostatic design basis equals 4000 PSI)

| SERVICE FACTOR | HDS |
| :---: | :---: |
| 0.5 | $2000 \mathrm{psi}(13.8 \mathrm{MPa})$ |
| 0.4 | $1600 \mathrm{psi}(11 \mathrm{MPa})$ |

Material: PVC Type I \& CPVC

## TEMPERATURE-PRESSURE AND MODULUS RELATIONSHIPS

## Temperature Derating

Pressure ratings for thermoplastic pipe are generally determined in a water medium at room temperature $\left(73^{\circ} \mathrm{F}\right)$. As the system temperature increases, the thermoplastic pipe becomes more ductile, increases in impact strength, and decreases in tensile strength. The pressure ratings of thermoplastic pipe must therefore be decreased accordingly.

The effects of temperature have been exhaustively studied and correction (derating) factors developed for each thermoplastic piping compound. To determine the maximum operating pressure at any given temperature, multiply the pressure rating at ambient shown in Table 10 by the temperature correction factor for that material shown in Table 11. Attention must also be given to the pressure rating of the joining technique, i.e., threaded system normally reduces pressure capabilities substantially.

Table 10
MAXIMUM OPERATING PRESSURES (PSI) AT 73
BASED UPON A SERVICE FACTOR OF . 5

| NOMINAL SIZE | PVC \& CPVC SCHEDULE 40 SOLVENT WELD | PVC \& CPVC SCHEDULE 80 |  | POLYPROPYLENE*(PP) |  |  | POLYVINYLIDENE FLUORIDE (PVDF) |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  |  |  | PPRO-SEAL | $\begin{aligned} & \hline \text { PROLINE } \\ & \text { SDR } \end{aligned}$ |  | SUPER PROLINE SDR |  | SCHEDULE 80 |  |
|  |  | SOLVENT WELD | THREADED |  |  |  | SOCKET |  |
|  |  |  |  |  | 11 | 32 |  |  | 11 | 32 | FUSION | THREADED |
| 1/4 | 780 | 1130 | -- | N/A | N/A | N/A | N/A | N/A | N/A | N/A |
| 3/8 | 620 | 920 | -- | N/A | N/A | N/A | N/A | N/A | N/A | N/A |
| 1/2 | 600 | 850 | 420 | 150 | 160 | 45 | 230 | N/A | 975 | 290 |
| 3/4 | 480 | 690 | 340 | 150 | 160 | 45 | 230 | N/A | 790 | 235 |
| 1 | 450 | 630 | 320 | 150 | 160 | 45 | 230 | N/A | 725 | 215 |
| 1-1/4 | 370 | 520 | 260 | N/A | 160 | 45 | 230 | N/A | 600 | 180 |
| 1-1/2 | 330 | 471 | 240 | 150 | 160 | 45 | 230 | N/A | 540 | 160 |
| 2 | 280 | 400 | 200 | 150 | 160 | 45 | 230 | N/A | 465 | 135 |
| 2-1/2 | 300 | 425 | 210** | N/A | 160 | 45 | N/A | 160 | N/A | N/R |
| 3 | 260 | 375 | 190** | N/A | 160 | 45 | N/A | 160 | 430 | N/R |
| 4 | 220 | 324 | 160** | N/A | 160 | 45 | N/A | 160 | 370 | N/R |
| 6 | 180 | 280 | N/R | N/A | 160 |  | N/A | 160 | N/A | N/R |
| 8 | 160 | 250 | N/R | N/A | 160 |  | N/A | 160 | N/A | N/A |
| 10 | 140 | 230 | $N / R$ | N/A | 160 |  | N/A | 160 | N/A | N/A |
| 12 | 130 | 230 | N/R | N/A | 160 |  | N/A | 160 | N/A | N/A |

[^1]FOR SERVICE, PLEASE CALL 1-800-877-HIPCO

## SYSTEMS ENGINEERING DATA <br> FOR THERMOPLASTIC PIPING

## Table 11

TEMPERATURE CORRECTION FACTORS

| OPERATING TEMPERATURES ${ }^{\circ} \mathrm{F}$ | FACTORS |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  |  | POLYPROPYLENE |  | POLYVINYLIDENE FLUORIDE |  |
|  | PVC | CPVC | PPRO-SEAL NATURAL | PROLINE | SUPER PROLINE | SCHEDULE 80 |
| 73 | 1.00 | 1.00 | 1.00 | 1.00 | 1.00 | 1.00 |
| 80 | . 88 | . 94 | . 93 |  | . 95 | . 93 |
| 90 | . 75 | . 86 | . 83 |  | . 87 | . 87 |
| 100 | . 62 | . 78 | . 74 | . 64 | . 80 | . 82 |
| 110 | . 50 | . 71 | . 66 |  |  | . 76 |
| 120 | . 40 | . 64 | . 58 |  | . 68 | . 71 |
| 130 | . 30 | . 57 | . 51 |  |  | . 65 |
| 140 | . 22 | . 50 | . 40 | . 40 | . 58 | . 61 |
| 150 | N/R | . 43 | . 38 |  |  | . 57 |
| 160 | $\mathrm{N} / \mathrm{R}$ | . 37 | . 35 |  | . 49 | . 54 |
| 180 | N/R | . 25 | . 23 | . 28 | . 42 | . 47 |
| 200 | N/R | . 18 | . 14 | . 10 | . 36 | . 41 |
| 210 | N/R | . 16 | . 10 | N/R |  | . 38 |
| 220 | N/R | N/R | N/R | N/R |  | . 35 |
| 240 | N/R | N/R | N/R | N/R | . 25 |  |
| 250 | N/R | N/R | N/R | N/R |  | . 28 |
| 280 | N/R | N/R | N/R | N/R | . 18 | . 22 |

## FLANGED SYSTEMS

Table 12- MAXIMUM OPERATING PRESSURE
(PSI) FOR FLANGED SYSTEMS

## FLANGED SYSTEMS

Maximum pressure for any flanged system is 150 psi. At elevated temperatures the pressure capability of a flanged system must be derated as shown in Table 12.

Design Pressure - Pressure rating at $73^{\circ} \mathrm{F}$ x temperature correction factor.

| OPERATING TEMPERATURE ${ }^{\circ} \mathrm{F}$ | PVC* | CPVC* | PP** | PVDF |
| :---: | :---: | :---: | :---: | :---: |
| 100 | 150 | 150 | 150 | 150 |
| 110 | 135 | 145 | 140 | 150 |
| 120 | 110 | 135 | 130 | 150 |
| 130 | 75 | 125 | 118 | 150 |
| 140 | 50 | 110 | 105 | 150 |
| 150 | N/R | 100 | 93 | 140 |
| 160 | $N / R$ | 90 | 80 | 133 |
| 170 | N/R | 80 | 70 | 125 |
| 180 | N/R | 70 | 50 | 115 |
| 190 | N/R | 60 | N/R | 106 |
| 200 | N/R | 50 | N/R | 97 |
| 210 | $N / R$ | 40 | N/R | 90 |
| 240 | N/R | N/R | N/R | 60 |
| 280 | N/R | N/R | N/R | 25 |

N/R = Not Recommended

* PVC and CPVC flanges sizes 2-1/2 through 3-/and 4-inch threaded must be backwelded for the above pressure capability to be applicable.
** Threaded PP flanges size $1 / 2$ through 4 inch as well as the 6 " back welded socket flange are not recommended for pressure applications (drainage only).


# PRESSURE RATINGS <br> PVC LARGE DIAMETER FABRICATED FITTINGS AT $73^{\circ} \mathrm{F}$ 10" $\mathrm{THROUGH} 24 "$ 

The following tables indicate the working pressure recommended by the manufacturer for large diameter PVC fabricated fittings. These fittings are not generally recommended for high pressure applications. Pressure capabilities are not necessarily the same as the rating of the pipe from which they are fabricated. Be sure pressure to temperature correction factors are considered when system design calls for temperatures above $73^{\circ} \mathrm{F}$.

Water hammer and surge pressure are the two most critical elements in large-diameter design. Keeping velocities below 5 feet per second and working pressures to these guidelines will give years of trouble-free service.

Table 13
$90^{\circ}$ ELBOW

| NOMINAL <br> SIZE <br> (IN.) | SCHEDULE 40 |  | SCHEDULE 80 |  |
| :---: | :---: | :---: | :---: | :---: |
|  | WT. <br> (LBS.) | PSI <br> RTG | WT. <br> (LBS.) | PSI <br> RTG |
| $\mathbf{1 0}$ | 22 | 140 | 34 | 230 |
| $\mathbf{1 2}$ | 30 | 130 | 50 | 230 |
| $\mathbf{1 4}$ | 40 | 130 | 70 | 220 |
| $\mathbf{1 6}$ | 56 | 130 | 100 | 220 |
| $\mathbf{1 8}$ | 90 | 100 | 93 | 125 |
| $\mathbf{2 0}$ | 121 | 50 | 125 | 75 |
| $\mathbf{2 4}$ | 202 | 50 | 208 | 75 |

Table 14
COUPLING

| NOMINAL <br> SIZE <br> (IN.) | SCHEDULE 40 |  | SCHEDULE 80 |  |
| :---: | :---: | :---: | :---: | :---: |
|  | $\begin{gathered} \text { WT. } \\ \text { (LBS.) } \end{gathered}$ | $\begin{gathered} \hline \text { PSI } \\ \text { RTG } \end{gathered}$ | $\begin{gathered} \text { WT. } \\ \text { (LBS.) } \end{gathered}$ | $\begin{gathered} \text { PSI } \\ \text { RTG } \end{gathered}$ |
| 10 | 9 | 140 | 15 | 230 |
| 12 | 15 | 130 | 23 | 230 |
| 14 | 19 | 130 | 33 | 220 |
| 16 | 29 | 130 | 54 | 220 |
| 18 | 33 | 100 | 53 | 160 |
| 20 | 45 | 50 | 74 | 75 |
| 24 | 77 | 50 | 110 | 75 |

Table 15
TEE

| NOMINAL <br> SIZE <br> (IN.) | SCHEDULE 40 |  | SCHEDULE 80 |  |
| :---: | :---: | :---: | :---: | :---: |
|  | WT. <br> (LBS.) | PSI <br> RTG | WT. <br> (LBS.) | PSI <br> RTG |
| $\mathbf{1 0}$ | 28 | 140 | 44 | 230 |
| $\mathbf{1 2}$ | 41 | 130 | 69 | 230 |
| $\mathbf{1 4}$ | 54 | 130 | 95 | 220 |
| $\mathbf{1 6}$ | 78 | 130 | 139 | 220 |
| $\mathbf{1 8}$ | 115 | 100 | 156 | 160 |
| $\mathbf{2 0}$ | 153 | 50 | 204 | 75 |
| $\mathbf{2 4}$ | 231 | 50 | 338 | 75 |

Table 16
$45^{\circ}$ ELBOW

| NOMINAL <br> SIZE <br> (IN.) | SCHEDULE 40 |  | SCHEDULE 80 |  |
| :---: | :---: | :---: | :---: | :---: |
|  | WT. <br> (LBS.) | PSI <br> RTG | WT. <br> (LBS.) | PSI <br> RTG |
| $\mathbf{1 0}$ | 15 | 140 | 24 | 230 |
| $\mathbf{1 2}$ | 21 | 130 | 36 | 230 |
| $\mathbf{1 4}$ | 30 | 130 | 52 | 220 |
| $\mathbf{1 6}$ | 42 | 130 | 75 | 220 |
| $\mathbf{1 8}$ | 47 | 100 | 71 | 160 |
| $\mathbf{2 0}$ | 62 | 50 | 95 | 75 |
| $\mathbf{2 4}$ | 103 | 50 | 159 | 75 |

Table 17
REDUCING TEE

| NOMINAL <br> SIZE <br> (IN.) | SCHEDULE 40 |  | SCHEDULE 80 |  |
| :---: | :---: | :---: | :---: | :---: |
|  | WT. <br> (LBS.) | PSI <br> RTG | WT. <br> (LBS.) | PSI <br> RTG |
| $\mathbf{1 0 \times 8}$ | 23 | 140 | 32 | 230 |
| $\mathbf{1 0 \times 6}$ | 21 | 140 | 30 | 230 |
| $\mathbf{1 0 \times 4}$ | 18 | 140 | 28 | 230 |
| $\mathbf{1 2 \times 1 0}$ | 32 | 130 | 55 | 220 |
| $\mathbf{1 2 \times 8}$ | 30 | 130 | 49 | 220 |
| $\mathbf{1 2 \times 6}$ | 26 | 130 | 47 | 220 |
| $\mathbf{1 2 \times 4}$ | 24 | 130 | 45 | 220 |
| $\mathbf{1 4 \times 1 2}$ | 46 | 100 | 70 | 160 |
| $\mathbf{1 4 \times 1 0}$ | 39 | 100 | 66 | 160 |
| $\mathbf{1 4 \times 8}$ | 36 | 100 | 59 | 160 |
| $\mathbf{1 6 \times 1 4}$ | 68 | 100 | 118 | 160 |
| $\mathbf{1 6 \times 1 2}$ | 61 | 100 | 105 | 160 |
| $\mathbf{1 6 \times 1 0}$ | 54 | 100 | 90 | 160 |
| $\mathbf{1 6 \times 8}$ | 49 | 100 | 82 | 160 |
| $\mathbf{1 8 \times 1 6}$ | 82 | 100 | 132 | 160 |
| $\mathbf{1 8 \times 1 4}$ | 73 | 100 | 116 | 160 |
| $\mathbf{2 0 \times 1 8}$ | 104 | 75 | 160 | 100 |
| $\mathbf{2 0 \times 1 6}$ | 98 | 75 | 156 | 100 |
| $\mathbf{2 4 \times 2 0}$ | 162 | 50 | 251 | 75 |

## PRESSURE RATINGS

## PVC LARGE DIAMETER FABRICATED FITTINGS AT $73^{\circ} \mathrm{F}$ 10" THROUGH 24"

Table 18
CONCENTRIC REDUCER

| NOMINAL <br> SIZE <br> (IN.) | SCHEDULE 40 |  |
| :---: | :---: | :---: |
|  | WT. <br> (LBS.) | PSI <br> RTG |
| $\mathbf{1 0 \times 6}$ | 9 | 140 |
| $\mathbf{1 0 \times 4}$ | 22 | 140 |
| $\mathbf{1 2 \times 1 0}$ | 23 | 140 |
| $\mathbf{1 2 \times 8}$ | 15 | 130 |
| $\mathbf{1 2 \times 6}$ | 31 | 130 |
| $\mathbf{1 4 \times 1 \mathbf { 2 }}$ | 34 | 130 |
| $\mathbf{1 4 \times 1 0}$ | 23 | 130 |
| $\mathbf{1 6 \times 1 4}$ | 36 | 130 |
| $\mathbf{1 6 \times 1 2}$ | 32 | 130 |
| $\mathbf{1 8 \times 1 6}$ | 46 | 130 |
| $\mathbf{2 0 \times 1 8}$ | 45 | 100 |
| $\mathbf{2 4 \times 2 0}$ | 87 | 100 |

## Table 19

BUSHING (SPIG x SOC)

| NOMINAL <br> SIZE <br> (IN.) | SCHEDULE 40 |  |
| :---: | :---: | :---: |
|  | $\begin{gathered} \text { WT. } \\ \text { (LBS.) } \end{gathered}$ | $\begin{aligned} & \text { PSI } \\ & \text { RTG } \end{aligned}$ |
| $10 \times 8$ | 11 | 140 |
| $10 \times 6$ | 16 | 140 |
| $10 \times 4$ | 20 | 140 |
| $12 \times 10$ | 15 | 130 |
| $12 \times 8$ | 26 | 130 |
| $12 \times 6$ | 31 | 130 |
| $14 \times 12$ | 24 | 100 |
| $16 \times 14$ | 22 | 100 |
| $16 \times 12$ | 46 | 100 |
| $16 \times 10$ | 61 | 100 |
| $16 \times 8$ | 72 | 100 |
| $18 \times 16$ | 30 | 100 |
| $20 \times 18$ | 33 | 100 |
| $24 \times 20$ | 55 | 100 |

Table 21
MALE ADAPTOR

| NOMINAL <br> SIZE <br> (IN.) | SCHEDULE <br> W0 <br> (LBS.) | PSI <br> RTG |
| :---: | :---: | :---: |
|  | 6 | 25 |
| $\mathbf{8}$ | 7 | 25 |
| $\mathbf{1 0}$ | 8 | 25 |
| $\mathbf{1 2}$ | 14 | 25 |

Table 20
EXTENDED BUSHING

| NOMINAL <br> SIZE <br> (IN.) | $\|c\|$ | WT. <br> (LBS.) |
| :---: | :---: | :---: |
|  | 11 | PSI <br> RTG |
| $\mathbf{1 2 \times 1 0}$ | 19 | 140 |
| $\mathbf{1 4 \times 1 2}$ | 28 | 130 |
| $\mathbf{1 6 \times 1 4}$ | 38 | 130 |

Table 22
FEMALE ADAPTOR

| NOMINAL <br> SIZE <br> (IN.) | WT. <br> (LBS.) | PSI <br> RTG |
| :---: | :---: | :---: |
|  | 6 | 25 |
| $\mathbf{8}$ | 7 | 25 |
| $\mathbf{1 0}$ | 8 | 25 |
| $\mathbf{1 2}$ | 14 | 25 |

# PRESSURE RATINGS PVC LARGE DIAMETER FABRICATED FITTINGS AT $73^{\circ} \mathrm{F}$ 

Table 23
CROSS

| NOMINAL <br> SIZE <br> (IN.) | SCHEDULE 40 |  | SCHEDULE 80 |  |
| :---: | :---: | :---: | :---: | :---: |
|  | WT. <br> (LBS.) | PSI <br> RTG | WT. <br> (LBS.) | PSI <br> RTG |
| $\mathbf{3}$ | 2 | 240 | 5 | 260 |
| $\mathbf{4}$ | 3 | 220 | 7 | 240 |
| $\mathbf{6}$ | 13 | 160 | 22 | 240 |
| $\mathbf{8}$ | 22 | 160 | 30 | 240 |
| $\mathbf{1 0}$ | 38 | 140 | 62 | 230 |
| $\mathbf{1 2}$ | 58 | 130 | 95 | 230 |
| $\mathbf{1 4}$ | 74 | 130 | 129 | 220 |
| $\mathbf{1 6}$ | 107 | 130 | 190 | 220 |
| $\mathbf{1 8}$ | 117 | 100 | 185 | 160 |
| $\mathbf{2 0}$ | 158 | 50 | 247 | 75 |
| $\mathbf{2 4}$ | 267 | 50 | 413 | 75 |

Table 24
FLANGE (BLIND)

| NOMINAL <br> SIZE <br> (IN.) | SCHEDULE 40 |  | SCHEDULE 80 |  |
| :---: | :---: | :---: | :---: | :---: |
|  | WT. |  |  |  |
| (LBS.) | PSI <br> RTG | WT. <br> (LBS.) | PSI <br> RTG |  |
| $\mathbf{1 0}$ | 16 | 25 | 32 | 75 |
| $\mathbf{1 2}$ | 21 | 25 | 42 | 75 |
| $\mathbf{1 4}$ | 26 | 25 | 52 | 75 |
| $\mathbf{1 6}$ | 33 | 25 | 66 | 75 |
| $\mathbf{1 8}$ | 36 | 25 | 72 | 75 |
| $\mathbf{2 0}$ | 44 | 25 | 88 | 75 |
| $\mathbf{2 4}$ | 57 | 25 | 114 | 75 |

Table 25
CAP

| NOMINAL <br> SIZE <br> (IN.) | SCHEDULE 40 |  | SCHEDULE 80 |  |
| :---: | :---: | :---: | :---: | :---: |
|  | WT. <br> (LBS.) | PSI <br> RTG | WT. <br> (LBS.) | PSI <br> RTG |
| $\mathbf{1 0}$ | 5 | 140 | 14 | 230 |
| $\mathbf{1 2}$ | 7 | 130 | 17 | 230 |
| $\mathbf{1 4}$ | 23 | 130 | 35 | 220 |
| $\mathbf{1 6}$ | 32 | 130 | 49 | 220 |
| $\mathbf{1 8}$ | 38 | 100 | 54 | 160 |
| $\mathbf{2 0}$ | 49 | 50 | 69 | 75 |
| $\mathbf{2 4}$ | 74 | 50 | 108 | 75 |

Table 26
IPS PIPE DIMENSION TABLE

| NOMINAL <br> PIPE SIZE <br> (IN.) |  | SCHEDULE 40 |  | SCHEDULE 80 |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  | O.D. | AVERAGE I.D. | MINIMUM WALL | AVERAGE I.D. | MINIMUM WALL |
| $\mathbf{1}$ | 1.315 | 1.033 | .133 | .935 | .179 |
| $\mathbf{1 - 1 / 4}$ | 1.660 | 1.364 | .140 | 1.256 | .191 |
| $\mathbf{1 - 1 / 2}$ | 1.900 | 1.592 | .145 | 1.476 | .200 |
| $\mathbf{2}$ | 2.375 | 2.049 | .154 | 1.913 | .218 |
| $\mathbf{3}$ | 3.500 | 3.042 | .216 | 2.864 | .300 |
| $\mathbf{4}$ | 4.500 | 3.998 | .237 | 3.786 | .337 |
| $\mathbf{5}$ | 5.563 | 5.047 | .258 | 4.813 | .375 |
| $\mathbf{6}$ | 6.625 | 6.013 | .280 | 5.709 | .432 |
| $\mathbf{8}$ | 8.625 | 7.943 | .322 | 7.565 | .500 |
| $\mathbf{1 0}$ | 10.750 | 9.976 | .365 | 9.492 | .593 |
| $\mathbf{1 2}$ | 12.750 | 11.890 | .406 | 11.294 | .687 |
| $\mathbf{1 4}$ | 14.000 | 13.126 | .437 | 12.440 | .780 |
| $\mathbf{1 6}$ | 16.000 | 15.000 | .500 | 14.200 | .900 |
| $\boldsymbol{1 8}$ | 18.000 | CLASS 100 | 17.120 |  |  |
| $\mathbf{2 0}$ | 20.000 | 19.022 | .440 | 16.614 | CLASS 160 |
| $\mathbf{2 4}$ | 24.000 | 22.870 | .489 | 18.460 | .693 |

# SYSTEMS ENGINEERING DATA FOR THERMOPLASTIC PIPING 

Table 27
MODULUS OF ELASTICITY (x10s) PSI VS. TEMPERATURE

| MATERIAL | TEMPERATURE, ${ }^{\circ} \mathrm{F}$ |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | 73 | 90 | 110 | 140 | 170 | 200 | 210 | 250 | 280 |
| PVC | 4.20 | 3.85 | 3.40 | 3.00 | -- | - | -- | -- | - |
| CPVC | 4.23 | 4.10 | 3.70 | 3.27 | 2.93 | 2.40 | 2.26 | -- | -- |
| PP Fuseal | 2.00 | 1.30 | . 097 | . 074 | 0.61 | 0.55 | 0.53 | -- | -- |
| PP Pressure | 1.50 | 1.34 | 1.18 | 0.96 | 0.77 | 0.59 | 0.53 | - | -- |
| PVDF | 2.13 | 1.66 | 1.37 | 1.04 | 0.80 | 0.61 | 0.55 | 0.37 | 0.29 |

## EXTERNAL PRESSURES - COLLAPSE RATING

Thermoplastic pipe is frequently specified for situations where uniform external pressures are applied to the pipe, such as in underwater applications. In these applications, the collapse rating of the pipe determines the maximum permissible pressure differential between external and internal pressures. The basic formulas for collapsing external pressure applied uniformly to a long pipe are:

1. For thick wall pipe where collapse is caused by compression and failure of the pipe material:

$$
\mathrm{Pc}=\frac{o}{2 \mathrm{Do}^{2}} \quad\left(\mathrm{Do}^{2}-\mathrm{Di}^{2}\right)
$$

2. For thin wall pipe where collapse is caused by elastic instability of the pipe wall:

$$
\mathrm{Pc}=\frac{2 \mathrm{cE}}{1-v^{2}}\left(\frac{\mathrm{t}}{\mathrm{Dm}}\right)^{3}
$$

Where:
Pc = Collapse Pressure (external minus internal pressure), psi
o = Compressive Strength, psi
E = Modulus of elasticity, psi
$v=$ Poisson's Ratio
Do = Outside Pipe Diameter, in.
Dm = Mean Pipe Diameter, in.
Di = Inside Pipe Diameter, in.
$\mathrm{t}=$ Wall Thickness, in.
c = Out-of-Roundness Factor, Approximately 0.66
Choice of Formula - By using formula 2 on thick-wall pipe, an excessively large pressure will be obtained. It is therefore necessary to calculate, for a given pipe size, the collapse pressure using both formulas and use the lower value as a guide to safe working pressure. For short-term loading conditions, the values of $\mathrm{E}, o$ and $v$ from the relative properties charts shown on pages 40-41 will yield reasonable results. See individual materials charts for short-term collapse pressures at $73^{\circ} \mathrm{F}$. For long-term loading conditions, appropriate long-term data should be used.

## SHORT-TERM COLLAPSE PRESSURE

Thermoplastic pipe is often used for suction lines or in applications where external pressures are applied to the pipe, such as in heat exchangers, or underwater loading conditions. The differential pressure rating of the pipe between the internal and external pressures is detemined by derating collapse pressures of the pipe. The differential pressure rating of the pipe is determined by derating the short-term collapse pressures shown in Table 28.

Collapse pressures must be adjusted for temperatures other than for room temperature. The pressure temperature correction chart (Table 28) used to adjust pipe pressure ratings may be used for this purpose. (See note below table).
Table 28
SHORT-TERM COLLAPSE PRESSURE IN PSI AT $73^{\circ} \mathrm{F}$

| 1/2 | 3/4 | 1 | \|1-1/4| | 1-1/2 | 2 | 3 | 4 | 6 | 8 | 10 | 12 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| SCHEDULE 40 PVC |  |  |  |  |  |  |  |  |  |  |  |
| 2095 | 1108 | 900 | 494 | 356 | 211 | 180 | 109 | 54 | 39 | 27 | 22 |
| SCHEDULE 80 PVC |  |  |  |  |  |  |  |  |  |  |  |
| 2772 | 2403 | 2258 | 1389 | 927 | 632 | 521 | 335 | 215 | 147 | 126 | 117 |
| SCHEDULE 80 CPVC - IPS |  |  |  |  |  |  |  |  |  |  |  |
| 2772 | 2403 | 2258 | 1389 | 927 | 632 | 521 | 335 | 215 | 147 | 126 | 117 |
| SCHEDULE 80 PRESSURE POLYPROPYLENE - IPS |  |  |  |  |  |  |  |  |  |  |  |
| 1011 | 876 | 823 | 612 | 412 | 278 | 229 | 147 | 94 | 65 | 55 | 51 |
| SCHEDULE 80 PVDF - IPS |  |  |  |  |  |  |  |  |  |  |  |
| 2936 | 1576 | 1205 | 680 | 464 | 309 | 255 | 164 | 105 | 72 | 61 | 57 |
| PROLINE PRO 150 |  |  |  |  |  |  |  |  |  |  |  |
| 40 | 40 | 40 | 40 | 40 | 40 | 40 | 40 | 40 | 40 | 40 | 40 |
| PROLINE PRO 45 |  |  |  |  |  |  |  |  |  |  |  |
| 1.6 | 1.6 | 1.6 | 1.6 | 1.6 | 1.6 | 1.6 | 1.6 | 1.6 | 1.6 | 1.6 | 1.6 |
| SUPER PROLINE |  |  |  |  |  |  |  |  |  |  |  |
| 202 | 99 | 92 | 44 | 41 | 22 | 5.8 | 5.8 | 5.8 | 5.8 | 5.8 | 5.8 |

NOTE: These are short-term ratings; long-term ratings should be reduced by $1 / 3$ to $1 / 2$ of the short-term ratings.

Vacuum Service - All sizes of Schedule 80 thermoplastic pipe are suitable for vacuum service up to $140^{\circ} \mathrm{F}$ and 30 inches of mercury. Solvent-cemented joints are recommended for vacuum applications when using PVC. Schedule 40 PVC will handle full vacuum up to 24 " diameter.

Laboratory tests have been conducted on Schedule 80 PVC pipe to determine performance under vacuum at temperatures above recommended operating conditions. Pipe sizes under 6 inches show no deformation at temperatures to $170^{\circ} \mathrm{F}$ and 27 inches of mercury vacuum.

The 6 inch pipe showed slight deformation at $165^{\circ} \mathrm{F}$, and 20 inches of mercury. Above this temperature, failure occurred due to thread deformation.

CARRYING CAPACITY AND FRICTION LOSS FOR SCHEDULE 80 THERMOPLASTIC PIPE
(Independent variables: Gallons per minute and nominal pipe size O.D.
Dependent variables: Velocity, friction head and pressure drop per 100 feet of pipe, interior smooth .)


CARRYING CAPACITY AND FRICTION LOSS FOR SCHEDULE 40 THERMOPLASTIC PIPE
(Independent variables: Gallons per minute and nominal pipe size O.D.
Dependent variables: Velocity, friction head and pressure drop per 100 feet of pipe, interior smooth .)


CARRYING CAPACITY AND FRICTION LOSS FOR 315 PSI AND SDR 13.5 THERMOPLASTIC PIPE
(Independent variables: Gallons per minute and nominal pipe size O.D.
Dependent variables: Velocity, friction head and pressure drop per 100 feet of pipe, interior smooth .)


CARRYING CAPACITY AND FRICTION LOSS FOR 200 PSI AND SDR 21 THERMOPLASTIC PIPE
(Independent variables: Gallons per minute and nominal pipe size O.D.
Dependent variables: Velocity, friction head and pressure drop per 100 feet of pipe, interior smooth .)


## CARRYING CAPACITY AND FRICTION LOSS 160 PSI AND SDR 26 THERMOPLASTIC PIPE

(Independent variables: Gallons per minute and nominal pipe size O.D.
Dependent variables: Velocity, friction head and pressure drop per 100 feet of pipe, interior smooth .)


TABLE 34


TABLE 35


TABLE 36


TABLE 37


## SLOPE OF HORIZONTAL DRAINAGE PIPING

Horizontal drains are designated to flow at half full capacity under uniform flow conditions so as to prevent the generation of positive pressure fluctuations. A minimum of $1 / 4^{\prime \prime}$ per foot should be provided for 3 " pipe and smaller, $1 / 8^{\prime \prime}$ per foot for 4 " through $6^{\prime \prime}$, and $1 / 16^{\prime \prime}$ per foot for $8^{\prime \prime}$ and larger. These minimum slopes are required to maintain a velocity of flow greater than 2 feet per second for scouring action. Table 41 gives the approximate velocities and discharge rated for given slopes and diameters of horizontal drains based on modified Manning Formula for $1 / 2$ full pipe and $n=0.015$. The valves for $R, R$ $2 / 3, A, S, S 1 / 2$ and $n$ are from Tables 38, $39 \& 40$.

\[

\]

Table 38

| PIPE <br> SIZE <br> (IN.) | $\mathbf{R}=\frac{\mathbf{D}}{\mathbf{4}}$ <br> FEET | $\mathbf{R}^{2 / 3}$ | A-CROSS-SECTIONAL <br> AREA FOR FULL FLOW <br> SQ. FT. | A - CROSS-SECTIONAL <br> AREA FOR HALF FULL FLOW <br> SQ. FT. |
| :---: | :---: | :---: | :---: | :---: |
| $\mathbf{1 - 1 / 2}$ | 0.0335 | 0.1040 | 0.01412 | 0.00706 |
| $\mathbf{2}$ | 0.0417 | 0.1200 | 0.02180 | 0.01090 |
| $\mathbf{2 - 1 / 2}$ | 0.0521 | 0.1396 | 0.03408 | 0.01704 |
| $\mathbf{3}$ | 0.0625 | 0.1570 | 0.04910 | 0.02455 |
| $\mathbf{4}$ | 0.0833 | 0.1910 | 0.08730 | 0.04365 |
| $\mathbf{5}$ | 0.1040 | 0.2210 | 0.13640 | 0.06820 |
| $\mathbf{6}$ | 0.1250 | 0.2500 | 0.19640 | 0.09820 |
| $\mathbf{8}$ | 0.1670 | 0.3030 | 0.34920 | 0.17460 |
| $\mathbf{1 0}$ | 0.2080 | 0.3510 | 0.54540 | 0.27270 |
| $\mathbf{1 2}$ | 0.2500 | 0.3970 | 0.78540 | 0.39270 |
| $\mathbf{1 4}$ | 0.3125 | 0.4610 | 1.22700 | 0.61350 |

Table 39 VALUES OF S AND S ${ }^{1 / 2}$.

| SLOPE <br> INCHES <br> PER FOOT | FOOT PER FOOT | $\mathbf{S}^{1 / 2}$ |
| :---: | :---: | :---: |
| $\mathbf{1 / 8}$ | 0.0104 | 0.102 |
| $\mathbf{1 / 4}$ | 0.0208 | 0.144 |
| $\mathbf{1 / 2}$ | 0.0416 | 0.204 |

Table 40 VALUES OF $\mathbf{n}$.

| PIPE SIZE | $\mathbf{n}$ |
| :---: | :---: |
| $\mathbf{1 - 1 / 2 "}$ | 0.012 |
| 2" through 3" | 0.013 |
| 4" | 0.014 |
| 5" and 6" | 0.015 |
| 8" and larger | 0.016 |

## Table 41 APPROXIMATE DISCHARGE RATES AND VELOCITIES IN SLOPING DRAINS

FLOWING HALF FULL DISCHARGE RATE AND VELOCITY

| ACTUAL INSIDE DIAMETER OF PIPE INCHES | $\begin{aligned} & \text { 1/16 IN./FT. } \\ & \text { SLOPE } \end{aligned}$ |  | $\begin{aligned} & \text { 1/8 IN./FT. } \\ & \text { SLOPE } \end{aligned}$ |  | $\begin{aligned} & \text { 1/4 IN./FT. } \\ & \text { SLOPE } \end{aligned}$ |  | $\begin{aligned} & \text { 1/2 IN./FT. } \\ & \text { SLOPE } \end{aligned}$ |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | DISCHARGE GPM | $\begin{gathered} \text { VELOCITY } \\ \text { FPS } \end{gathered}$ | DISCHARGE GPM | $\begin{gathered} \text { VELOCITY } \\ \text { FPS } \end{gathered}$ | $\begin{aligned} & \text { DISCHARGE } \\ & \text { GPM } \end{aligned}$ | $\begin{aligned} & \text { VELOCITY } \\ & \text { FPS } \end{aligned}$ | $\begin{aligned} & \text { DISCHARGE } \\ & \text { GPM } \end{aligned}$ | $\begin{gathered} \text { VELOCITY } \\ \text { FPS } \end{gathered}$ |
| 1-1/4 | - | - | - | - | - | - | 3.40 | 1.78 |
| 1-3/8 | - | - | - | - | 3.13 | 1.34 | 4.44 | 1.90 |
| 1-1/2 | - | - | - | - | 3.91 | 1.42 | 5.53 | 2.01 |
| 1-5/8 | - | - | - | - | 4.81 | 1.50 | 6.80 | 2.12 |
| 2 | - | - | - | - | 8.42 | 1.72 | 11.9 | 2.43 |
| 2-1/2 | - | - | 10.8 | 1.41 | 15.3 | 1.99 | 21.6 | 2.82 |
| 3 | - | - | 17.6 | 1.59 | 24.8 | 2.25 | 35.1 | 3.19 |
| 4 | 26.70 | 1.36 | 37.8 | 1.93 | 53.4 | 2.73 | 75.5 | 3.86 |
| 5 | 48.3 | 1.58 | 68.3 | 2.23 | 96.6 | 3.16 | 137. | 4.47 |
| 6 | 78.5 | 1.78 | 111. | 2.52 | 157. | 3.57 | 222. | 5.04 |
| 8 | 170. | 2.17 | 240. | 3.07 | 340. | 4.34 | 480. | 6.13 |
| 10 | 308. | 2.52 | 436. | 3.56 | 616. | 5.04 | 872. | 7.12 |
| 12 | 500. | 2.83 | 707. | 4.01 | 999. | 5.67 | 1413. | 8.02 |

## SYSTEMS ENGINEERING DATA FOR THERMOPLASTIC PIPING

WATER HAMMER
Surge pressures due to water hammer are a major factor contributing to pipe failure in liquid transmission systems. A column of moving fluid within a pipeline, owing to its mass and velocity, contains stored energy. Since liquids are essentially incompressible, this energy cannot be absorbed by the fluid when a valve is suddenly closed.
The result is a high momentary pressure surge, usually called water hammer. The five factors that determine the severity of water hammer are:

1. Velocity (The primary factor in excessive water hammer: see discussion of "Velocity " and "Safety Factor" on page 62).
2. Modulus of elasticity of material of which the pipe is made.
3. Inside diameter of pipe.
4. Wall thickness of pipe.
5. Valve closing time.

Maximum pressure surges caused by water hammer can be calculated by using the equation below. This surge pressure should be added to the existing line pressure to arrive at a maximum operating pressure figure.

$$
P s=V\left(\frac{E t 3960}{E t+3 \times 10^{5} D i}\right)^{1 / 2}
$$

Where:
Ps = Surge Pressure. in psi
$\mathrm{V}=$ Liquid Velocity, in ft. per sec.
Di = Inside Diameter of Pipe, in.
$\mathrm{E}=$ Modulus of Elasticity of Pipe Material, psi
$\mathrm{t}=$ Wall Thickness of Pipe, in.
Calculated surge pressure, which assumes instantaneous valve closure, can be calculated for any material using the values for E (Modulus of Elasticity) found in the properties chart, pages 40-41. Here are the most commonly used surge pressure tables for IPS pipe sizes.

Table 42 - SURGE PRESSURE, Ps IN PSI AT $73^{\circ} \mathrm{F}$

| WATER VELOCITY (FT/SEC) | NOMINAL PIPE SIZE |  |  |  |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | 1/2 | 3/4 | 1 | 1-1/4 | 1-1/2 | 2 | 3 | 4 | 6 | 8 | 10 | 12 |

SCHEDULE 40 PVC \& CPVC

| 1 | 27.9 | 25.3 | 24.4 | 22.2 | 21.1 | 19.3 | 18.9 | 17.4 | 15.5 | 14.6 | 13.9 | 13.4 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 2 | 55.8 | 50.6 | 48.8 | 44.4 | 42.2 | 38.6 | 37.8 | 34.8 | 31.0 | 29.2 | 27.8 | 26.8 |
| 3 | 83.7 | 75.9 | 73.2 | 66.6 | 63.3 | 57.9 | 56.7 | 52.2 | 46.5 | 43.8 | 41.7 | 40.2 |
| 4 | 111.6 | 101.2 | 97.6 | 88.8 | 84.4 | 77.2 | 75.6 | 69.6 | 62.0 | 58.4 | 55.6 | 53.6 |
| 5 | 139.5 | 126.5 | 122.0 | 111.0 | 105.5 | 96.5 | 94.5 | 87.0 | 77.5 | 73.0 | 69.5 | 67.0 |
| 6 | 167.4 | 151.8 | 146.4 | 133.2 | 126.6 | 115.8 | 113.4 | 104.4 | 93.0 | 87.6 | 83.4 | 80.4 |

SCHEDULE 80 PVC \& CPVC

| 1 | 32.9 | 29.9 | 28.7 | 26.2 | 25.0 | 23.2 | 22.4 | 20.9 | 19.4 | 18.3 | 17.3 | 17.6 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 2 | 65.6 | 59.8 | 57.4 | 52.4 | 50.0 | 46.4 | 44.8 | 41.8 | 38.8 | 36.6 | 35.6 | 35.2 |
| 3 | 98.7 | 89.7 | 86.7 | 78.6 | 75.0 | 69.6 | 67.2 | 62.7 | 58.2 | 59.9 | 53.4 | 52.8 |
| 4 | 131.6 | 119.6 | 114.8 | 104.8 | 107.0 | 92.8 | 89.6 | 83.6 | 77.6 | 73.2 | 71.2 | 70.4 |
| 5 | 164.5 | 149.5 | 143.5 | 131.0 | 125.0 | 116.0 | 112.0 | 104.5 | 97.0 | 91.5 | 89.0 | 88.0 |
| 6 | 197.4 | 179.4 | 172.2 | 157.2 | 150.0 | 133.2 | 134.4 | 125.4 | 116.4 | 109.8 | 106.8 | 105.6 |

SCHEDULE 80 POYLPROPYLENE

| 1 | 23.5 | 20.9 | 20.0 | 18.1 | 17.1 | 15.9 | 15.2 | 14.1 | 13.1 | 12.2 | 11.9 | 11.8 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 2 | 47.0 | 41.8 | 40.0 | 36.2 | 34.2 | 31.6 | 30.4 | 28.2 | 26.2 | 24.4 | 23,8 | 23.6 |
| 3 | 70.5 | 62.7 | 60.0 | 54.3 | 51.3 | 47.4 | 45.6 | 42.3 | 39.3 | 36.6 | 35.7 | 35.4 |
| 4 | 94.0 | 83.6 | 80.0 | 72.4 | 68.4 | 63.2 | 60.8 | 56.4 | 52.4 | 48.8 | 47.6 | 47.2 |
| 5 | 117.5 | 104.5 | 100.0 | 90.5 | 85.5 | 79.0 | 76.0 | 70.5 | 65.5 | 61.0 | 59.5 | 59.0 |
| 6 | 141.0 | 125.4 | 120.0 | 108.6 | 102.6 | 94.8 | 91.2 | 84.6 | 78.6 | 73.2 | 71.4 | 70.8 |

## SCHEDULE 80 PVDF

| 1 | 25.2 | 22.6 | 21.6 | 19.5 | 18.5 | 17.1 | 16.5 | 15.3 | 14.2 | 13.3 | 12.9 | 12.8 |
| ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: |
| 2 | 50.4 | 45.2 | 43.2 | 39.0 | 37.0 | 34.2 | 33.0 | 30.6 | 28.9 | 26.6 | 25.8 | 25.6 |
| 3 | 75.6 | 67.8 | 64.8 | 58.5 | 55.5 | 51.3 | 49.5 | 45.9 | 42.6 | 39.9 | 38.7 | 38.4 |
| 4 | 100.8 | 90.4 | 86.4 | 78.0 | 74.0 | 68.4 | 66.0 | 61.2 | 56.8 | 53.2 | 51.6 | 51.2 |
| 5 | 126.0 | 118.0 | 108.0 | 97.5 | 92.5 | 86.5 | 82.5 | 76.5 | 71.0 | 66.5 | 64.5 | 64.0 |
| 6 | 151.2 | 135.6 | 129.6 | 117.0 | 11.0 | 102.6 | 99.0 | 91.8 | 85.2 | 79.8 | 77.4 | 76.8 |

## SUPER PROLINE

| 1 | 22.3 | 19.8 | 19.6 | 17.4 | 17.1 | 15.5 | 18.4 | 12.6 | 12.5 | 12.4 | 12.4 |
| :--- | ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: |
| 2 | 44.5 | 39.7 | 39.1 | 34.7 | 34.2 | 30.9 | 24.8 | 25.2 | 24.9 | 24.8 | 24.9 |
| 3 | 66.8 | 59.5 | 58.7 | 52.1 | 51.4 | 46.4 | 37.2 | 37.7 | 37.4 | 37.2 | 37.3 |
| 4 | 89.1 | 79.4 | 78.3 | 69.5 | 68.5 | 61.8 | 49.7 | 50.3 | 49.9 | 49.6 | 49.8 |
| 5 | 111.3 | 99.2 | 97.9 | 86.9 | 85.6 | 77.3 | 62.1 | 62.9 | 62.3 | 62.0 | 62.2 |
| 6 | 133.6 | 119.0 | 117.4 | 104.2 | 102.7 | 92.8 | 74.5 | 75.5 | 74.8 | 74.4 | 74.6 |

## PROLINE PRO 150

| 1 | 15.3 | 14.1 | 12.9 | 12.6 | 12.8 | 12.8 | 12.7 | 12.7 | 12.8 | 12.7 | 12.7 |
| :--- | :--- | :--- | :--- | :--- | :--- | :--- | :--- | :--- | :--- | :--- | :--- |
| 2 | 30.7 | 28.2 | 25.9 | 25.3 | 25.6 | 25.6 | 25.5 | 25.4 | 25.5 | 25.5 | 25.5 |
| 3 | 46.0 | 42.3 | 38.8 | 37.9 | 38.4 | 38.4 | 38.2 | 38.2 | 38.3 | 38.2 | 38.2 |
| 4 | 61.4 | 56.4 | 51.8 | 50.5 | 51.2 | 51.2 | 51.0 | 50.9 | 51.0 | 50.9 | 51.0 |
| 5 | 76.7 | 70.5 | 64.7 | 63.2 | 64.0 | 64.0 | 63.7 | 63.6 | 63.8 | 63.7 | 63.7 |
| 6 | 92.1 | 84.6 | 77.6 | 75.8 | 76.8 | 76.8 | 76.5 | 76.3 | 76.5 | 76.4 | 76.5 |

## PROLINE PRO 45

| 1 | - | - | - | - | - | 7.1 | 7.0 | 7.1 | 7.1 | 7.0 | 7.1 | 7.1 |
| :--- | :--- | :--- | :--- | :--- | :--- | ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: |
| 2 | - | - | - | - | - | 14.2 | 14.1 | 14.3 | 14.2 | 14.1 | 14.1 | 14.1 |
| 3 | - | - | - | - | - | 21.3 | 21.1 | 21.4 | 21.2 | 21.1 | 21.2 | 21.1 |
| 4 | - | - | - | - | - | 28.4 | 28.1 | 28.6 | 28.3 | 28.2 | 28.2 | 28.2 |
| 5 | - | - | - | - | - | 35.5 | 35.2 | 35.7 | 35.4 | 35.2 | 35.3 | 35.3 |
| 6 | - | - | - | - | - | 42.5 | 42.3 | 42.8 | 42.5 | 42.2 | 42.4 | 42.3 |

NOTE: For sizes larger than 12", call Harrington's Technical Services Group.

## SYSTEMS ENGINEERING DATA FOR THERMOPLASTIC PIPING

## WATER HAMMER (continued)

However, to keep water hammer pressures within reasonable limits, it is common practice to design valves for closure times considerably greater than 2L/C.

Where:

$$
\mathrm{T}_{\mathrm{C}}>2 \mathrm{~L}
$$

$\mathrm{T}_{\mathrm{C}}=$ Valve Closure time, sec.
$L^{C}=$ Length of Pipe run, ft .
C = Sonic Velocity of the Pressure Wave $=4720 \mathrm{ft} . \mathrm{sec}$.

Another formula which closely predicts water hammer effects is:

$$
p=a \frac{w}{144 g}
$$

which is based on the elastic wave theory. In this text, we have further simplified the equation to:

$$
\mathrm{p}=\mathrm{Cv}
$$

Where $p=$ maximum surge pressure, psi
$\mathrm{v}=$ fluid velocity in feet per second
$\mathrm{C}=$ surge wave constant for water at $73^{\circ} \mathrm{F}$
It should be noted that the surge pressure (water hammer) calculated here is a maximum pressure rise for any fluid velocity, such as would be expected from the instant closing of a valve. It would therefore yield a somewhat conservative figure for use with slow closing actuated valves, etc.

For fluids heavier than water, the following correction should be made to the surge wave constant C .

$$
\mathrm{C}^{1}=\frac{(\mathrm{S} \cdot \mathrm{G} .-1) \mathrm{C}+\mathrm{C}}{2}
$$

Where $\mathrm{C}^{1}=$ Corrected Surge Wave Constant
S.G. $=$ Specific Gravity or Liquid

For example, for a liquid with a specific gravity of 1.2 in 2" Schedule 80 PVC pipe, from Table $43=24.2$

$$
\begin{aligned}
& \mathrm{C}^{1}=\frac{(1.2-1)}{2}(24.2)+24.2 \\
& \mathrm{C}^{1}=2.42+24.2 \\
& \mathrm{C}^{1}=26.6
\end{aligned}
$$

Table 43 - Surge Wave Correction for Specific Gravity

| $\begin{aligned} & \text { PIPE } \\ & \text { SIZE } \\ & \text { (IN.) } \end{aligned}$ | PVCSCH 40 SCH 80 |  | CPVCSCH 40 SCH 80 |  | $\begin{aligned} & \text { POLY- } \\ & \text { PROPYLENE } \\ & \text { SCH } 80 \\ & \hline \end{aligned}$ | KYNAR (PVDF) SCH 80 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 1/4 | 31.3 | 34.7 | 33.2 | 37.3 | -- | - |
| 3/8 | 29.3 | 32.7 | 31.0 | 34.7 | - | -- |
| 1/2 | 28.7 | 31.7 | 30.3 | 33.7 | 25.9 | 28.3 |
| 3/4 | 26.3 | 29.8 | 27.8 | 31.6 | 23.1 | 25.2 |
| 1 | 25.7 | 29.2 | 27.0 | 30.7 | 21.7 | 24.0 |
| 1-1/4 | 23.2 | 27.0 | 24.5 | 28.6 | 19.8 | - |
| 1-1/2 | 22.0 | 25.8 | 23.2 | 27.3 | 18.8 | 20.6 |
| 2 | 20.2 | 24.2 | 21.3 | 25.3 | 17.3 | 19.0 |
| 2-1/2 | 21.1 | 24.7 | 22.2 | 26.0 | - |  |
| 3 | 19.5 | 23.2 | 20.6 | 24.5 | 16.6 |  |
| 4 | 17.8 | 21.8 | 18.8 | 22.9 | 15.4 |  |
| 6 | 15.7 | 20.2 | 16.8 | 21.3 |  |  |
| 8 | 14.8 | 18.8 | 15.8 | 19.8 |  |  |
| 10 | 14.0 | 18.3 | 15.1 | 19.3 |  |  |
| 12 | 13.7 | 18.0 | 14.7 | 19.2 |  |  |
| 14 | 13.4 | 17.9 | 14.4 | 19.2 |  |  |

Proper design when laying out a piping system will eliminate the possibility of water hammer damage.

The following suggestions will help in avoiding problems:

1) In a plastic piping system, a fluid velocity not exceeding $5 \mathrm{ft} / \mathrm{sec}$. will minimize water hammer effects, even with quickly closing valves, such as solenoid valves.
2) Using actuated valves which have a specific closing time will eliminate the possibility of someone inadvertently slamming a valve open or closed too quickly. With pneumatic and air-spring actuators, it may be necessary to place a valve in the air line to slow down the valve operation cycle.
3) If possible, when starting a pump, partially close the valve in the discharge line to minimize the volume of liquid which is rapidly accelerating through the system. Once the pump is up to speed and the line completely full, the valve may be opened.
4) A check valve installed near a pump in the discharge line will keep the line full and help prevent excessive water hammer during pump start-up.

## VELOCITY

Thermoplastic piping systems have been installed that have successfully handled water velocities in excess of 10 feet per second. Thermoplastic pipe is not subject to erosion caused by high velocities and turbulent flow, and in this respect is superior to metal piping systems, particularly where corrosive or chemically agressive fluids are involved. The Plastics Pipe Institute has issued the following policy statement on water velocity:

The maximum safe water velocity in a themoplastic piping system depends on the specific details of the system and the operating conditions. In general, 5 feet per second is considered to be safe. Higher velocities may be used in cases where the operating characteristics of valves and pumps are known so that sudden changes in flow velocity can be controlled. The total pressure in the system at any time (operating plus surge or water hammer) should not exceed 150 percent of the pressure rating of the system.

## SAFETY FACTOR

As the duration of pressure surges due to water hammer is extremely short - seconds, or more likely, fractions of a second - in determining the safety factor the maximum fiber stress due to total internal pressure must be compared to some very short-term strength value. Referring to Figure 6, shown on page 43, it will be seen that the failure stress for very short time periods is very high when compared to the hydrostatic design stress.

The calculation of safety factor may thus be based very conservatively on the 20 -second strength value given in Figure 6 , shown on page 43-8470 psi for PVC Type 1.

A sample calculation is shown below, based upon the listed criteria:

```
Pipe = 1-1/4" Schedule }80\mathrm{ PVC
    O.D. = 1.660: Wall = 0.191
    HDS = 2000 psi
```

The calculated surge pressure for $1-1 / 4$ " Schedule 80 PVC pipe at a velocity of $1 \mathrm{ft} / \mathrm{sec}$ is $26.2 \mathrm{psi} / \mathrm{ft} / \mathrm{sec}$.

## SYSTEMS ENGINEERING DATA FOR THERMOPLASTIC PIPING

Water Velocity = 5 feet per second
Static Pressure in System = 300 psi
Total System Pressure = Static Pressure + Surge Pressure: $\mathrm{Pt}=\mathrm{P} \times \mathrm{Ps}$

$$
=300+5 \times 26.2
$$

$$
=431.0 \mathrm{psi}
$$

Maximum circumferential stress is calculated from a variation of the ISO Equation:

$$
\begin{aligned}
& \quad S=\frac{P t(\text { Do-t })}{2 t}=\frac{431(1.660-.191)}{2 x .191}=1657.4 \\
& \text { Safety Factor }=\frac{20 \text { second strength }}{\text { Maximum stress }}=\frac{8470}{1657}=5.11
\end{aligned}
$$

Table 44 gives the results of safety factor calculations based upon service factors of 0.5 and 0.4 for the 1-1/4" PVC Schedule 80 pipe of the example shown above using the full pressure rating calculated from the listed hydrostatic designstress.
Table 44
SAFETY FACTORS VS. SERVICE FACTORS - PVC TYPE 1 THERMOPLASTIC PIPE

| PIPE CLASS | SERVICE <br> FACTOR | HDS <br> PSI | PRESSURE <br> RATING <br> PSI | SURGE <br> PRESSURE <br> AT 5 FT/SEC | MAXIMUM <br> PRESSURE <br> PSI | MAXIMUM <br> STRESS <br> PSI | SAFETY <br> FACTOR |
| :--- | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $1-1 / 4^{\prime \prime}$ Sch. 80 | 0.5 | 2000 | 520 | 131.0 | 651.0 | 2503.5 | 3.38 |
| $1-1 / 4^{\prime \prime}$ Sch. 80 | 0.4 | 1600 | 416 | 131.0 | 547.0 | 2103.5 | 4.03 |

Pressure rating values are for PVC pipe, and for most sizes are calculated from the experimentally determined long-term strength of PVC extrusion compounds. Because molding compounds may differ in long term strength and elevated temperature properties from pipe compounds, piping systems

In each case, the hydrostatic design basis $=4000$ psi, and the water velocity $=5$ feet per second.

Comparing safety factor for this $1-1 / 4$ " Schedule 80 pipe at different service factors, it is instructive to note that changing from a service factor of 0.5 to a more conservative 0.4 increases the safety factor only by $16 \%$.

$$
100 \times\left(\frac{1-3.38}{4.03}\right)=16 \%
$$

In the same way, changing the service factor from 0.4 to 0.35 increases the safety factor only by $9 \%$. Changing the service factor from 0.5 to 0.35 increases the safety factor by 24\%.

From these comparisons it is obvious that little is to be gained in safety from surge pressures by fairly large changes in the hydrostatic design stress resulting from choice of more conservative service factors.

## FRICTION LOSS CHARACTERISTICS OF WATER THROUGH PLASTIC PIPE, FITTINGS AND VALVES

## INTRODUCTION

A major advantage of thermoplastic pipe is its exceptionally smooth inside surface area, which reduces friction loss compared to other materials.

Friction loss in plastic pipe remains constant over extended periods of time, in contrast to some other materials where the value of the Hazen and Williams C factor (constant for inside roughness) decreases with time. As a result, the flow capacity of thermoplastics is greater under fully turbulent flow conditions like those encountered in water service.

## C FACTORS

Tests made both with new pipe and pipe that had been in service revealed C factor values for plastic pipe between 160 and 165. Thus, the factor of 150 recommended for water in the equation below is on the conservative side. On the other hand, the C factor for metallic pipe varies from 65 to 125, depending upon age and interior roughening. The obvious benefit is that with plastic systems it is often possible to use a smaller diameter pipe and still obtain the same or even lower friction losses.

The most significant losses occur as a result of the length of pipe and fittings and depend on the following factors.

1. Flow velocity of the fluid.
2. The type of fluid being transmitted, especially its viscosity.
3. Diameter of the pipe.
4. Surface roughness of interior of the pipe.
5. The length of the pipeline.

## Hazen and Williams Formula

The head losses resulting from various water flow rates in plastic piping may be calculated by means of the Hazen and Williams formula:

$$
\begin{aligned}
\mathrm{f} & =0.2083\left(\frac{100}{\mathrm{C}}\right)^{1.852} \times \frac{\mathrm{q}^{1.852}}{\mathrm{Di}^{4.8655}} \\
& =.0983 \frac{\mathrm{q}^{1.852}}{\mathrm{Di} \mathrm{i}^{4.8655}} \text { for } \mathrm{C}=150 \\
\mathrm{P} & =.4335 \mathrm{f}
\end{aligned}
$$

## Where:

$\mathrm{f}=$ Friction Head in ft . of Water per 100 ft of Pipe
$P=$ Pressure Loss in psi per 100 ft . of Pipe
$\mathrm{Di}=$ Inside Diameter of Pipe, in.
$\mathrm{q}=$ Flow Rate in U.S. gal/min
C = Constant for Inside Roughness (C equals 150 thermoplastics)

## SYSTEMS ENGINEERING DATA <br> FOR THERMOPLASTIC PIPING

## FLOW OF FLUIDS AND HEAD LOSS CALCULATIONS

Tables，flow charts，or a monograph may be used to assist in the design of a piping system depending upon the accuracy desired．In computing the internal pressure for a specified flow rate，changes in static head loss due to restrictions（valves，orifices，etc．）as well as flow head loss must be considered．

The formula in Table 45 can be used to determine the head loss due to flow if the fluid viscosity and density and flow rate are known．The head loss in feet of fluid is given by：

$$
\mathrm{h}=: 186 \frac{\mathrm{fLV}}{\mathrm{~d}^{2}}
$$

f ，the friction factor，is a funcion of the Reynolds number，adimen－ sionless parameter which indicates the degree of turbulence．

$$
\text { The Reynolds number is defined as: } f=\frac{d V W}{12 U}
$$

Figure 7 below shows the relationship between the friction factor， f ， and the Reynolds number，R．It is seen that three distinct flow zones exist．In the laminar flow zone，from Reynolds numbers 0 to 2000， the friction factor is given by the equation：

$$
f=\frac{64}{R}
$$

Substituting this in the equation for the head loss，the formula for laminar flow becomes：

Flow in the critical zone，Reynolds numbers 2000 to 4000，is unsta－ ble and a surging type of flow exists．Pipe lines should be designed to avoid operation in the critical zone since head losses cannot be calculated accurately in this zone．In addition，the unstable flow results in pressure surges and water hammer which may be exces－ sively high．In the transition zone，the degree of turbulence increas－ es as the Reynolds number increases．However，due to the smooth inside surface of plastic pipe，complete turbulence rarely exists． Most pipe systems are designed to operate in the transition zone．

TABLE 45
FORMULAS FOR HEAD LOSS CALCULATIONS
$R=\frac{d V w}{12 u} \quad$ SYMBOL QUANTITY UNITS

$$
\mathrm{R}=\frac{\begin{array}{c}
12 \mathrm{u} \\
3160 \mathrm{G} \\
\mathrm{kd}
\end{array}}{\text { 隹 }}
$$

B flow rate barrels／hour
d inside diameter inches
f friction factor dimensionless gallons／minute feet of fluid centistokes feet lbs／in ${ }^{2}$ $\mathrm{ft}^{3} / \mathrm{sec}$ ． dimensionless $\mathrm{lb} / \mathrm{tt}-\mathrm{sec}$ ． ft ／sec． lbs／tt ${ }^{3}$ centipoises

## MANNING EQUATION

The Manning roughness factor is another equation used to deter－ mine friction loss in hydraulic flow．Like the Hazen－Williams C fac－ tor，the Manning＂$n$＂factor is an empirical number that defines the interior wall smoothness of a pipe．PVC pipe has an＂$n$＂value that ranges from 0.008 to 0.012 from laboratory testing．Comparing with cast iron with a range of 0.011 to 0.015 ，PVC is at least 37.5 per－ cent more efficient，or another way to express this would be to have equal flow with the PVC pipe size being one－third smaller than the cast iron．The following table gives the range of＂n＂value for various piping materials．

Table 46

| PIPE MATERIAL | ＂n＂RANGE |
| :--- | :---: |
| CAST IRON | $0.011-0.015$ |
| WROUGHT IRON（BLACK） | $0.012-0.015$ |
| WROUGHT IRON（GALVANIZED） | $0.013-0.017$ |
| SMOOTH BRASS | $0.009-0.013$ |
| GLASS | $0.009-0.013$ |
| RIVETED AND SPIRAL STEEL | $0.013-0.017$ |
| CLAY DRAINAGE TILE | $0.011-0.017$ |
| CONCRETE | $0.012-0.016$ |
| CONCRETE LINED | $0.012-0.018$ |
| CONCRETE－RUBBLE SURFACE | $0.017-0.030$ |
| PVC | $0.008-0.012$ |
| WOOD | $0.010-0.013$ |

# ABOVE-GROUND INSTALLATION OF THERMOPLASTIC PIPING 

## EXPANSION AND CONTRACTION OF PLASTIC PIPE

Plastics, like other piping materials, undergo dimensional changes as a result of temperature variations above and below the installation temperature. In most cases, piping should be allowed to move unrestrained in the piping support system between desired anchor points without abrasion, cutting or restriction of the piping. Excessive piping movement and stresses between anchor points must be compensated for and eliminated by installing expansion loops, offsets, changes in direction or teflon bellows expansion joints. (See Figure 7 for installed examples.)

If movement resulting from these dimensional changes is restricted by adjacent equipment, improper pipe clamping and support, inadequate expansion compensation, or by a vessel to which the pipe is attached, the resultant stresses and forces may cause damage to the equipment or piping.

## A. Calculating Dimensional Change and Expansion Loop Size

The extent of expansion or contraction $(\Delta \mathrm{L})$ is dependent upon the piping material of construction and its coefficient of linear expansion $(\mathrm{Y})$, the length of straight run being considered (L), and the temperature that the piping will possibly experience ( $\mathrm{T}_{1}-\mathrm{T}_{2}$ ). The worst possible situations for maximum and minimum temperatures must be considered. The formula for determining change in pipe length due to temperature change is:

$$
\Delta L=\frac{Y\left(T_{1}-T_{2}\right)}{10} \times \frac{L}{100}
$$

Where: $\Delta \mathrm{L}=$ Dimensional change due to thermal expansion or contraction (inches).
$\mathrm{Y}=$ Expansion coefficient (inches $/ 10^{\circ} \mathrm{F} / 100 \mathrm{ft}$ ) See Table 47
$\left(T_{1}-T_{2}\right)=$ Temperature differential (degrees $F$ )
$L=$ Length of straight pipe run being considered (Feet)

TABLE 47
EXPANSION COEFFICIENT

## Material

FRP (Epoxy and Vinylester)
PVC
Y value (in $\left./ 10^{\circ} \mathrm{F} / 100 \mathrm{ft}\right)$
. 100
.360
CPVC . 456
Fuseal (PP) 1-1/2-6 in. . 600
Fuseal (PP) 8, 10, 12 in . 732
Proseal (PP) . 732
Proline (PP) 1.000
Polyethylene (PE) 1.250
Superproline (PVDF) 0.800
Generally, stresses due to expansion and contraction of a piping system can be reduced or eliminated through frequent changes in direction or through the installation of expansion loops. Loops, as depicted in Figure 7, are fabricated with 4 elbows and straight pipe and are much less expensive than teflon expansion joints. The loop sizing formula is as follows:

$$
\mathrm{R}=1.44 \quad \sqrt{ } \mathrm{D} \quad \Delta \mathrm{~L}
$$

Where: $R=$ Expansion loop leg length in feet
D = Nominal outside diameter (O.D.) of pipe in inches
$\Delta L=$ Change in length in inches due to expansion or contraction

## EXAMPLE:

How much expansion can be expected in a 300 foot straight run of 6 inch PVC Sch. 80 pipe that will be installed at $80^{\circ} \mathrm{F}$, operated at $110^{\circ} \mathrm{F}$, and will experience a $50^{\circ} \mathrm{F}$ minimum in winter and $120^{\circ} \mathrm{F}$ maximum in summer? How long should the expansion loop legs be to compensate for the resultant expansion and contraction?

$$
\begin{aligned}
\Delta \mathrm{L} & =0.360 \frac{(120-50)}{10} \times \frac{300}{100} \\
& =0.360 \times 7.0 \times 3 \\
& =7.56 \text { inches change in length } \\
\mathrm{R} & =1.44 \sqrt{ } \mathrm{D} \Delta \mathrm{~L} \\
& =1.44 \sqrt{ } 6.625 \times 7.56 \\
& =1.44 \times 7.08 \\
& =10.20 \text { Feet }
\end{aligned}
$$

Figure 7



Loop


## ABOVE-GROUND INSTALLATION OF THERMOPLASTIC PIPING

THERMAL EXPANSION COMPENSATION
The change in length of thermoplastic pipe with temperature variation should always be considered when installing pipe lines and

Table 48 THERMAL EXPANSION $\Delta L$ (in.) - PVC Type 1

| TEMP. <br> CHANGE <br> $\Delta \mathbf{T}^{\circ} \mathbf{F}$ | $\mathbf{1 0}$ | $\mathbf{2 0}$ | $\mathbf{3 0}$ | $\mathbf{4 0}$ | $\mathbf{5 0}$ | $\mathbf{6 0}$ | $\mathbf{7 0}$ | $\mathbf{8 0}$ | $\mathbf{9 0}$ | $\mathbf{1 0 0}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 30 | .11 | .22 | .32 | .43 | .54 | .65 | .76 | .86 | .97 | 1.08 |
| 40 | .14 | .29 | .43 | .58 | .72 | .86 | 1.01 | 1.15 | 1.30 | 1.44 |
| 50 | .18 | .36 | .54 | .72 | .90 | 1.08 | 1.26 | 1.40 | 1.62 | 1.80 |
| 60 | .22 | .43 | .65 | .86 | 1.08 | 1.30 | 1.51 | 1.72 | 1.94 | 2.16 |
| 70 | .25 | .50 | .76 | 1.01 | 1.26 | 1.51 | 1.76 | 2.02 | 2.27 | 2.52 |
| 80 | .29 | .58 | .86 | 1.15 | 1.44 | 1.73 | 2.02 | 2.30 | 2.59 | 2.88 |
| 90 | .32 | .65 | .97 | 1.30 | 1.62 | 1.94 | 2.27 | 2.59 | 2.92 | 3.24 |
| 100 | .36 | .72 | 1.03 | 1.44 | 1.80 | 2.16 | 2.52 | 2.88 | 3.24 | 3.60 |

Example: Highest temperature expected $-120^{\circ} \mathrm{F}$
Lowest temperature expected
Total change ( $\Delta \mathrm{T}$ )
$\frac{50^{\circ} \mathrm{F}}{70^{\circ} \mathrm{F}}$
Length of run- 40 feet
From $70^{\circ} \mathrm{F}$ row on PVC chart read 1.01 in. length change ( $\Delta \mathrm{L}$ )
NOTE: Table is based on: $\Delta \mathrm{L}=12 \mathrm{eL}(\Delta \mathrm{T})$
Where $e=$ Coefficient of Thermal Expansion
$=3.0 \times 10^{-5} \mathrm{in} . / \mathrm{in} .{ }^{\circ} \mathrm{F}$
$\mathrm{L}=$ Length of Run
$\Delta T=$ Temperature Change
Table 49 THERMAL EXPANSION $\Delta \mathbf{L}$ (in.)
CPVC Schedule 80

| TEMP. <br> CHANGE <br> $\Delta \mathbf{T}^{\circ} \mathbf{F}$ | $\mathbf{1 0}$ |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  | $\mathbf{2 0}$ | $\mathbf{3 0}$ | $\mathbf{4 0}$ | $\mathbf{5 0}$ | $\mathbf{6 0}$ | $\mathbf{7 0}$ | $\mathbf{8 0}$ | $\mathbf{9 0}$ | $\mathbf{1 0 0}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $\mathbf{2 0}$ | .09 | .18 | .27 | .36 | .46 | .55 | .64 | .73 | .82 | .91 |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |
| $\mathbf{3 0}$ | .14 | .27 | .41 | .55 | .68 | .82 | .96 | 1.09 | 1.23 | 1.37 |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |
| $\mathbf{4 0}$ | .18 | .36 | .55 | .73 | .91 | 1.09 | 1.28 | 1.46 | 1.64 | 1.82 |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |
| $\mathbf{5 0}$ | .23 | .46 | .68 | .91 | 1.14 | 1.37 | 1.60 | 1.82 | 2.05 | 2.28 |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |
| $\mathbf{6 0}$ | .27 | .55 | .82 | 1.09 | 1.37 | 1.64 | 1.92 | 2.19 | 2.46 | 2.74 |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |
| $\mathbf{7 0}$ | .32 | .64 | .96 | 1.28 | 1.60 | 1.92 | 2.23 | 2.55 | 2.87 | 3.19 |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |
| $\mathbf{8 0}$ | .36 | .73 | 1.09 | 1.46 | 1.82 | 2.19 | 2.55 | 2.92 | 3.28 | 3.65 |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |
| $\mathbf{9 0}$ | .41 | .82 | 1.23 | 1.64 | 2.05 | 2.46 | 2.87 | 3.28 | 3.69 | 4.10 |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |
| $\mathbf{1 0 0}$ | .46 | .91 | 1.37 | 1.82 | 2.28 | 2.74 | 3.19 | 3.65 | 4.10 | 4.56 |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |  |

Table 50 THERMAL EXPANSION $\Delta \mathrm{L}$ (in)
Copolymer Polypropylene

| TEMP. <br> CHANGE <br> $\Delta \mathbf{T}^{\circ} \mathbf{F}$ | $\mathbf{1 0}$ | $\mathbf{2 0}$ | $\mathbf{3 0}$ | $\mathbf{4 0}$ | $\mathbf{5 0}$ | $\mathbf{6 0}$ | $\mathbf{7 0}$ | $\mathbf{8 0}$ | $\mathbf{9 0}$ | $\mathbf{1 0 0}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $\mathbf{2 0}$ | .15 | .29 | .44 | .59 | .73 | .88 | 1.02 | 1.17 | 1.32 | 1.46 |
| $\mathbf{3 0}$ | .22 | .44 | .66 | .88 | 1.10 | 1.32 | 1.54 | 1.76 | 1.98 | 2.20 |
| $\mathbf{4 0}$ | .29 | .59 | .88 | 1.17 | 1.46 | 1.76 | 2.05 | 2.34 | 2.64 | 2.93 |
| $\mathbf{5 0}$ | .37 | .73 | 1.10 | 1.46 | 1.83 | 2.20 | 2.56 | 2.93 | 3.29 | 3.66 |
| $\mathbf{6 0}$ | .44 | .88 | 1.32 | 1.76 | 2.20 | 2.64 | 3.07 | 3.51 | 3.95 | 4.39 |
| $\mathbf{7 0}$ | .51 | 1.02 | 1.54 | 2.05 | 2.56 | 3.07 | 3.59 | 4.10 | 4.61 | 5.12 |
| $\mathbf{8 0}$ | .59 | 1.17 | 1.76 | 2.34 | 2.93 | 3.51 | 4.10 | 4.68 | 5.27 | 5.86 |
| $\mathbf{9 0}$ | .66 | 1.32 | 1.98 | 2.69 | 3.29 | 3.95 | 4.61 | 5.27 | 5.93 | 6.59 |
| $\mathbf{1 0 0}$ | .73 | 1.46 | 2.20 | 2.93 | 3.66 | 4.39 | 5.12 | 5.86 | 6.59 | 7.32 |

proviisions made to compensate for this change in length. The following tables have been prepared to assist you in determining this expansion.
Table 51 THERMAL EXPANSION $\Delta$ L (in.) - PVDF

## Schedule 80

| TEMP. | LENGTH OF RUN IN FEET |  |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $\Delta \mathrm{T}^{\circ} \mathrm{F}$ | 10 | 20 | 30 | 40 | 50 | 60 | 70 | 80 | 90 | 100 |
| 20 | . 19 | . 38 | . 58 | . 77 | . 96 | 1.15 | 1.34 | 1.54 | 1.73 | 1.92 |
| 40 | . 38 | . 77 | 1.15 | 1.54 | 1.92 | 2.30 | 2.69 | 3.07 | 3.46 | 3.84 |
| 50 | . 48 | . 96 | 1.44 | 1.92 | 2.40 | 2.88 | 3.36 | 3.84 | 4.32 | 4.80 |
| 60 | . 58 | 1.15 | 1.73 | 2.30 | 2.88 | 3.46 | 4.03 | 4.61 | 5.18 | 5.76 |
| 70 | . 67 | 1.34 | 2.02 | 2.69 | 3.36 | 4.03 | 4.70 | 5.38 | 6.05 | 6.72 |
| 80 | . 77 | 1.54 | 2.30 | 3.07 | 3.84 | 4.61 | 5.38 | 6.14 | 6.91 | 7.68 |
| 90 | . 86 | 1.73 | 2.59 | 3.46 | 4.32 | 5.18 | 6.05 | 6.91 | 7.78 | 8.64 |
| 100 | . 96 | 1.92 | 2.88 | 3.84 | 4.80 | 5.76 | 6.72 | 7.68 | 8.64 | 9.60 |

The following expansion loop and offset lengths have been calculated based on stress and modulus of elasticities at the temperature shown below each chart. To calculate the proper length of loop at other temperatures the following formula may be used:
$1 \sqrt{\frac{3 E(O . D .) \Delta L}{2 S}}$
Where:
$\Delta \mathrm{T}=$ Temperature Change in ${ }^{\circ} \mathrm{F}$
S = Thermal Stress, psi $=e(\Delta T) E$
$\mathrm{E}=$ Modulus of Elasticity (found in relative properties chart on pages 40-41.
$\Delta \mathrm{L}=$ Length Change in Inches at $\Delta \mathrm{T}$ (see tables above)
$I=$ Total Length of Loop or Offset

Table 52 EXPANSION LOOPS AND OFFSET LENGTHS, PVC Type 1 Schedule 40 and 80

| NOM. PIPE SIZE | AVERAGE | LENGTH OF RUN IN FEET |  |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 10 | 20 | 30 | 40 | 50 | 60 | 70 | 80 | 90 | 100 |
|  | O.D. | LENGTH OF LOOP " $\mu$ " IN INCHES |  |  |  |  |  |  |  |  |  |
| 1/2 | . 840 | 11 | 15 | 19 | 22 | 24 | 27 | 29 | 31 | 32 | 34 |
| 3/4 | 1.050 | 12 | 17 | 21 | 24 | 27 | 30 | 32 | 34 | 36 | 38 |
| 1 | 1.315 | 14 | 19 | 23 | 27 | 30 | 33 | 36 | 38 | 41 | 43 |
| 1-1/4 | 1.660 | 15 | 22 | 26 | 30 | 34 | 37 | 40 | 43 | 46 | 48 |
| 1-1/2 | 1.900 | 16 | 23 | 28 | 33 | 36 | 40 | 43 | 46 | 49 | 51 |
| 2 | 2.375 | 18 | 26 | 32 | 36 | 41 | 45 | 48 | 52 | 55 | 58 |
| 3 | 3.500 | 22 | 31 | 38 | 44 | 49 | 54 | 58 | 63 | 66 | 70 |
| 4 | 4.500 | 25 | 35 | 43 | 50 | 56 | 61 | 66 | 71 | 75 | 79 |
| 6 | 6.625 | 30 | 43 | 53 | 61 | 68 | 74 | 80 | 86 | 91 | 96 |
| 8 | 8.625 | 35 | 49 | 60 | 69 | 78 | 85 | 92 | 98 | 104 | 110 |
| 10 | 10.750 | 39 | 55 | 67 | 77 | 87 | 95 | 102 | 110 | 116 | 122 |
| 12 | 12.750 | 42 | 60 | 73 | 84 | 94 | 103 | 112 | 119 | 126 | 133 |

NOTE: Table based on stress and modulus of elasticity at $130^{\circ} \mathrm{F}$ $\Delta \mathrm{T}=50^{\circ} \mathrm{F}$
$\mathrm{S}=600 \mathrm{psi}$
$\mathrm{E}=3.1 \times 10^{5} \mathrm{psi}$

## ABOVE-GROUND INSTALLATION OF THERMOPLASTIC PIPING

Table 53
EXPANSION LOOPS AND OFFSET LENGTHS, CPVC Schedule 80

| NOM. PIPE SIZE | AVERAGE O.D. | LENGTH OF RUN IN FEET |  |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 10 | 20 | 30 | 40 | 50 | 60 | 70 | 80 | 90 | 100 |
|  |  | LENGTH OF LOOP "]" IN INCHES |  |  |  |  |  |  |  |  |  |
| 1/2 | . 840 | 15 | 21 | 26 | 30 | 33 | 37 | 39 | 42 | 45 | 47 |
| 3/4 | 1.050 | 17 | 22 | 27 | 31 | 34 | 38 | 40 | 43 | 46 | 48 |
| 1 | 1.315 | 19 | 26 | 32 | 37 | 42 | 46 | 49 | 53 | 56 | 59 |
| 1-1/4 | 1.660 | 21 | 30 | 36 | 42 | 47 | 52 | 56 | 59 | 63 | 67 |
| 1-1/2 | 1.900 | 23 | 32 | 39 | 45 | 50 | 55 | 59 | 64 | 67 | 71 |
| 2 | 2.375 | 25 | 35 | 43 | 50 | 56 | 62 | 67 | 71 | 75 | 80 |
| 3 | 3.500 | 31 | 43 | 53 | 61 | 68 | 75 | 81 | 86 | 91 | 97 |
| 4 | 4.500 | 35 | 49 | 60 | 69 | 77 | 85 | 92 | 98 | 103 | 109 |
| 6 | 6.625 | 42 | 59 | 73 | 84 | 94 | 103 | 111 | 119 | 125 | 133 |
| 8 | 8.625 | 48 | 67 | 83 | 96 | 107 | 118 | 127 | 135 | 143 | 152 |
| 10 | 10.750 | 54 | 75 | 93 | 107 | 119 | 131 | 142 | 151 | 160 | 169 |
| 12 | 12.750 | 59 | 82 | 101 | 116 | 130 | 143 | 154 | 164 | 174 | 184 |

NOTE: Table based on stress and modulus of elasticity at $160^{\circ} \mathrm{F}$.

$$
\begin{aligned}
& \Delta \mathrm{T}=100^{\circ} \mathrm{F} \\
& \mathrm{~S}=750 \mathrm{psi} \\
& \mathrm{E}=2.91 \times 10^{5} \mathrm{psi}
\end{aligned}
$$

Table 54
EXPANSION LOOPS AND OFFSET LENGTHS
Copolymer Polypropylene

| NOM PIPE SIZE | AVERAGE O.D. | LENGTH OF RUN IN FEET |  |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 10 | 20 | 30 | 40 | 50 | 60 | 70 | 80 | 90 | 100 |
|  |  | LENGTH OF LOOP " $¢$ " IN INCHES |  |  |  |  |  |  |  |  |  |
| 1/2 | . 840 | 18 | 25 | 31 | 36 | 40 | 44 | 47 | 50 | 54 | 57 |
| 3/4 | 1.050 | 20 | 28 | 35 | 40 | 45 | 49 | 53 | 56 | 60 | 63 |
| 1 | 1.315 | 22 | 32 | 39 | 45 | 50 | 55 | 59 | 63 | 67 | 71 |
| 1-1/4 | 1.660 | 25 | 35 | 43 | 50 | 56 | 62 | 66 | 71 | 75 | 79 |
| 1-1/2 | 1.900 | 27 | 38 | 46 | 54 | 60 | 66 | 71 | 76 | 81 | 85 |
| 2 | 2.375 | 30 | 42 | 52 | 60 | 67 | 74 | 79 | 85 | 90 | 95 |
| 3 | 3.500 | 36 | 52 | 63 | 73 | 81 | 89 | 96 | 103 | 109 | 115 |
| 4 | 4.500 | 41 | 58 | 71 | 83 | 92 | 101 | 109 | 117 | 124 | 13 |
| 6 | 6.625 | 50 | 71 | 87 | 100 | 112 | 123 | 132 | 142 | 151 | 159 |
| 8 | 8.625 | 57 | 81 | 99 | 114 | 128 | 140 | 151 | 162 | 172 | 181 |
| 10 | 10.750 | 64 | 90 | 111 | 128 | 143 | 156 | 169 | 181 | 192 | 202 |
| 12 | 12.750 | 69 | 98 | 121 | 139 | 155 | 170 | 184 | 197 | 209 | 220 |

NOTE: Table based on stress and modulus of elasticity at $160^{\circ} \mathrm{F}$.

$$
\begin{aligned}
& \Delta \mathrm{T}=100^{\circ} \mathrm{F} \\
& \mathrm{~S}=240 \mathrm{psi} \\
& \mathrm{E}=.83 \times 10^{5} \mathrm{lb} . / \mathrm{in} .^{2}
\end{aligned}
$$

Table 55
EXPANSION LOOPS AND OFFSET LENGTHS, PVDF Schedule 80

| NOM. PIPE SIZE | AVERAGE O.D. | LENGTH OF RUN IN FEET |  |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  |  | 10 | 20 | 30 | 40 | 50 | 60 | 70 | 80 | 90 | 100 |
|  |  | LENGTH OF LOOP "I" IN INCHES |  |  |  |  |  |  |  |  |  |
| 1/2 | . 840 | 10 | 15 | 18 | 20 | 23 | 25 | 27 | 29 | 31 | 32 |
| 3/4 | 1.050 | 11 | 16 | 20 | 23 | 26 | 28 | 30 | 32 | 34 | 36 |
| 1 | 1.315 | 13 | 18 | 22 | 26 | 29 | 31 | 34 | 36 | 38 | 40 |
| 1-1/4 | 1.660 | 14 | 20 | 25 | 29 | 32 | 35 | 38 | 41 | 41 | 45 |
| 1-1/2 | 1.900 | 15 | 22 | 27 | 31 | 34 | 38 | 41 | 44 | 44 | 49 |
| 2 | 2.375 | 17 | 24 | 30 | 34 | 38 | 42 | 46 | 49 | 49 | 54 |

NOTE: Table based on stress and modulus of elasticity at $180^{\circ} \mathrm{F}$. $\Delta T=100^{\circ} \mathrm{F}$
$\mathrm{S}=1080 \mathrm{psi}$
$\mathrm{E}=1.04 \times 10^{5} \mathrm{psi}$


## ABOVE-GROUND INSTALLATION <br> OF THERMOPLASTIC PIPING

These tables are based on:
F = As = restraining force, lbs.
A $=$ Cross sectional wall area, in. ${ }^{2}$
$\mathrm{S}=\mathrm{e}(\Delta \mathrm{T}) \mathrm{E}^{*}$
e = Coefficient of liner expansion*
$E=$ Modulus of elasticity*
$\Delta \mathrm{T}=$ Temperature change, ${ }^{\circ} \mathrm{F}$
*All values are available from relative properties chart on pages 40-41.

Table 56
RESTRAINT FORCE "F" (LB.) - PVC Type 1
Schedule 40 and 80.

| $\begin{aligned} & \text { PIPE } \\ & \text { SIZE } \end{aligned}$ | SCHEDULE 40 PVC |  |  | SCHEDULE 80 PVC |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | CROSS SECTIONAL WALL AREA $\left(\right.$ IN $\left.^{2}\right)$ | $\begin{gathered} \Delta \mathrm{T}= \\ 50^{\circ} \mathrm{F} \\ \mathrm{~S}= \\ 630 \mathrm{PSI} \end{gathered}$ | $\begin{gathered} \Delta \mathrm{T}= \\ 100^{\circ} \mathrm{F} \\ \mathrm{~S}= \\ 1260 \mathrm{PS} \end{gathered}$ | CROSS SECTIONAL WALL AREA $\left(\mathrm{IN}^{2}\right)$ | $\begin{gathered} \Delta \mathrm{T}= \\ 50^{\circ} \mathrm{F} \\ \mathrm{~S}= \\ 630 \mathrm{PS} \end{gathered}$ | $\begin{gathered} \Delta \mathrm{T}= \\ 100^{\circ} \mathrm{F} \\ \mathrm{~S}= \\ 1260 \mathrm{PS} \end{gathered}$ |
| 1/2 | . 250 | 155 | 310 | . 320 | 200 | 400 |
| 3/4 | . 333 | 210 | 420 | . 434 | 275 | 550 |
| 1 | . 494 | 310 | 6220 | . 639 | 405 | 810 |
| 1-1/4 | . 669 | 420 | 840 | . 882 | 555 | 1,110 |
| 1-1/2 | . 800 | 505 | 1,010 | 1.068 | 675 | 1,350 |
| 2 | 1.075 | 675 | 1,350 | 1.477 | 930 | 1,860 |
| 3 | 2.229 | 1,405 | 2,810 | 3.016 | 1,900 | 3,800 |
| 4 | 3.174 | 2,000 | 4,000 | 4.407 | 2,775 | 5,550 |
| 6 | 5.581 | 3,515 | 7,030 | 8.405 | 5,295 | 10,590 |
| 8 | 8.399 | 5,290 | 10,580 | 12.763 | 8,040 | 16,080 |
| 10 | 11.908 | 7,500 | 15,000 | 18.922 | 11,920 | 23,840 |
| 12 | 15.745 | 9,920 | 19,840 | 26.035 | 16,400 | 32,800 |

Table 57
RESTRAINT FORCE "F" (LB.) CPVC Schedule 80

| PIPE <br> SIZE | CROSS SECTIONAL <br> WALL AREA $\left(\mathbf{I N}^{\mathbf{2}}\right)$ | $\Delta \mathbf{T}=\mathbf{5 0} \mathbf{0}^{\circ} \mathbf{F}$ <br> $\mathbf{S}=\mathbf{8 0 5} \mathbf{~ P S I}$ | $\Delta \mathbf{T}=\mathbf{1 0 0}^{\circ} \mathbf{F}$ <br> $\mathbf{S}=\mathbf{1 6 1 0} \mathbf{P S I}$ |
| :---: | :---: | :---: | :---: |
| $\mathbf{1 / 2}$ | .320 | 260 | 520 |
| $\mathbf{3 / 4}$ | .434 | 350 | 700 |
| $\mathbf{1}$ | .639 | 515 | 1,030 |
| $\mathbf{1 - 1 / 4}$ | .882 | 710 | 1,420 |
| $\mathbf{1 - 1 / 2}$ | 1.068 | 860 | 1,720 |
| $\mathbf{2}$ | 1.477 | 1,190 | 2,380 |
| $\mathbf{3}$ | 3.016 | 2,430 | 4,860 |
| $\mathbf{4}$ | 4.407 | 3,550 | 7,100 |
| $\mathbf{6}$ | 8.405 | 6,765 | 13,530 |
| $\mathbf{8}$ | 12.763 | 10,275 | 20,550 |
| $\mathbf{1 0}$ | 18.922 | 15,230 | 30,460 |
| $\mathbf{1 2}$ | 26.035 | 20,960 | 41,920 |

Table 58
RESTRAINT FORCE "F" (LB.) Copolymer Polypropylene Schedule 80

| PIPE <br> SIZE | $\left.\begin{array}{c}\text { CROSS SECTIONAL } \\ \text { WALL AREA (IN }\end{array} \mathbf{}^{2}\right)$ | $\Delta \mathbf{T}=\mathbf{5 0}{ }^{\circ} \mathbf{F}$ <br> $\mathbf{S}=\mathbf{5 5 0} \mathbf{~ P S I ~}$ | $\Delta \mathbf{T}=\mathbf{1 0 0}^{\circ} \mathbf{F}$ <br> $\mathbf{S}=\mathbf{1 1 1 0} \mathbf{~ P S I ~}$ |
| :---: | :---: | :---: | :---: |
| $\mathbf{1 / 2}$ | .320 | 147 | 294 |
| $\mathbf{3 / 4}$ | .434 | 199 | 398 |
| $\mathbf{1}$ | .639 | 293 | 586 |
| $\mathbf{1 - 1 / 4}$ | .882 | 404 | 808 |
| $\mathbf{1 - 1 / 2}$ | 1.068 | 489 | 978 |
| $\mathbf{2}$ | 1.477 | 663 | 1,325 |
| $\mathbf{3}$ | 3.016 | 1,381 | 2,276 |
| $\mathbf{4}$ | 4.407 | 2,018 | 4,036 |
| $\mathbf{6}$ | 8.405 | 3,899 | 7,698 |
| $\mathbf{8}$ | 12.763 | 5,895 | 11,690 |
| $\mathbf{1 0}$ | 18.922 | 8,666 | 17,332 |
| $\mathbf{1 2}$ | 26.035 | 11,929 | 23,848 |

Table 59
RESTRAINT FORCE "F" (LB.) PVDF Schedule 80

| PIPE <br> SIZE | CROSS SECTIONAL <br> WALL AREA $\left(\mathbf{I N}^{2} \mathbf{}\right)$ | $\Delta \mathbf{T}=\mathbf{5 0}{ }^{\circ} \mathbf{F}$ <br> $\mathbf{S}=\mathbf{8 5 0} \mathbf{P S I}$ | $\Delta \mathbf{T}=\mathbf{1 0 0}{ }^{\circ} \mathbf{F}$ <br> $\mathbf{S}=\mathbf{1 7 0 0} \mathbf{P S I}$ |
| :---: | :---: | :---: | :---: |
| $\mathbf{1 / 2}$ | .320 | 270 | 540 |
| $\mathbf{3 / 4}$ | .434 | 370 | 740 |
| $\mathbf{1}$ | .639 | 540 | 1,080 |
| $\mathbf{1 - 1 / 4}$ | .882 | 750 | 1,500 |
| $\mathbf{1 - 1 / \mathbf { 2 }}$ | 1.068 | 905 | 1,810 |
| $\mathbf{2}$ | 1.477 | 1,255 | 2,510 |
| $\mathbf{3}$ | 3.016 | 2,565 | 5,130 |
| $\mathbf{4}$ | 4.407 | 3,745 | 7,490 |

## ABOVE-GROUND INSTALLATION OF THERMOPLASTIC PIPING

## A. HANGERS

Plastic piping hangers must allow axial movement between anchor points. Hangers must prevent transverse movement and in conjunction with anchors, prevent point loading of the piping. Figures 8, 9, 10, 11 and 12 on page 70 are examples of types of hangers, anchors and support which may be used. Sleeving plastic piping at horizontal support points with a plastic pipe one pipe size larger which will allow unrestricted movement is recommended. Anchors should be placed at tees, valves, and desired locations to create sections of predictable expansion and contraction in the piping system.

Vertical lines must also be supported at proper intervals so that the fitting at the lower end is not overloaded. The supports should not exert a compressive strain on the pipe such as the double-bolt type. Riser clamps squeeze the pipe and are not recommended. If possible, each clamp should be located just below a coupling or other fitting so that the shoulder of the coupling provides bearing support to the clamp.

## B. SUPPORT SPACING OF PLASTIC PIPE

When thermoplastic piping systems are installed aboveground, they must be properly supported to avoid unnecessary stresses and possible sagging.

Horizontal runs require the use of hangers spaced approximately as indicated in tables for individual material shown below. Note that additional support is required as temperatures increase. Continuous support can be accomplished by the use of a smooth structural angle or channel.

Where the pipe is exposed to impact damage, protective shields should be installed.

Tables are based on the maximum deflection of a uniformly loaded, continuously supported beam calculated from:

$$
y=.00541 \frac{\mathrm{wL} L^{4}}{E l}
$$

Where:
y = Deflection or sag, in.
$\mathrm{w}=$ Weight per unit length, lb/in.
$\mathrm{L}=$ Support spacing, in.
$\mathrm{E}=$ Modulus of elasticity at given temp. $\mathrm{Ib} / \mathrm{in}^{2}$
I = Moment of inertia, in. ${ }^{4}$

If 0.100 in . is chosen arbitrarily as the permissible sag ( y ) between supports, then:

Where:

$$
L^{4}=18.48 \frac{\mathrm{El}}{\mathrm{~W}}
$$

W = Weight of Pipe + Weight of Liquid, lb./in.
For a pipe $I=\frac{\pi}{64}\left(D o^{4}-D i^{4}\right)$
Where:
Do = Outside diameter of the pipe, in.
$\mathrm{Di}=$ Inside diameter of the pipe, in.
Then:


Table 60
SUPPORT SPACING "L" (FT.) - PVC

|  | NOMINAL PIPE SIZE |  |  |  |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| ${ }^{\circ} \mathrm{F}$ | 1/2 | 3/4 | 1 | 1-1/4 | 1-1/2 | 2 | 3 | 4 | 6 | 8 | 10 | 12 |
| SCHEDULE 40 PVC |  |  |  |  |  |  |  |  |  |  |  |  |
| 60 | 4-1/4 | 4-1/2 | 5 | 5-1/2 | 5-3/4 | 6-1/4 | 7-1/2 | 8-1/4 | 9-1/2 | 10-1/2 | 11-1/2 | 12-1/2 |
| 100 | 4 | 4-1/4 | 4-3/4 | 5-1/4 | 5-1/2 | 6 | 7 | 7-3/4 | 9 | 10 | 11 | 11-3/4 |
| 140 | 3-3/4 | 4 | 4-1/2 | 5 | 5-1/4 | 5-3/4 | 6-3/4 | 7-1/2 | 8-1/2 | 9-3/4 | 10-1/2 | 11-1/4 |
| SCHEDULE 80 PVC |  |  |  |  |  |  |  |  |  |  |  |  |
| 60 | 4-1/2 | 4-3/4 | 5-1/4 | 5-3/4 | 6 | 6-1/2 | 8 | 8-3/4 | 10-1/2 | 11-1/2 | 12-3/4 | 14 |
| 100 | 4 | 4-1/2 | 5 | 5-1/2 | 5-3/4 | 6-1/4 | 7-1/2 | 8-1/4 | 10 | 11 | 12-1/4 | 13-1/4 |
| 140 | 3-3/4 | 4-1/4 | 4-3/4 | 5-1/4 | 5-1/4 | 6 | 7 | 8 | 9-1/2 | 10-1/2 | 11-1/2 | 12-1/2 |

Table 61
SUPPORT SPACING "L" (FT.) - CPVC Schedule 80

| TEMP <br> ${ }^{\circ} \mathrm{F}$ | NOMINAL PIPE SIZE |  |  |  |  |  |  |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | $\mathbf{1 / 2}$ | $\mathbf{3 / 4}$ | $\mathbf{1}$ | $\mathbf{1 - 1 / 4}$ | $\mathbf{1 - 1 / 2}$ | $\mathbf{2}$ | $\mathbf{3}$ | $\mathbf{4}$ | $\mathbf{6}$ | $\mathbf{8}$ | $\mathbf{1 0}$ | $\mathbf{1 2}$ |  |  |  |
| 73 | 4 | $4-1 / 2$ | 5 | $5-1 / 2$ | $5-3 / 4$ | $6-1 / 2$ | $7-3 / 4$ | $8-1 / 2$ | $10-1 / 4$ | $11-1 / 4$ | $12-1 / 2$ | $13-3 / 4$ |  |  |  |
| 100 | 4 | $4-1 / 2$ | 5 | $5-1 / 2$ | $5-3 / 4$ | $6-1 / 4$ | $7-1 / 2$ | $8-1 / 4$ | 10 | 11 | $12-1 / 2$ | $13-1 / 4$ |  |  |  |
| 120 | 4 | $4-1 / 4$ | $4-3 / 4$ | $5-1 / 4$ | $5-1 / 2$ | $6-1 / 4$ | $7-1 / 2$ | $8-1 / 4$ | $9-3 / 4$ | $10-1 / 2$ | 12 | 13 |  |  |  |
| 140 | 4 | $4-1 / 4$ | $4-3 / 4$ | $5-1 / 4$ | $5-1 / 2$ | 6 | $7-1 / 4$ | 8 | $9-1 / 2$ | $10-1 / 2$ | $11-3 / 4$ | $12-3 / 4$ |  |  |  |
| 160 | $3-3 / 4$ | $4-1 / 4$ | $4-1 / 2$ | 5 | $5-1 / 4$ | $5-3 / 4$ | 7 | $7-3 / 4$ | $9-1 / 4$ | $10-1 / 4$ | $11-1 / 2$ | $12-1 / 2$ |  |  |  |
| 180 | $3-3 / 4$ | 4 | $4-1 / 2$ | 5 | $5-1 / 4$ | $5-3 / 4$ | 7 | $7-1 / 2$ | 9 | $10-1 / 4$ | $11-1 / 4$ | $12-1 / 4$ |  |  |  |
| 210 | $3-1 / 2$ | 4 | $4-1 / 4$ | $4-3 / 4$ | 5 | $5-1 / 2$ | $6-1 / 2$ | $7-1 / 4$ | $8-3 / 4$ | $9-3 / 4$ | $10-3 / 4$ | $11-3 / 4$ |  |  |  |

# ABOVE-GROUND INSTALLATION <br> OF THERMOPLASTIC PIPING 

Table 62
SUPPORT SPACING "L" (FT.) - Polypro Schedule 80

| TEMP <br> $F$ | NOMINAL PIPE SIZE |  |  |  |  |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | $\mathbf{1 / 2}$ | $\mathbf{3 / 4}$ | $\mathbf{1}$ | $\mathbf{1 - 1 / 4}$ | $\mathbf{1 - 1 / 2}$ | $\mathbf{2}$ | $\mathbf{3}$ | $\mathbf{4}$ | $\mathbf{6}$ | $\mathbf{8}$ | $\mathbf{1 0}$ | $\mathbf{1 2}$ |  |
| 73 | $3-3 / 4$ | 4 | $4-1 / 2$ | $4-3 / 4$ | 5 | $5-1 / 2$ | $6-1 / 2$ | $7-1 / 4$ | $8-1 / 2$ | $9-1 / 2$ | $10-1 / 2$ | $11-1 / 4$ |  |
| 120 | $3-1 / 2$ | $3-3 / 4$ | 4 | $4-1 / 2$ | $4-3 / 4$ | 5 | 6 | $6-3 / 4$ | 8 | $8-3 / 4$ | $9-3 / 4$ | $10-1 / 2$ |  |
| 140 | 3 | $3-1 / 2$ | $3-3 / 4$ | 4 | $4-1 / 4$ | $4-1 / 2$ | $5-1 / 2$ | 6 | $7-1 / 4$ | 8 | $8-3 / 4$ | $9-1 / 2$ |  |
| 160 | 3 | 3 | $3-1 / 2$ | $3-3 / 4$ | 4 | $4-1 / 4$ | $5-1 / 4$ | $5-3 / 4$ | $6-3 / 4$ | $7-1 / 2$ | $8-1 / 4$ | 9 |  |
| 180 | $2-3 / 4$ | 3 | $3-1 / 4$ | $3-1 / 2$ | $3-3 / 4$ | 4 | 5 | $5-1 / 2$ | $6-1 / 2$ | 7 | $7-3 / 4$ | $8-1 / 2$ |  |
| 200 | $2-1 / 2$ | $2-3 / 4$ | 3 | $3-1 / 2$ | $3-1 / 2$ | 4 | $4-3 / 4$ | $5-1 / 4$ | 6 | $6-3 / 4$ | $7-1 / 2$ | 8 |  |
| 212 | $2-1 / 2$ | $2-3 / 4$ | 3 | $3-1 / 4$ | $3-1 / 4$ | $3-3 / 4$ | $4-1 / 2$ | 5 | $5-3 / 4$ | $6-1 / 2$ | $7-1 / 4$ | $7-3 / 4$ |  |

Support spacing subject to change with SDR piping systems and different manufacturers' resins. See manufacturers support spacing guide prior to installation.

Table 63
SUPPORT SPACING "L"(FT.) - Proline \& Super Proline

| PIPE SIZE <br> (IN.) | TEMPERATURE |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | $\begin{aligned} & 68^{\circ} \mathrm{F} / \\ & 20^{\circ} \mathrm{C} \end{aligned}$ | $\begin{aligned} & 86^{\circ} \mathrm{F} / \\ & 30^{\circ} \mathrm{C} \end{aligned}$ | $\begin{gathered} 104^{\circ} \mathrm{F} / \\ 40^{\circ} \mathrm{C} \end{gathered}$ | $\begin{gathered} 122^{\circ} \mathrm{F} / \\ 50^{\circ} \mathrm{C} \end{gathered}$ | $\begin{gathered} 140^{\circ} \mathrm{F} / \\ 60^{\circ} \mathrm{C} \end{gathered}$ | $\begin{gathered} 158^{\circ} \mathrm{F} / \\ 70^{\circ} \mathrm{C} \end{gathered}$ | $\begin{gathered} 176^{\circ} \mathrm{F} / \\ 80^{\circ} \mathrm{C} \end{gathered}$ |
| 1/2 | 3.0 | 2.5 | 2.5 | 2.0 | 2.0 | 2.0 | 2.0 |
| 3/4 | 3.0 | 3.0 | 2.5 | 2.5 | 2.5 | 2.5 | 2.0 |
| 1 | 3.5 | 3.0 | 3.0 | 3.0 | 3.0 | 2.5 | 2.5 |
| 1-1/2 | 4.0 | 3.5 | 3.0 | 3.0 | 3.0 | 3.0 | 3.0 |
| 2 | 4.5 | 4.0 | 4.0 | 3.5 | 3.0 | 3.0 | 3.0 |
| 2-1/2 | 5.0 | 4.5 | 4.0 | 4.0 | 3.5 | 3.0 | 3.0 |
| 3 | 5.5 | 5.0 | 4.0 | 4.0 | 4.0 | 3.5 | 3.5 |
| 4 | 6.0 | 5.0 | 5.0 | 4.0 | 4.0 | 4.0 | 4.0 |
| 6 | 7.0 | 6.0 | 6.0 | 5.0 | 5.0 | 4.5 | 4.5 |
| 8 | 7.5 | 7.0 | 6.0 | 6.0 | 5.5 | 5.0 | 5.0 |
| 10 | 8.5 | 7.5 | 7.0 | 6.5 | 6.0 | 6.0 | 5.5 |
| 12 | 9.5 | 8.5 | 8.0 | 7.0 | 7.0 | 6.5 | 6.0 |
| 14 | 10.0 | 8.5 | 8.0 | 7.5 | 7.0 | 6.5 | 6.5 |
| 16 | 10.5 | 9.5 | 8.5 | 8.0 | 7.5 | 7.0 | 6.5 |
| 18 | 11.5 | 10.0 | 9.0 | 8.5 | 8.0 | 7.5 | 7.0 |
| 20 | 12.0 | 10.5 | 9.5 | 8.5 | 8.5 | 8.0 | 7.5 |
| 24 | 13.5 | 11.5 | 10.0 | 9.5 | 8.5 | 8.0 | 7.5 |

This support spacing chart shows spans for polypropylene (PP) SDR 11, PP SDR 17.6, and PVDF pipes. For PP SDR 32, multiply span times .55 for the reduced value.

The support spacing chart shown above is based on liquids with a specific gravity of 1.0 . Spacing should be reduced by $10 \%$ for liquids having 1.5 specific gravity, $15 \%$ for 2.0 s.q., and $20 \%$ for 2.5 s.q.

Table 64
SUPPORT SPACING "L" (FT.) - PVDF Schedule 80

| TEMP | NOMINAL PIPE SIZE |  |  |  |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| ${ }^{\circ} \mathrm{F}$ | 1/2 | 3/4 | 1 | 1-1/4 | 1-1/2 | 2 | 3 | 4 | 6 | 8 | 10 | 12 |
| 68 | 3-1/2 | 3-3/4 | 4-1/4 | 4-1/2 | 4-3/4 | 5-1/4 | 6-1/2 | 7 | 8-1/2 | 9-1/2 | 10-1/2 | 11-1/4 |
| 120 | 3 | 3-1/4 | 3-3/4 | 4 | 4-1/4 | 4-3/4 | 5-3/4 | 6-1/4 | 7-1/2 | 8-1/4 | 9-1/4 | 10 |
| 160 | 2-3/4 | 3 | 3-1/2 | 3-3/4 | 4 | 4-1/4 | 5-1/4 | 5-3/4 | 6-3/4 | 7-1/2 | 8-1/2 | 9 |
| 200 | 2-1/2 | 2-3/4 | 3 | 3-1/2 | 3-1/2 | 4 | 4-3/4 | 5-1/4 | 6-1/4 | 7 | 7-3/4 | 8-1/4 |
| 240 | 2-1/4 | 2-1/2 | 2-3/4 | 3 | 3-1/4 | 3-1/2 | 4-1/4 | 4-3/4 | 5-1/2 | 6-1/4 | 7 | 7-1/2 |
| 260 | 2-1/4 | 2-1/2 | 2-3/4 | 3 | 3-1/4 | 3-1/2 | 4 | 4-1/2 | 5-1/2 | 6 | 6-3/4 | 7-1/4 |
| 280 | 2 | 2-1/4 | 2-1/2 | 2-3/4 | 3 | 3-1/4 | 4 | 4-1/4 | 5-1/4 | 5-3/4 | 6-1/2 | 7 |

Support spacing subject to change with SDR piping systems and different manufacturers' resins. See manufacturers support spacing guide prior to installation.


NOTE: All tables shown are based in . 100 inch SAG between supports.

## ABOVE-GROUND INSTALLATION OF THERMOPLASTIC PIPING

## PLASTICS AND FIRE (continued)

The surface burning characteristics of building materials are based upon UBC 42-1 Standards and ASTM E-84 testing to provide flame and smoke spread information of plastic material found on page 41.

All plastics melt before they burn when exposed to an open flame, and generate toxic carbon monoxide, non-toxic carbon dioxide, water vapor by-products, and dense smoke. PVC and CPVC also release toxic hydrogen chloride when burned. PVDF and other fluorocarbons release hydrogen fluoride. ABS, nylon and other nitrogen containing polymers release hydrogen cyanide.

An Underwriters Lab approved kaolin clay thermal insulation cloth, which will fireproof any plastic piping system to a 0 flame spread and 0 smoke spread per ASTM E-84 testing, has been used effectively to meet fire codes.

## TABLE 65 FLAME-SPREAD CLASSIFICATION (UBC 1994)

| Class | Flame-Spread Index |
| :---: | :---: |
| I | $0-25$ |
| II | $26-75$ |
| III | $76-200$ |

TABLE 66 MAXIMUM FLAME-SPREAD CLASS
(UBC 1994)

| Occupancy Group | Description Enclo | osed Vertical Exitways | Other Exitways | Rooms or Areas |
| :---: | :---: | :---: | :---: | :---: |
| A | Stadium | I | II | II |
| E | High Schools | I | II | III |
| I | Hospital | 1 | I | II |
| H-1 | High Explosive | 1 | II | III |
| H-2 | Moderate Explosive |  |  |  |
| H-3 | High Fire |  |  |  |
| H-4 | Repair Garage, Not B below |  |  |  |
| H-5 | Aircraft Repair, Not B below |  |  |  |
| H-6 | Semiconductor Fab and |  |  |  |
|  | Research and Development |  |  |  |
| H-7 | Health Hazards - Highly Corrosive or Toxic |  |  |  |
| B-1 | Gas Stations Office Buildings - No highly flammable or combustible materials |  |  |  |
| B-2 |  |  |  |  |
| B-3 | Airplane Hangar, No open flame |  |  |  |
| B-4 | Power Plant, Factories using non-combustible and non-explosive materials |  |  |  |
| R-1 | Hotel, Apartment | II | II | III |
| R-3 | Houses | III | III | III |

## SEISMIC DESIGNS FOR STORAGE TANKS

The Uniform Building Code 1994 edition states: "Flat bottom tanks or other tanks with supported bottoms found at or below grade shall be designed to resist the seismic forces calculated using the procedures in Section 2312 (i) for rigid
structures considering the entire weight of the tanks and its contents." Seismic forces and wind forces tend to topple a tank. These forces must be calculated by a registered engineer and an approved restraint system utilized when installing a tank.


SEISMIC ZONE MAP OF THE UNITED STATES

# ABOVE-GROUND INSTALLATION OF THERMOPLASTIC PIPING 

## SUNLIGHT WEATHERING AND PAINTING

Plastic pipe and fittings have varying resistance to weathering. PVC, CPVC, and Polypropylene undergo surface oxidation and embrittlement by exposure to sunlight over a period of several years. The surface oxidation is evident by a change in pipe color from gray to white. Oxidized piping does not lose any of its pressure capability. It does, however, become much more susceptible to impact damage. PVDF is unaffected by sunlight but is translucent when unpigmented.

PVC and CPVC pipe and fittings can be easily protected from ultraviolet oxidation by painting with a heavily pigmented, exterior water base latex paint. The color of the paint is of no particular importance, as the pigment acts as an ultraviolet screen and prevents sunlight damage. White or some other light color is recommended as it helps reduce pipe temperature. The latex paint must be thickly applied as an opaque coating on the pipe and fittings that have been cleaned well and very lightly sanded.

Polypropylene and PVDF pipe and fittings are very difficult to paint properly and should be protected by insulation.

## THERMAL EFFECTS ON PLASTICS

The physical properties of thermoplastic piping is significantly related to its operating temperature. As the operating temperature falls, the pipe's stiffness and tensile strength increases, increasing the pipe's pressure capacity and its ability to resist earth-loading deflection. With the drop in temperature, impact strength is reduced.

With an increase in temperature, there is a decrease in pipe tensile strength and stiffness and a reduction in pressure capability, as outlined in the Temperature-Pressure charts on page 44.

## THERMAL CONDUCTIVITY, HEAT TRACING AND INSULATION

Plastic piping, unlike metal, is a very poor conductor of heat. Thermal conductivity is expressed as BTU/hr./sq.ft./ ${ }^{\circ} \mathrm{F} / \mathrm{in}$. where BTU/hr. or British Thermal Unit per hour is energy required to raise temperature of 1 pound of water ( 12 gallons $\div$ specific gravity) one Fahrenheit degree in one hour. Sq. ft. refers to 1 square foot where heat is being transferred. Inch refers to 1 inch of pipe wall thickness. As pipe wall increases, thermal conductivity decreases.

A comparison to steel, aluminum, and copper can be seen on page 41. Copper, a good conductor of heat, will lose $2,610 \mathrm{BTU} / \mathrm{hr}$ per square foot of surface area with a wall thickness of 1 inch. PVC will lose only $1.2 \mathrm{BTU} / \mathrm{hr}$ ! If wall thickness is reduced to 0.250 inches, the heat loss increases 4 times.

Although plastics are poor conductors of heat, heat tracing of plastic piping may be necessary to maintain a constant elevated temperature of a viscous liquid, prevent liquid freezing, or to prevent a liquid, such as $50 \%$ sodium hydroxide, from crystallizing in a pipeline at $68^{\circ} \mathrm{F}$. Electric heat tracing with self-regulating, temperature-sensing tape such as Raychem Chemelex Autotrace will maintain a $90^{\circ} \mathrm{F}$ temperature to prevent sodium hydroxide from freezing. The tape should be S-pattern wrapped on the pipe to allow pipe repairs and to avoid deflection caused by heating one side of the pipe. Heat tracing should be applied directly on the pipe within the insulation, and must not exceed the temper-ature-pressure-chemical resistance design of the system.

Insulation to further reduce plastic piping heat loss is available in several different forms from several manufacturers. The most popular is a two half foam insulation installed within a snap together with aluminum casing. Insulation can also provide weathering protection and fireproofing to plastic piping and is discussed later.

## ULTRA-VIOLET LIGHT STERILIZATION

UV sterilizers for killing bacteria in deionized water are becoming common. The intense light generated will stress crack PVC, CPVC, polypropylene, and PVDF piping over time that is directly connected to the sterilizer. PVDF goes through a cross-linking of H-F causing a discoloration of the fitting and pipe material, and joint stress cracking.

## VIBRATION ISOLATION

Plastic piping will conduct vibration from pumping and other sources of resonance frequencies, such as liquid flow through a partially open valve. Vibration isolation is best accomplished using a flanged, teflon, or thin rubber bellows expansion joint installed near the pump discharge or source of vibration. Metallic or thick rubber expansion joints lack the flexibility to provide flange movement and vibration isolation and should not be used in plastic piping systems. The proper bellows expansion joint will also provide for pipe system flexibility against a stationary mounted pump, storage tank, or equipment during an earthquake to reduce pipe breakage.

# BELOW-GROUND INSTALLATION OF THERMOPLASTIC PIPE 

## INTRODUCTION

Many problems experienced by above-ground plastic piping such as weathering/painting, expansion/contraction, pipe support/hangers, fire, and external mechanical damage are virtually eliminated by proper below-ground installation. The depth and width of trenching, bedding and backfilling, thrust blocking, snaking, air and pressure relief, and size and wall thickness of pipe must be considered.

## TRENCHING AND BEDDING DEPTH

In installing underground piping systems, the depth of the trench is determined by the intended service and by local conditions (as well as by local, state and national codes that may require a greater trench depth and cover than are technically necessary).

Underground pipes are subjected to external loads caused by the weight of the backfill material and by loads applied at the surface of the fill. These can range from static to dynamic loads.

Static loads comprise the weight of the soil above the top of the pipe plus any additional material that might be stacked above ground. An important point is that the load on a flexible pipe will be less than on a rigid pipe buried in the same manner. This is because the flexible conduit transfers part of the load to the surrounding soil and not the reverse. Soil loads are minimal with narrow trenches until a pipe depth of 10 feet is attained.

Dynamic loads are loads due to moving vehicles such as trucks, trains and other heavy equipment. For shallow burial conditions live loads should be considered and added to static loads, but at depths greater than 10 feet, live loads have very little effect.

Pipe intended for potable water service should be buried at least 12 inches below the maximum expected frost penetration.

## WIDTH

The width of the trench should be sufficient to provide adequate room for "snaking" $1 / 2$ to $2-1 / 2$ inch nominal diameter pipe from side to side along the trench bottom, as described below, and for placing and compacting the side fills. The trench width can be held to a minimum with most pressure piping materials by joining the pipe at the surface and then lowering it into the trench after adequate joint strength has been obtained.

## BEDDING

The bottom of the trench should provide a firm, continuous bearing surface along the entire length of the pipe run. It should be relatively smooth and free of rocks. Where hardpan, ledge rock or boulders are present, it is recommended that the trench bottom be cushioned with at least four (4) inches of sand or compacted fine-grained soils.

## SNAKING

To compensate for thermal expansion and contraction when laying small diameter pipe in hot weather, the snaking technique of offsetting $1 / 2$ to $2-1 / 2$ inch nominal diameter pipe with relation to the trench center line is recommended.
A. 1/2 inch to 2-1/2 inch nominal diameter. When the installation temperature is substantially lower than the operating temperature, the pipe should, if possible, be installed with straight alignment and brought up to operating temperature after joints are properly cured but before backfilling. This procedure will permit expansion of the pipe to be accommodated by a "snaking" action.

When the installation temperature is substantially above the operating temperature, the pipe should be installed by snaking in the trench. For example, a 100 -foot length of PVC Type 1 pipe will expand or contract about $3 / 4$ inch for each $20^{\circ} \mathrm{F}$ temperature change. On a hot summer day, the direct rays of the sun on the pipe can drive the surface temperature up to $150^{\circ} \mathrm{F}$. At night, the air temperature may drop to $70^{\circ} \mathrm{F}$. In this hypothetical case, the pipe would undergo a temperature change of $80^{\circ} \mathrm{F}$ and every 100 feet of pipe would contract 3 inches overnight. This degree of contraction would put such a strain on newly cemented pipe joints that a poorly made joint might pull apart.

A practical and economical method is to cement the line together at the side of the trench during the normal working day. When the newly cemented joint has dried, the pipe is snaked from one side of the trench to the other in gentle alternate curves. This added length will compensate for any contraction after the trench is backfilled. See Figure 13.
B. 3 inch and larger nominal diameter pipes should be installed in straight alignment. Before backfilling to the extent that longitudinal movement is restricted, the pipe temperature should be adjusted to within $15^{\circ} \mathrm{F}$ of the operating temperature, if possible.

## BELOW-GROUND INSTALLATION OF THERMOPLASTIC PIPING

FIGURE 13
Table shown below gives the required loop length in feet and offset in inches for various temperature variations.

Snaking of thermoplastic pipe within trench to compensate for thermal expansion and contraction.


Table 67
SNAKING LENGTH VS. OFFSET (IN.) TO COMPENSATE FOR THERMAL CONTRACTION

| SNAKING <br> LENGTH <br> (FT.) | MAXIMUM TEMPERATURE VARIATION ( ${ }^{\circ}$ F) BETWEEN TIME OF CEMENTING AND FINAL BACKFILLING |  |  |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | $10^{\circ}$ | $20^{\circ}$ | $30^{\circ}$ | $40^{\circ}$ | $50^{\circ}$ | $60^{\circ}$ | $70^{\circ}$ | $80^{\circ}$ | $90^{\circ}$ | $100^{\circ}$ |
|  | LOOP OFFSET (IN.) |  |  |  |  |  |  |  |  |  |
| 20 | 2.5 | 3.5 | 4.5 | 5.20 | 5.75 | 6.25 | 6.75 | 7.25 | 7.75 | 8.00 |
| 50 | 6.5 | 9.0 | 11.0 | 12.75 | 14.25 | 15.50 | 17.00 | 18.00 | 19.25 | 20.25 |
| 100 | 13.0 | 18.0 | 22.0 | 26.00 | 29.00 | 31.50 | 35.00 | 37.00 | 40.00 | 42.00 |



DETERMINING SOIL LOADING FOR FLEXIBLE PLASTIC PIPE, SCHEDULE 80
Underground pipes are subjected to external loads caused by the weight of the backfill material and by loads applied at the surface of the fill. These can range from static to dynamic loads.

Static loads comprise the weight of the soil above the top of the pipe plus any additional material that might be stacked above ground. An important point is that the load on a flexible pipe will be less than on a rigid pipe buried in the same manner. This is because the flexible conduit transfers part of the load to the surrounding soil and not the reverse. Soil loads are minimal with narrow trenches until a pipe depth of 10 feet is attained.

Dynamic loads are loads due to moving vehicles such as trucks, trains and other heavy equipment. For shallow burial conditions live loads should be considered and added to static loads, but at depths greater than 10 feet, live loads have very little effect.

Soil load and pipe resistance for other thermoplastic piping products can be calculated using the following formula or using Tables $68 \& 69$.

$$
\begin{aligned}
\text { Wc' } & =\frac{\Delta X\left(E I+.061 \mathrm{E}^{\prime} r^{3}\right) 80}{r^{3}} \\
\text { Wc' } & =\text { Load Resistance of the Pipe, Ib./ft. } \\
\Delta x & =\text { Deflection in Inches @ } 5 \% ~(.05 \times \text { I.D. }) \\
\mathrm{E} & =\text { Modulus of Elasticity } \\
\mathrm{t} & =\text { Pipe Wall Thickness, in. } \\
\mathrm{r} & =\text { Mean Radius of Pipe (O.D. -t }) / 2 \\
\mathrm{E}^{\prime} & =\text { Modulus of Passive Soil Resistance, psi } \\
\mathrm{H} & =\text { Height of Fill Above Top of Pipe, ft. } \\
\mathrm{I} & =\text { Moment of } \frac{\text { Inertia } \mathrm{t}^{3}}{12}
\end{aligned}
$$

TABLE 68
LIVE LOAD FOR BURIED FLEXIBLE PIPE (LB/LIN.FT)

| PIPE <br> SIZE | H20 WHEEL LOADS FOR VARIOUS <br> DEPTHS OF PIPE (LB./LIN.FT.) |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  | $\mathbf{2}$ | $\mathbf{4}$ | $\mathbf{6}$ | $\mathbf{8}$ | $\mathbf{1 0}$ |
|  | 309 | 82 | 38 | 18 | 16 |
| $\mathbf{3}$ | 442 | 118 | 56 | 32 | 21 |
| $\mathbf{4}$ | 574 | 154 | 72 | 42 | 27 |
| $\mathbf{6}$ | 837 | 224 | 106 | 61 | 40 |
| $\mathbf{8}$ | 1102 | 298 | 141 | 82 | 53 |
| $\mathbf{1 0}$ | 1361 | 371 | 176 | 101 | 66 |
| $\mathbf{1 2}$ | 1601 | 440 | 210 | 120 | 78 |

NOTE: H20 wheel load is $16,000 \mathrm{lb} . /$ wheel

## BELOW-GROUND INSTALLATION OF THERMOPLASTIC PIPING

TABLE 69
SOIL LOAD AND PIPE RESISTANCE FOR FLEXIBLE THERMOPLASTIC PIPE PVC Schedule 40 and 80 Pipe

| NOM. SIZE <br> (IN.) | $\begin{gathered} \text { Wc' = LOAD RESISTANCE OF } \\ \text { PIPE (LB./FT.) } \end{gathered}$ |  |  |  | $\begin{gathered} \mathrm{H} \\ \text { (FT) } \end{gathered}$ | Wc = SOIL LOADS AT VARIOUS TRENCH WIDTHS AT TOP OF PIPE (LB./FT.) |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | $E^{\prime}=200$ | E'=700 | E'=200 | $E^{\prime}=700$ |  | 2 FT | 3 FT | 4 FT | 5 FT |
| 1-1/2 | 1084 | 1282 | 2809 | 2993 | $\begin{aligned} & 10 \\ & 20 \\ & 30 \\ & 40 \end{aligned}$ | $\begin{array}{r} 106 \\ 138 \\ 144 \\ - \end{array}$ | $\begin{aligned} & 125 \\ & 182 \\ & 207 \\ & 214 \end{aligned}$ | $\begin{aligned} & 136 \\ & 212 \\ & 254 \\ & 269 \end{aligned}$ | $\begin{aligned} & 152 \\ & 233 \\ & 314 \\ & 318 \end{aligned}$ |
| 2 | 879 | 1130 | 2344 | 2581 | $\begin{aligned} & 10 \\ & 20 \\ & 30 \\ & 40 \end{aligned}$ | $\begin{aligned} & 132 \\ & 172 \\ & 180 \\ & - \end{aligned}$ | $\begin{aligned} & 156 \\ & 227 \\ & 259 \\ & 267 \end{aligned}$ | $\begin{aligned} & 170 \\ & 265 \\ & 317 \\ & 337 \end{aligned}$ | $\begin{aligned} & 190 \\ & 291 \\ & 392 \\ & 398 \end{aligned}$ |
| 2-1/2 | 1344 | 1647 | 3218 | 3502 | $\begin{aligned} & 10 \\ & 20 \\ & 30 \\ & 40 \end{aligned}$ | $\begin{aligned} & 160 \\ & 204 \\ & 216 \end{aligned}$ | $\begin{aligned} & 191 \\ & 273 \\ & 306 \\ & 323 \end{aligned}$ | $\begin{aligned} & 210 \\ & 321 \\ & 377 \\ & 408 \end{aligned}$ | $\begin{aligned} & 230 \\ & 352 \\ & 474 \\ & 482 \end{aligned}$ |
| 3 | 1126 | 1500 | 2818 | 3173 | $\begin{aligned} & 10 \\ & 20 \\ & 30 \\ & 40 \end{aligned}$ | $\begin{gathered} 196 \\ 256 \\ 266 \\ - \end{gathered}$ | $\begin{aligned} & 231 \\ & 336 \\ & 266 \\ & 394 \end{aligned}$ | $\begin{aligned} & 252 \\ & 392 \\ & 384 \\ & 497 \end{aligned}$ | $\begin{aligned} & 280 \\ & 429 \\ & 469 \\ & 586 \end{aligned}$ |
| 3-1/2 | 1021 | 1453 | 2591 | 3002 | $\begin{aligned} & 10 \\ & 20 \\ & 30 \\ & 40 \end{aligned}$ | $\begin{gathered} 223 \\ 284 \\ 300 \\ - \end{gathered}$ | $\begin{aligned} & 266 \\ & 380 \\ & 426 \\ & 450 \end{aligned}$ | $\begin{aligned} & 293 \\ & 446 \\ & 524 \\ & 568 \end{aligned}$ | $\begin{aligned} & 320 \\ & 490 \\ & 660 \\ & 670 \end{aligned}$ |
| 4 | 969 | 1459 | 2456 | 2922 | $\begin{aligned} & 10 \\ & 20 \\ & 30 \\ & 40 \end{aligned}$ | $\begin{gathered} 252 \\ 328 \\ 342 \\ - \end{gathered}$ | $\begin{aligned} & 297 \\ & 432 \\ & 493 \\ & 506 \end{aligned}$ | $\begin{aligned} & 324 \\ & 540 \\ & 603 \\ & 639 \end{aligned}$ | $\begin{aligned} & 360 \\ & 551 \\ & 743 \\ & 754 \end{aligned}$ |
| 5 | 896 | 1511 | 2272 | 2861 | $\begin{aligned} & 10 \\ & 20 \\ & 30 \\ & 40 \end{aligned}$ | $\begin{gathered} 310 \\ 395 \\ 417 \\ - \end{gathered}$ | $\begin{aligned} & 370 \\ & 529 \\ & 592 \\ & 625 \end{aligned}$ | $\begin{aligned} & 407 \\ & 621 \\ & 730 \\ & 790 \end{aligned}$ | $\begin{aligned} & 445 \\ & 681 \\ & 918 \\ & 932 \end{aligned}$ |
| 6 | 880 | 1620 | 2469 | 3173 | $\begin{aligned} & 10 \\ & 20 \\ & 30 \\ & 40 \end{aligned}$ | $\begin{aligned} & 371 \\ & 484 \\ & 503 \\ & - \end{aligned}$ | $\begin{aligned} & 437 \\ & 636 \\ & 725 \\ & 745 \end{aligned}$ | $\begin{aligned} & 477 \\ & 742 \\ & 888 \\ & 941 \end{aligned}$ | $\begin{array}{\|c} 530 \\ 812 \\ 1093 \\ 1110 \end{array}$ |
| 8 | 911 | 1885 | 2360 | 3290 | $\begin{aligned} & 10 \\ & 20 \\ & 30 \\ & 40 \end{aligned}$ | $\begin{aligned} & 483 \\ & 630 \\ & 656 \end{aligned}$ | $\begin{aligned} & 569 \\ & 828 \\ & 945 \\ & 970 \end{aligned}$ | $\begin{gathered} 621 \\ 966 \\ 1156 \\ 1225 \end{gathered}$ | $\begin{array}{\|c} 690 \\ 1057 \\ 1423 \\ 1445 \end{array}$ |
| 10 | 976 | 2198 | 2597 | 3764 | $\begin{aligned} & 10 \\ & 20 \\ & 30 \\ & 40 \end{aligned}$ | $\begin{gathered} 602 \\ 785 \\ 817 \\ - \end{gathered}$ | $\begin{gathered} 710 \\ 1032 \\ 1177 \\ 1209 \end{gathered}$ | $\begin{array}{\|c\|} \hline 774 \\ 1204 \\ 1405 \\ 1527 \end{array}$ | $\begin{array}{\|c} 860 \\ 1317 \\ 1774 \\ 1801 \end{array}$ |
| 12 | 1058 | 2515 | 2909 | 4298 | $\begin{aligned} & 10 \\ & 20 \\ & 30 \\ & 40 \end{aligned}$ | $\begin{gathered} 714 \\ 931 \\ 969 \\ - \end{gathered}$ | $\begin{gathered} 942 \\ 1225 \\ 1397 \\ 1434 \end{gathered}$ | $\begin{array}{\|c} 919 \\ 1429 \\ 1709 \\ 1811 \end{array}$ | $\begin{aligned} & 1020 \\ & 1562 \\ & 2104 \\ & 2136 \end{aligned}$ |

NOTE 1: Figures are calculated from minimum soil resistance values ( $E^{\prime}=200 \mathrm{psi}$ for uncompacted sandy clay foam) and compacted soil ( $E^{\prime}=700$ for side-fill that is compacted to $90 \%$ or more of Proctor Density for distance of two pipe diameters on each side of the pipe). If Wc' is less than Wc at a given trench depth and width, then soil compaction will be necessary
NOTE 2: These are soil loads only and do not include live loads.


## HEAVY TRAFFIC

When plastic pipe is installed beneath streets, railroads, or other surfaces that are subjected to heavy traffic and resulting shock and vibration, it should be run within a protective metal or concrete casing.

## HYDROSTATIC PRESSURE TESTING

Plastic pipe is not designed to provide structural strength beyond sustaining internal pressures up to its designed hydrostatic pressure rating and normal soil loads. Anchors, valves, and other connections must be independently supported to prevent added shearing and bending stresses on the pipe.

## RISERS

The above piping design rule applies also where pipe is brought out of the ground. Above-ground valves or other connections must be supported independently. If pipe is exposed to external damage, it should be protected with a separate, rigidly supported metal pipe sleeve at the danger areas. Thermoplastic pipe should not be brought above ground where it is exposed to high temperatures. Elevated temperatures can lower the pipes pressure rating below design levels.

## LOCATING BURIED PIPE

The location of plastic pipelines should be accurately recorded at the time of installation. Since pipe is a non-conductor, it does not respond to the electronic devices normally used to locate metal pipelines. However, a copper or galvanized wire can be spiraled around, taped to, or laid alongside or just above the pipe during installation to permit the use of a locating device, or use marker tape.

NOTE: For additional information see ASTM D-2774, "Underground Installation of Thermoplastic Pressure Piping."

## TESTING THERMOPLASTIC PIPING SYSTEMS

We strongly recommend that all plastic piping systems be hydrostatically tested as described below before being put into service. Water is normally used as the test medium. Note: Do not pressure test with compressed air or gas! Severe damage or bodily injury can result.

The water is introduced through a pipe of 1-inch diameter or smaller at the lowest point in the system. An air relief valve should be provided at the highest point in the system to bleed off any air that is present.

The piping system should gradually be brought up to the desired pressure rating using a pressure bypass valve to assure against over pressurization. The test pressure should in no event exceed the rated operating pressure of the lowest rated component in the system such as a 150 -pound flange.

## INITIAL LOW-PRESSURE TEST

The initial low-pressure hydrostatic test should be applied to the system after shallow back-filling which leaves joints exposed. Shallow back-filling eliminates expansion/contraction problems. The test should last long enough to determine that there are no minute leaks anywhere in the system.

## PRESSURE GAUGE METHOD

Where time is not a critical factor, the reading of a regular pressure gauge over a period of several hours will reveal any small leaks. If the gauge indicates leakage, that entire run of piping must then be visually inspected - paying special attention to the joints - to locate the source of the leak.

## VISUAL INSPECTION METHOD

After the line is pressurized, it can be visually inspected for leaks without waiting for the pressure gauge to reveal the presence or absence of a pressure drop.

Even though no leaks are found during the initial inspection, however, it is recommended that the pressure be maintained for a reasonable length of time. Checking the gauge several times during this period will reveal any slow developing leaks.

## LOCATE ALL LEAKS

Even though a leak has been found and the pipe or joint has been repaired, the low-pressure test should be continued until there is a reasonable certainty that no other leaks are present. Locating and repairing leaks is very much more difficult and expensive after the piping system has been buried. Joints should be exposed during testing.

## HIGH-PRESSURE TESTING

Following the successful completion of the low-pressure test, the system should be high-pressure tested for at least 12 hours. The run of pipe should be more heavily backfilled to prevent movement of the line under pressure. Since any leaks that may develop probably will occur at the fitting joints, these should be left uncovered.

Solvent-cemented piping systems must be fully cured before pressure testing. For cure times, refer to the solvent cementing instruction tables on page 84.

## TEST PRESSURE

The test pressure applied should not exceed: (a) the designed maximum operating pressure, (b) the designed pressure rating of the pipe, (c) the designed pressure rating of any system component, whichever is lowest.

## SAFETY PRECAUTIONS

(1) Do not test with fluid velocities exceeding 5 ft ./sec. since excessive water hammer could damage the system. (2) Do not allow any personnel not actually working on the highpressure test in the area, in case of a pipe or joint rupture.
(3) Do not test with air or gas.

## TRANSITION FROM PLASTIC TO OTHER MATERIALS

Transitions from plastic piping to metal piping may be made with flanges, threaded fittings, or unions. Flanged connections are limited to 150 psi, and threaded connections are limited to $50 \%$ of the rated pressure of the pipe.

NOTE: When tying into a threaded metal piping system, it is recommended that a plastic male thread be joined to a metal female thread. Since the two materials have different coefficients of expansion, the male plastic fitting will actually become tighter within the female metal fitting when expansion occurs.


DO NOT TEST WITH AIR OR COMPRESSED GAS.

# INSTALLATION OF THERMOPLASTIC PIPING SYSTEMS HANDLING \& STORAGE PLASTIC PIPE 

Normal precautions should be taken to prevent excessive mechanical abuse. However, when unloading pipe from a truck, for example, it is unwise to drag a length off the tailgate and allow the free end to crash to the ground. Remember, too, that SCRATCHES AND GOUGES ON THE PIPE SURFACE CAN LEAD TO REDUCED PRESSURE-CARRYING CAPACITY. Standard pipe wrenches should not be used for making up threaded connections since they can deform or scar the pipe. Use strap wrenches instead. When using a pipe vise or chuck, wrap jaws with emery cloth or soft metal.

Pipe should be stored on racks that afford continuous support and prevent sagging or draping of longer lengths. Burrs and sharp edges of metal racks should be avoided. Plastic fittings and flanges should be s ${ }^{\circ} A ́$, Bê4 $4^{\circ} A ́ A ̂ ’ \sum$ «?Ëkÿ4*ùíl $\sum 3$ )ı̀ À À ÀPÔ , 0ốn $\approx \rightarrow$.rÚ\$ $1+$; jÛ\% $\%+$ qiت̂
Û…

## FIELD STACKING

During prolonged field storage of loose pipe, its stacks should not exceed two feet in height. Bundled pipe may be doublestacked providing its weight is distributed by its packaging boards.

## HANDLING

Care should be exercised to avoid rough handling of pipe and fittings. They should not be pushed or pulled over sharp projections, dropped or have any objects dropped upon them. Particular care should be taken to avoid kinking or buckling the pipe. Any kinks or buckles which occur should be removed by cutting out the entire damaged section as a cylinder. All sharp edges on a pipe carrier or trailer that could come in contact with the pipe should be padded; i.e., can use old fire hose or heavy rubber strips. Only nylon or rope slings should be used for lifting bundles of pipe; chains are not to be used.

## INSPECTION

Before installation, all lengths of pipe and fittings should be thoroughly inspected for cuts, scratches, gouges, buckling, and any other imperfections which may have been imparted to the pipe during shipping, unloading, storing, and stringing. Any pipe or pre-coupled fittings containing harmful or even questionable defects should be removed by cutting out the damaged section as a complete cylinder.

## JOINING TECHNIQUES <br> FOR THERMOPLASTIC PIPE

There are six recommended methods of joining thermoplastic pipe and fittings, each with its own advantages and limitations:

## SOLVENT CEMENTING

The most widely used method in Schedule 40 PVC, Schedule 80 PVC and CPVC piping systems as described in ASTM D-285593. The O.D. of the pipe and the I.D. of the fitting are primed, coated with special cement and joined together, as described in detail below. Knowledge of the principles of solvent cementing is essential to a good job. These are discussed in the Solvent Welding Instructions Section.
NOTE: The single most significant cause of improperly or failed solvent cement joints is lack of solvent penetration or inadequate primer application.

## THREADING

Schedule 80 PVC, CPVC, PVDF, and PP can be threaded with special pipe dyes for mating with Schedule 80 fittings provided with threaded connections. Since this method makes the piping system easy to disassemble, repair, and test, it is often employed on temporary or take-down piping systems, as well as systems joining dissimilar materials. However, threaded pipe must be derated by 50 percent from solvent-cemented systems. (Threaded joints are not recommended for PP pressure applications.)

## FLANGES

Flanges are available for joining all thermoplastic piping systems. They can be joined to the piping either with solvent-cemented or threaded connections. Flanging offers the same general advantages as threading and consequently is often employed in piping systems that must frequently be dismantled. The technique is limited to $\mathbf{1 5 0}$ psi working pressure.

## BUTT FUSION

This technique us used to connect all sizes of Polypropylene (Proline), PVDF (Super Proline) and large diameter Fuseal. Butt fusion is an easy, efficient fusion method especially in larger diameters.

## SOCKET FUSION

This technique is used to assemble PVDF and polypropylene pipe and fittings for high-temperature, corrosive-service applications. (See each material Design Data section for recommended joining technique.)

## FUSEAL HEAT FUSION

$R \& G$ Sloane's Fuseal is a patented method of electrically fusing pipe and fitting into a single homogenous unit. This advanced technique is used for GSR Fuseal polypropylene corrosive waste-handling systems.

## FUSEAL MECHANICAL JOINT

Mechanical Joint polypropylene drainage system is used extensively for accessible smaller sized piping areas. The system, as the name implies, is a mechanical sealed joint that consists of a seal-ring, grab-ring, and nut. It is quick and easy to install and can be disconnected just as easily. You will find it most suitable for under sink and under counter piping.

## INSTALLATION OF THERMOPLASTIC PIPING SYSTEMS BASIC PRINCIPLES OF SOLVENT CEMENTING

## SAFETY PRECAUTIONS

Cements contain highly volatile solvents which evaporate rapidly. Avoid breathing the vapors. If necessary, use a fan to keep the work area clear of fumes. Avoid skin or eye contact. Do not use near heat, sparks, or open flame. Do not pressure test with compressed air or gas! Severe damage or bodily injury can result.

Solvent cementing is a preferred method of joining rigid PVC (Polyvinyl Chloride) and CPVC (Chlorinated Polyvinyl Chloride) pipe and fittings providing a chemically fused joint. The solvent-cemented joint is the last vital link in the installation process. It can mean the success or failure of the whole system. Accordingly, it requires the same professional care and attention that is given to the other components of the system. Experience shows that most field failures of plastic piping systems are due to improperly made solventcemented joints.

There are step-by-step procedures on just how to make sol-vent-cemented joints shown on the following pages. However, we feel that if the basic principles involved are first explained and understood, better quality installation can result with ease. To consistently make good joints, the following basics should be clearly understood by the installer.

1. The joining surfaces must be clean, then softened and made semi-fluid.
2. Sufficient cement must be applied to fill the gap between pipe and fittings.
3. Assembly of pipe and fittings must be made while the surfaces are still wet and fluid.
4. Joint strength develops as the cement dries. In the tight part of the joint the surfaces will tend to fuse together. In the loose part the cement will bond to both surfaces.

Penetration and softening should be achieved with a suitable primer such as P70. Primer will penetrate and soften the surfaces more quickly than cement alone. Primer also provides a safety factor for the installer, as he can know under various temperature conditions when he has achieved sufficient softening of the material surfaces. For example, in cold weather more time and additional applications of primer will be required.

More than sufficient cement to fill the loose part of the joint must be applied. Besides filling the gap, adequate cement layers will penetrate the surface and also remain wet until the joint is assembled. Prove this for yourself. Apply on the top surface of a piece of pipe two separate layers of cement. First, flow on a heavy layer of cement, then alongside it a thin brushed out layer. Test the layers every 15 seconds or so by a gentle tap with your finger. You will note that the thin layer becomes tacky and dries quickly (probably within 15 seconds). The heavy layer will remain wet much longer. Now check for penetration a few minutes after applying these layers. Scrape them with a knife. The thin layer will have achieved little or no penetration, the heavy one much more penetration.


If the cement coating on the pipe and fittings are wet and fluid when assembly takes place, they will tend to flow together and become one cement layer. Also, if the cement is wet the surface beneath them will be soft, and these softened surfaces in the tight part of the joint will tend to fuse together.


As the solvent dissipates, the cement layer and the softened surfaces will harden with a corresponding increase in joint strength. A good joint will take the required pressure long before the joint is fully dry and final strength is obtained. In the tight (fused) part of the joint, strength will develop more quickly than in the loose (bonded) part of the joint. Information about the development of the bond strength of solvent-cemented joints is available on request.


## INSTALLATION OF THERMOPLASTIC PIPING SYSTEMS SOLVENT CEMENTING INSTRUCTIONS FOR PVC AND CPVC PIPE AND FITTINGS

Before commencing work, this entire section should be studied and thoroughly understood. It is important that workers making joints be knowledgeable of these instructions and follow them carefully. Do not take shortcuts or omit any of the detailed steps.

## KNOW YOUR MATERIAL

There are two general types of rigid vinyl materials, PVC and CPVC. Fitting are made of both materials and in both Schedule 40 and Schedule 80 weights.

Because of the difference in socket dimensions between the Schedule 40 and Schedule 80 fittings, more care must be taken with the Schedule 80 fittings and the cure schedules are different. Determine before proceeding with the job which type of vinyl plastic you are working with and which weight of fitting.

## HANDLING CEMENTS AND PRIMERS

Cements and primers contain highly volatile solvents which evaporate rapidly. Avoid breathing the vapors. If necessary, use a fan to keep the work area clear of fumes. Avoid skin or eye contact. Keep cans closed when not actually in use. Solvent cements are formulated to be used "as received" in the original containers. If the cement thickens much beyond its original consistency, discard it. Cement should be free flowing, not jelly-like. Do not attempt to dilute it with thinner, as this may change the character of the cement and make it ineffective. Caution: Solvent cement has limited shelf life, usually one year for CPVC and two years for PVC. Date of manufacture is usually stamped on the bottom of the can. Do not use the cement beyond the period recommended by the manufacturer. Always keep solvent cements and primers out of the reach of children.

## SELECTION OF CEMENTS, PRIMERS AND APPLICATORS

1. Obtain the correct primer and solvent cement for the product being installed. (See Harrington's Catalog for detailed information on solvent cements and primers.)

PVC
(a) Use \#P-70 purple primer for all sizes of PVC pipe and fittings.
(b) Use \#710 clear, light-bodied cement with PVC Schedule 40 fittings having an interference fit through 2 " size. Not for use on Schedule 80.
(c) Use \#705 clear, medium-bodied cement with PVC Schedule 40 fittings having an interference fit though 6" size. Not for use on Schedule 80.
(d) Use \#711 gray, heavy-bodied cement with PVC Schedule 80 fittings through 8" and Schedule 40 fittings 6 " and 8 " size.
(e) Use \#719 gray, extra-heavy-bodied cement for Schedule 40,80 , and all class or schedule sizes over 8 " size.

CPVC
(a) Use \#P-70 purple primer for all sizes of CPVC pipe and fittings except copper tube size CPVC (which requires \#P-72 or 729).
(b) Use \#714 orange or gray, heavy-bodied cement for all sizes of CPVC pipe and fittings.
2. Obtain the correct primer applicators. (See Harrington's Catalog for applicators.) Generally, the applicator should be about $1 / 2$ the pipe diameter.
(a) Use \#DP-75, 3/4" diameter, dauber (Supplied with pint size cans of $\mathrm{P}-70$ primer.) for pipe sizes thru $11 / 4^{\prime \prime}$.
(b) Use \#DP-150, 1 1/2" diameter, dauber for pipe sizes through 3".
(c) Use \#4020 cotton string mop for pipe sizes 4" and larger.

Low VOC 724 cement for hypochlorite service.
Weld-on 724 CPVC low VOC cement is a gray, medium bodied, fast setting solvent cement used for joining CPVC industrial piping through 12" diameter, and is specially formulated for services that include caustics and hypochlorites.
3. Obtain the correct solvent cement applicators. Generally, the applicator should be about $1 / 2$ the pipe diameter.

(a) Use \#DP-75 3/4" diameter dauber or a natural bristle brush for pipe sizes $1 / 2^{\prime \prime}$ through 1-1/4"
(b) Use \#DP-150 1-1/2" diameter dauber for pipe sizes $3 / 4$ " through 3". (1" natural bristle brush may be used for pipe sizes up to 2".).
(c) Use \#3020, 2" diameter, "Roll-A-Weld" roller for 3" through 6" pipe sizes.
(d) Use \#7020 7" long roller or \#4020 large cotton swab for 6 " through 12 " pipe sizes.
(e) Use extra-large natural bristle paint brush to flow cement onto pipe larger than $12^{\prime \prime}$.

## INSTALLATION OF THERMOPLASTIC PIPING SYSTEMS SOLVENT CEMENTING INSTRUCTIONS FOR PVC AND CPVC PIPE AND FITTINGS

## PREPARATION

Condition pipe and fittings to the same temperature.


1. Cut pipe square to desired length using a hand saw and miter box or mechanical cutoff saw. A diagonal cut reduces the bonding area in the most effective part of the joint.

2. Plastic tubing cutters may also be used for cutting plastic pipe. However, most produce a raised bead at the end of the pipe. This must be removed with a file, knife, or beveling tool. A raised bead will wipe the cement away when the pipe is inserted into the fitting.

3. Large diameter pipe should be cut and chamfered with appropriate power tools. See Harrington's Products Catalog for tools.


- For $3 / 8$ " to 8 " pipe $-1 / 16$ " to $3 / 32$ "
- For 10 " to 30 " pipe $-1 / 4$ " to $5 / 8$ "

4. Chamfer end of the pipe as shown above.

5. Clean and dry pipe and fitting socket of all dirt, moisture, and grease. Use a clean, dry rag.

Check pipe and fitting for fit (dry) before cementing. For proper interference fit, the pipe must go into the fitting $1 / 3$ to $3 / 4$ of the way to the stop. Too tight of a fit is not desirable. You must be able to fully bottom the pipe into the socket after it has been softened with primer. If the pipe and fitting are not out of round, a satisfactory joint can be made if there is a "net" fit. That is, the pipe bottoms in the fitting socket with no interference, but without slop. All pipe and fitting must conform to ASTM or other standards.

## INSTALLATION OF THERMOPLASTIC PIPING SYSTEMS solvent cementing instructions for pvc and cpvc pipe and fittings

## PRIMING

7. The purpose of the primer is to penetrate and soften the surfaces so that they can fuse together. The proper use of the primer and checking of its softening effect provides assurance that the surfaces are prepared for fusion in a wide variety of temperatures and working conditions.


Before starting the installation, we recommend checking the penetration and softening effect of the primer on a scrap piece of the material you will be working with. This should be done where the temperature and environmental conditions are the same as those where the actual installation will take place. The effect of the primer on the surface will vary with both time and temperature. To check for proper penetration and softening, apply primer as indicated in step number 9. After applying primer, use a knife or sharp scraper and draw the edge over the coated surface. Proper penetration has been made if you can scratch or scrape a few thousandths of an inch of the primed surface away.

8. Using the correct applicator as previously mentioned, apply primer freely with a scrubbing motion to the fitting socket, keeping the surface and applicator wet until the surface has been softened. This usually requires $5-15$ seconds. More time is needed for hard surfaces (found in belled-end pipe and fittings made from pipe stock) and in cold weather conditions. Redip the applicator in the primer as required.

When the surface is primed, remove any puddles of primer from the socket. Puddles of primer can weaken the pipe and/or joint itself.

9. Apply the primer to the end of the pipe equal to the depth of the fitting socket. Application should be made in the same manner as was done to the fitting socket. Be sure the entire surface is well dissolved or softened.
10. Apply a second application of primer to the fitting socket and immediately, while the surfaces are still wet, apply the appropriate solvent cement. Time becomes important at this stage. Do not allow cement or primer to dry or start forming film on the surface.

## CEMENTING

11. Apply a liberal coat of solvent cement to the male end of the pipe. Flow the cement on with the applicator. Do not brush cement out to a thin paint-type layer that will dry in a few seconds. The amount should be more than sufficient to fill any gap between the pipe and fitting.


## INSTALLATION OF THERMOPLASTIC PIPING SYSTEMS SOLVENT CEMENTING INSTRUCTIONS FOR PVC AND CPVC PIPE AND FITTINGS

12. Apply a medium layer of solvent cement to the fitting socket; avoid puddling cement in the socket. On bell-end pipe do not coat beyond the socket depth or allow cement to run down in the pipe beyond the bell.

13. Apply a second full, even coat of solvent cement to the male end of the pipe. There must be sufficient cement to fill any gap in the joint. The cement must be applied deliberately but without delay. It may be necessary for two men to work together when cementing three inch and larger pipe.

14. While both the inside of the socket and the outside surface of the male end of the pipe are soft and wet with cement, forcefully bottom the male end of the pipe into the socket. Give the male end of the pipe a one-quarter turn if possible. This will help drive any air bubbles out of the joint. The pipe must go into the bottom of the socket and stay there. Hold the joint together until both soft surfaces are firmly gripped. (Usually less than 30 seconds on small diameter piping, larger sizes will require more time.) Care must be used since the fitting sockets are tapered and the pipe will try to push out of the fitting just after assembly.

When solvent cementing large diameter (8 inch and above) pipe and fittings proper equipment should be used. We recommend using straps and come-alongs as shown. See the tool section of the Harrington catalog.

15. After assembly a properly made joint will normally show a ring or bead of cement completely around the juncture of the pipe and fitting. Any gaps at this point may indicate a defective assembly job, due to insufficient cement or the use of light bodied cement on larger diameters where heavy bodied cement should have been used.

16. Without disturbing the joint, use a rag and remove excess cement from the pipe at the end of the fitting socket. This includes the ring or bead noted earlier. This excess cement will not straighten the joint and may actually cause needless softening of the pipe and additional cure times.
17. Handle newly assembled joints carefully until initial set has taken place. Recommended setting time allowed before handling or moving is related to temperature. See initial set times (Table 70).
18. Allow the joint to cure for adequate time before pressure testing. Joint strength development is very rapid within the first 48 hours. Short cure periods are satisfactory for high ambient temperatures with low humidity, small pipe sizes, and interference-type fittings. Longer cure periods are necessary for low temperatures, large pipe sizes, loose fits, and relatively high humidity. See Table 71 for recommended cure times.

# INSTALLATION OF THERMOPLASTIC PIPING SYSTEMS SOLVENT CEMENTING INSTRUCTIONS FOR PVC AND CPVC PIPE AND FITTINGS 

Table 70
INITIAL SET TIMES

| TEMPERATURE RANGE DURING INITIAL SET TIME | $\begin{gathered} \hline \text { SET TIME } \\ \text { FOR PIPE } \\ \text { SIZES } \\ \text { 1/2"TO } 1 / 4 \text { " } \end{gathered}$ | $\begin{aligned} & \text { SET TIME } \\ & \text { FOR PIPE } \\ & \text { SIZES } \\ & 1 \text { 1/2"TO } 3 \text { " } \end{aligned}$ | SET TIME FOR PIPE SIZES 4"TO 8" | SET TIME FOR PIPE SIZES 10"TO 14" | SET TIME <br> FOR PIPE SIZES 16"TO 24" |
| :---: | :---: | :---: | :---: | :---: | :---: |
| $60^{\circ}$ TO $100^{\circ} \mathrm{F}$ | 15 MIN . | 30 MIN . | 1 HR . | 2 HR. | 4 HR . |
| $40^{\circ} \mathrm{TO} 59^{\circ} \mathrm{F}$ | 1 HR . | 2 HR. | 4 HR . | 8 HR. | 16 HR. |
| $0^{\circ} \mathrm{TO} 39^{\circ} \mathrm{F}$ | 3 HR . | 6 HR. | 12 HR. | 24 HR. | 48 HR. |

* In damp or humid weather allow 50\% more cure time.

The following cure schedules are suggested as guides. They are based on laboratory test data and should not be taken to be the recommendation of all cement manufacturers. Individual manufacturers' recommendations for their particular cement should be followed. These cure schedules are
based on laboratory test data obtained on net fit joints. (Net fit-in a dry fit the pipe bottoms snugly in the fitting socket without meeting interference.) If a gap joint is encountered in the system, double the following cure times.

## JOINT CURE SCHEDULE

Table 71
FOR PVC/CPVC PIPE AND FITTINGS

| RELATIVE HUMIDITY 60\% OR LESS* | $\begin{gathered} \hline \text { CURE TIME } \\ \text { FOR PIPE } \\ \text { SIZES } \\ \text { 1/2"TO } 1 \text { 1/4 } \end{gathered}$ |  | $\begin{aligned} & \hline \text { CURE TIME } \\ & \text { FOR PIPE } \\ & \text { SIZES } \\ & 1 \text { 1/2"TO } 3 " \end{aligned}$ |  | CURE TIME FOR PIPE SIZES 4"TO 8" |  | CURE TIME FOR PIPE SIZES 10"TO 14" | $\begin{aligned} & \text { CURE TIME } \\ & \text { FOR PIPE } \\ & \text { SIZES } \\ & 16 " \text { TO } 24 " \end{aligned}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| AND CURE TIME | $\begin{gathered} \text { Up To } \\ 180 \text { psi } \end{gathered}$ | Above 180 to 370 psi | Up To 180 psi | Above 180 to 315 ps | Up To 180 psi | Above 180 to 315 psi | $\begin{aligned} & \text { Up to } \\ & 180 \text { psi } \end{aligned}$ | $\begin{aligned} & \text { Up to } \\ & 100 \text { psi } \end{aligned}$ |
| $60^{\circ} \mathrm{TO} 100^{\circ} \mathrm{F}$ | 1 Hr . | 6 Hr . | 2 Hr . | 12 Hr . | 6 Hr . | 24 Hr . | 24 Hr . | 48-72 Hr. |
| $40^{\circ} \mathrm{TO} 59^{\circ} \mathrm{F}$ | 2 Hr . | 12 Hr . | 4 Hr . | 24 Hr . | 12 Hr . | 48 Hr . | 72 hrs | 5 Days |
| $0^{\circ} \mathrm{TO} 39^{\circ} \mathrm{F}$ | 8 Hr . | 48 Hr . | 16 Hr . | 96 Hr . | 48 Hr . | 8 Days | 8 Days | 10-14 Days |

## TROUBLESHOOTING AND TESTING SOLVENT CEMENT JOINTS

DO NOT TEST WITH AIR OR COMPRESSED GAS.
DO NOT TAKE SHORTCUTS. Experience has shown that shortcuts from the instructions given above are the cause of most field failures. Don't take a chance.

Solvent cemented joints correctly assembled with good cement under reasonable field conditions should never blow apart when tested, after the suggested cure period under recommended test pressures.

Good solvent cemented joints exhibit a complete dull surface on both surfaces when cut in half and pried apart. Leaky joints will show a continuous or an almost continuous series of shiny spots or channels from the bottom to the outer lip of the fitting. No bond occured at these shiny spots. The condition can increase to the point where the entire cemented area is shiny, and the fitting can blow off at this point.

Shiny areas can be attributed to one or a combination of the following causes:

1. Cementing surface not properly primed and dissolved prior to applying solvent cement.
2. Use of too small an applicator for primer or cement in comparison to pipe and fitting diameter.
3. Use of a cement which has partially or completely dried prior to bottoming the pipe into the fitting.
4. Use of jelled cement which will not bite into the pipe and fitting surface due to loss of the prime solvent.
5. Insufficient cement or cement applied only to one surface.
6. Excess gap which cannot be satisfactorily filled.
7. Excess time taken to make the joint after start of the cement application. In many of these cases, as well as condition No. 2, examination will show that it was impossible to bottom the fitting, since the lubrication effect of the cement had dissipated.
8. Cementing with pipe surfaces above $110^{\circ} \mathrm{F}$ has evaporated too much of the prime solvent.
9. Cementing with cement which has water added by one means or another, or excess humidity conditions coupled with low temperatures.
10. Joints that have been disturbed and the bond broken prior to the firm set, or readjusted for alignment after bottoming.

# INSTALLATION OF THERMOPLASTIC PIPING SYSTEMS SOLVENT CEMENTING INSTRUCTIONS FOR PVC AND CPVC PIPE AND FITTINGS 

## JOINING PLASTIC PIPE IN HOT WEATHER

There are many occasions when solvent cementing plastic pipe in $95^{\circ} \mathrm{F}$ temperatures and over cannot be avoided. If special precautions are taken, problems can be avoided. Solvent cements for plastic pipe contain high-strength solvents which evaporate faster at elevated temperatures. This is especially true when there is a hot wind blowing. If the pipe is stored in direct sunlight, surface temperatures may be $20^{\circ} \mathrm{F}$ to $30^{\circ} \mathrm{F}$ above the air temperature. Solvents attack these hot surfaces faster and deeper, especially inside the joint. Thus it is very important to avoid puddling inside the socket and to wipe off excess cement outside the joint.

By following our standard instructions and using a little extra care as outlined below, successful solvent cemented joints can be made even in the most extreme hot weather conditions.

## JOINING PLASTIC PIPE IN COLD WEATHER

Working in freezing temperatures is never easy, but sometimes the job is necessary. If that unavoidable job includes solvent cementing of plastic pipe, it can be done.

## GOOD JOINTS CAN BE MADE AT SUB-ZERO TEMPERATURES

By following our standard instructions and using a little extra care and patience, successful solvent cemented joints can be made at temperatures even as low as $-15^{\circ} \mathrm{F}$. In cold weather solvents penetrate and soften the surfaces more slowly than in warm weather. Also, the plastic is more resistant to solvent attack. Therefore, it becomes more important to presoften surfaces with primer.

Because solvents evaporate slower in cold weather, a longer cure time will be required. The cure schedule printed in Table 71 already allows a wide margin for safety. For colder weather, simply allow more cure time.

## TIPS TO FOLLOW WHEN SOLVENT CEMENTING IN HIGH TEMPERATURES:

1. Store solvent cements and primers in a cool or shaded area prior to use.
2. If possible, store fittings and pipe, or at least the ends to be solvent cemented, in a shady area before cementing.
3. Cool surfaces to be joined by wiping with a damp rag. Be sure that surface is dry prior to applying solvent cement.
4. Try to do the solvent cementing in the cooler morning hours.
5. Make sure that both surfaces to be joined are still wet with cement when putting them together. With large size pipe, more people on the crew may be necessary.
6. Use one of our heavier bodied, high viscosity cements since they will provide a little more working time.
7. Be prepared for a greater expansion-contraction factor in hot weather.

## INSTALLATION OF THERMOPLASTIC PIPING SYSTEMS SOLVENT CEMENTING INSTRUCTIONS FOR PVC AND CPVC PIPE AND FITTINGS

## TIPS TO FOLLOW IN SOLVENT CEMENTING DURING COLD WEATHER:

1. Prefabricate as much of the system as is possible in a heated working area.
2. Store cements and primers in a warmer area when not in use and make sure they remain fluid.
3. Take special care to remove moisture, including ice and snow.
4. Use extra primer to soften the joining surfaces before applying cement.
5. Allow a longer initial set and cure period before the joint is moved or the system is tested.
6. Read and follow all of our directions carefully before installation.

Regular cements are formulated to have well-balanced drying characteristics and to have good stability in sub-freezing temperatures. Some manufacturers offer special cements for cold weather because their regular cements do not have that same stability.

For all practical purposes, good solvent cemented joints can be made in very cold conditions with our existing products, providing proper care and a little common sense are used.

| PHYSICAL DATA <br> P-70 PRIMER FOR PVC AND CPVC |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: |
| BOILING POINT ( ${ }^{( } \mathrm{F}$ ) Based on 1st boiling $\begin{gathered}\text { Comp. THF. }\end{gathered}$ | $151{ }^{\circ} \mathrm{F}$ | SPECIFIC GRAVITY ( $\mathrm{H}_{2} 0=1$ ) | 0.870 | 0.010 |
| VAPOR PRESSURE ( $\underset{\text { THF Hg.) }}{\text { THF }} 25$ | 190 | PERCENT, VOLATILE BY VOLUME (\%) |  |  |
| VAPOR DENSITY (AIR = 1) APPROX. | 2.49 | EVAPORATION RATE ( $B U A C=1$ ) APPROX. |  |  |
| SOLUBILITY IN WATER 100\% |  |  |  |  |
| APPEARANCE AND ODOR - Purple Color, - Etheral Odor |  |  |  |  |
| FIRE AND EXPLOSION HAZARD DATA |  |  |  |  |
| FLASH POINT (Method used) (T.c.C.) $6^{\circ} \mathrm{F}$ | FLA | MMABLE LIMITS | $\begin{gathered} \text { Left } \\ 1.8 \end{gathered}$ | $\begin{array}{\|c} \hline \text { Used } \\ 11.8 \\ \hline \end{array}$ |
| EXTINGUISHING MEDIA <br> Dry chemical,Carbondioxide - Foam - Ansul "Purple K" National Aero-O-Foam |  |  |  |  |
| SPECIAL FIREFIGHTING PROCEDURES <br> Close or confined quarters require self contained breathing apparatus. Positive pressure hose mask or airline masks. |  |  |  |  |
| UNUSUAL FIRE AND EXPLOSION HAZARDS <br> Fire hazard because of low flash point, high volatility and heavy vapor. |  |  |  |  |


| PHYSICAL DATA |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: |
| BOILING POINT ( ${ }^{\circ}$ F) Based on 1st boiling Comp. THF. | $151{ }^{\circ} \mathrm{F}$ | SPECIFIC GRAVITY ( $\mathrm{H}_{2} \mathrm{O}=1$ ) | 0.920 | 0.02 |
| VAPOR PRESSURE (mm Hg.) THF @ $25^{\circ} \mathrm{C}$ | 190 | PERCENT, VOLATILE BY VOLUME (\%) APPROX |  | 90\% |
| VAPOR DENSITY (AIR = 1) APPROX. | 2.49 | EVAPORATION RATE (BUAC = 1) APPROX. |  |  |
| SOLUBILITY IN WATER Solvent portion PVC resin \& filler - Precipates |  |  |  |  |
| APPEARANCE AND ODOR - Clear,Thin syrupy liquid, Etheral odor |  |  |  |  |
| FIRE AND EXPLOSION HAZARD DATA |  |  |  |  |
| FLASH POINT (Method used) $\text { (T.O.C.) } 10^{\circ} \mathrm{F}$ | FLA | MMABLE LIMITS | $\begin{gathered} \text { Left } \\ 1.8 \end{gathered}$ | Used <br> 1.8 |
| EXTINGUISHING MEDIA <br> Dry chemical,Carbondioxide - Foam - Ansul "Purple K" National Aero-O-Foam |  |  |  |  |
| SPECIAL FIREFIGHTING PROCEDURES <br> Close or confined quarters require self contained breathing apparatus. Positive pressure hose mask or airline masks. |  |  |  |  |
| UNUSUAL FIRE AND EXPLOSION HAZARDS <br> Fire hazard because of low flash point, high volatility and heavy vapor. |  |  |  |  |


| 711 PRAY CEMENT FOR | SICAL | L DATA | 711 GRAY CEMENT FOR PVC |  |
| :---: | :---: | :---: | :---: | :---: |
| BOILING POINT ( ${ }^{\circ}$ F) Based on 1st boiling | $151{ }^{\circ} \mathrm{F}$ | SPECIFIC GRAVITY ( $\mathrm{H}_{2} \mathrm{O}=1$ ) | $0.958 \pm$ | 0.008 |
| VAPOR PRESSURE ( mm Hg THF @ ${ }^{\text {© }} 25^{\circ} \mathrm{C}$ | 190 | PERCENT, VOLATILE BY VOLUME (\%)APPROX. |  |  |
| VAPOR DENSITY (AIR = 1) APPROX | 2.49 | EVAPORATION RATE (BUAC = 1) APPROX. |  |  |
| SOLUBILITY IN WATER Solvent portion PVC resin \& filler - Precipates |  |  |  |  |
| APPEARANCE AND ODOR - Gary color, medium syrupy liquid - Etheral Odor |  |  |  |  |
| FIRE AND EXPLOSION HAZARD DATA |  |  |  |  |
| FLASH POINT (Method used) (T.O.C.) $8^{\circ} \mathrm{F}$ |  | FLAMMABLE LIMITS | $\begin{aligned} & \text { Left } \\ & 2.0 \end{aligned}$ | $\begin{aligned} & \text { Used } \\ & 11.8 \end{aligned}$ |
| EXTINGUISHING MEDIA <br> Dry chemical, Carbondioxide - Foam - Ansul "Purple K" National Aero-O-Foam |  |  |  |  |
| SPECIAL FIREFIGHTING PROCEDURES <br> Close or confined quarters require self contained breathing apparatus. Positive pressure hose mask or airline masks. |  |  |  |  |
| UNUSUAL FIRE AND EXPLOSION HAZARDS <br> Fire hazard because of low flash point, high volatility and heavy vapor. |  |  |  |  |
| PHYSICAL DATA <br> 719 GRAY CEMENT FOR PVC |  |  |  |  |
|  |  |  |  |  |
| BOILING POINT ( ${ }^{\circ}$ F) Based on 1st boiling Comp. THF. | $151{ }^{\circ} \mathrm{F}$ | SPECIFIC GRAVITY ( $\mathrm{H}_{2} 0=1$ ) | 0.009 | $\pm 0.004$ |
| VAPOR PRESSURE ( $\underset{\text { THF Hg.) }}{\text { © }}$ | 190 | PERCENT, VOLATILE BY VOLUME (\%) |  |  |
| VAPOR DENSITY (AIR = 1) APPROX. | 2.49 | EVAPORATION RATE (BUAC = 1) APPORX. Initial |  |  |
| SOLUBILITY IN WATER Solvent portion PVC resin \& filler - Precipates |  |  |  |  |
| APPEARANCE AND ODOR - Gray color, paste like, Etheral Odor |  |  |  |  |
| FIRE AND EXPLOSION HAZARD DATA |  |  |  |  |
| FLASH POINT (Method used) (T.C.C.) $8^{\circ} \mathrm{F}$ | flammable limits |  | Left 2 | $\begin{aligned} & \text { Used } \\ & 11.8 \end{aligned}$ |
| EXTINGUISHING MEDIA Carbondioxide, Dry chemicals |  |  |  |  |
| SPECIAL FIREFIGHTING PROCEDURES <br> Close or confined quarters require self-contained breathing apparatus. Positive pressure hose mask or airline masks. |  |  |  |  |
| UNUSUAL FIRE AND EXPLOSION HAZARDS <br> Fire hazard because of low flash point, high volatility and heavy vapor. |  |  |  |  |
| PHYSICAL DATA <br> 714 GRAY CEMENT FOR CPVC |  |  |  |  |
| BOILING POINT ( ${ }^{\circ} \mathrm{F}$ ) The lowest boiling point | $151^{\circ}$ | SPECIFIC GRAVITY ( $\mathrm{H}_{2} 0=1$ ) |  |  |
| VAPOR PRESSURE ( mm Hg T) ${ }_{\text {THF }}$ @ 25 | 190 | PERCENT, VOLATILE BY VOLUME (\%) |  |  |
| VAPOR DENSITY (AIR = 1) APPROX. | 2.49 | EVAPORATION RATE ( $B U A C=1$ ) Initially |  |  |
| SOLUBILITY IN WATER Resin precipates |  |  |  |  |
| APPEARANCE AND ODOR -Gray color, Medium syrupy liquid - Etheral Odor |  |  |  |  |
| FIRE AND EXPLOSION HAZARD DATA |  |  |  |  |
| FLASH POINT (Method used) (T.O.C.) $6^{\circ} \mathrm{F}$ | FLAMMABLE LIMITS |  | $\begin{gathered} \hline \text { Left } \\ 1.8 \% \end{gathered}$ | $\begin{gathered} \hline \text { Used } \\ 11.8 \% \end{gathered}$ |
| EXTINGUISHING MEDIA <br> Dry chemical, Carbondioxide - Foam - Ansul "Purple K" National Aero-O-Foam |  |  |  |  |
| SPECIAL FIREFIGHTING PROCEDURES <br> Close or confined quarters require self contained breathing apparatus. Positive pressure hose mask or airline masks |  |  |  |  |
| UNUSUAL FIRE AND EXPLOSION HAZARDS <br> Fire hazard because of low flash point, high volatility and heavy vapor. |  |  |  |  |

## Low VOC 724 cement for hypochlorite service

 weld-on 724 CPVC low VOC cement is a gray, medium bodied, fast-setting solvent cement used for joining CPVC industrial piping through $12^{\prime \prime}$ diameter and is specially formulated for services that include caustics and hypochlorites.THREADING INSTRUCTIONS PVC - CPVC - PP - PVDF


## SCOPE

The procedure presented herein covers threading of all IPS Schedule 80 or heavier thermoplastic pipe. The threads are National Pipe Threads (NPT) which are cut to the dimensions outlined in ANSI B2.1 and presented below:

DO NOT THREAD SCHEDULE 40 PIPE

Table 72
Threading Dimensions

| PIPE |  | THREADS |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |

## THREADING INSTRUCTIONS PVC - CPVC - PP - PVDF

## THREADING EQUIPMENT AND MATERIALS

- Pipe dies
- Pipe vise
- Threading ratchet or power machine
- Tapered plug
- Cutting lubricant (soap and water, soluble machine oil and water)
- Strap wrench
- Teflon tape
- Cutting tools
- Deburring tool


## PIPE PREPARATION

Cut pipe square and smooth and remove burrs or raised edges with a knife or file. To ensure square end cuts, a miter box, hold down or jig must be used. The pipe can be easily cut with a power or hand saw, circular or band saw. Smooth cuts are obtained by using fine-toothed cutting blades (1618 teeth per inch). A circumferential speed of about 6000 ft ./min. is suitable for circular saws, band saw speed should be approximately 3000 ft . $/ \mathrm{min}$. Pipe or tubing cutters can also be used to produce square, smooth cuts, however, the cutting wheel should be specifically designed for plastic pipe. Such a cutter is available from your local service center.

If a hold down vise is used when the pipe is cut, the jaws should be protected from scratching or gouging the pipe by inserting a rubber sheet between the vise jaws and the pipe.

## THREADING DIES

Thread-cutting dies should be clean, sharp and in good condition and should not be used to cut materials other than plastics. Dies with a $5^{\circ}$ negative front rake are recommended when using power threading equipment and dies with a $5^{\circ}$ to $10^{\circ}$ negative front rake are recommended when cutting threads by hand.

When cutting threads with power threading equipment, selfopening die heads and a slight chamfer to lead the dies will speed production.

## THREADING AND JOINING



1. Hold pipe firmly in a pipe vise. Protect the pipe at the point of grip by inserting a rubber sheet or other material between the pipe and vise.

2. A tapered plug must be inserted in the end of the pipe to be threaded. This plug provides additional support and prevents distortion of the pipe in the threaded area. Distortion of the pipe during the threading operation will result in eccentric threads, non-uniform circumferential thread depth, or gouging and tearing of the pipe wall. See Table 72 for approximate plug O.D. dimensions.
3. Use a die stock with a proper guide that is free of burrs or sharp edges, so the die will start and go on square to the pipe axis.

4. Push straight down on the handle avoiding side pressure that might distort the sides of the threads. If power threading equipment is used, the dies should not be driven at high speeds or with heavy pressure. Apply an external lubricant liberally when cutting the threads. Advance the die to the point where the thread dimensions are equal to those listed in Table 72. Do not overthread.

## THREADING INSTRUCTIONS PVC - CPVC - PP - PVDF

5. Periodically check the threads with a ring gauge to ensure that proper procedures are being followed. Thread dimensions are listed in Table 72 and the gauging tolerance is $+1-1 / 2$ turns.
6. Brush threads clean of chips and ribbons. Then starting with the second full thread and continuing over the thread length, wrap TFE (Teflon) thread tape in the direction of the threads. Overlap each wrap by one-half the width of the tape.

7. Screw the fitting onto the pipe and tighten by hand. Using a strap wrench only, further tighten the connection an additional one to two threads past hand tightness. Avoid excessive torque as this may cause thread damage or fitting damage.


TABLE 73
REINFORCING PLUG DIMENSIONS*

| NOMINAL PIPE SIZE <br> (IN.) | PLUG O.D.* |
| :---: | :---: |
| $\mathbf{1 / 2}$ | .526 |
| $\mathbf{3 / 4}$ | .722 |
| $\mathbf{1}$ | .935 |
| $\mathbf{1 - 1 / 4}$ | 1.254 |
| $\mathbf{1 - 1 / 2}$ | 1.475 |
| $\mathbf{2}$ | 1.913 |
| $\mathbf{2 - 1 / 2}$ | 2.289 |
| $\mathbf{3}$ | 2.864 |
| $\mathbf{4}$ | 3.786 |

*These dimensions are based on the median wall thickness and average outside diameter for the respective pipe sizes. Variations in wall thickness and O.D. dimensions may require alteration of the plug dimensions.

## PRESSURE TESTING

Threaded piping systems can be pressure tested up to 50\% of the pipe's hydrostatic pressure rating as soon as the last connection is made.

Caution: Air or compressed gas is not recommended and should not be used as a media for pressure testing of plastic piping systems.

Caution: Pressure ratings for threaded systems are reduced drastically. Check your application with your local service center prior to installation.

## FLANGED JOINTS

## SCOPE

Flanged joints are recommended extensively for plastic piping systems that require periodic dismantling. Flanges and flanged fittings are available in almost all materials and sizes to meet your requirements. Please consult your local service center for the availability of any flanged fitting not shown in this catalog. Flanges are normally assembled to pipe or fittings by solvent welding, threading, or thermal fusion.

Gasket seals between the flange faces should be an elastomeric, full, flat-faced gasket with a hardness of 50 to 70 durometer. Harrington Industrial Plastics can provide neoprene gaskets in the $1 / 2$ " through 24 " range having a $1 / 8$ " thickness. For chemical environments too aggressive for neoprene, other more resistant elastomers should be used.

## DIMENSIONS

Bolt circle and number of bolt holes for the flanges are the same as 150 lb . metal flanges per ANSI B16.1. Threads are tapered iron pipe size threads per ANSI B2.1. The socket dimensions conform to ASTMD 2467 which describes onehalf through 8 " sizes.

## PRESSURE RATING

Maximum pressure for any flanged system is 150 psi . At elevated temperatures the pressure capability of a flanged system must be derated as follows:

Table 74
MAXIMUM OPERATING PRESSURE (PSI)

| OPERATING <br> TEMPERATURE |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: |
| ( ${ }^{\circ}$ F) | PVC* | CPVC* | PP** $^{*}$ | PVDF |
| 100 | 150 | 150 | 150 | 150 |
| 110 | 135 | 140 | 140 | 150 |
| 120 | 110 | 130 | 130 | 150 |
| 130 | 75 | 120 | 118 | 150 |
| 140 | 50 | 110 | 105 | 150 |
| 150 | NR | 100 | 93 | 140 |
| 160 | NR | 90 | 80 | 133 |
| 170 | NR | 80 | 70 | 125 |
| 180 | NR | 70 | 50 | 115 |
| 190 | NR | 60 | NR | 106 |
| 200 | NR | 50 | NR | 97 |
| 250 | NR | NR | NR | 50 |
| 280 | NR | NR | NR | 25 |

NR- Not Recommended

* PVC and CPVC flanges sizes 2-1/2, 3 and 4-inch threaded must be back welded for the above pressure capability to be applicable.
** Threaded PP flanges size $1 / 2$ thru 4 " as well as the 6 " back weld socket flange are not recommended for pressure applications (drainage only).


## SEALING

The faces of flanges are tapered back away from the orifice area at a $1 / 2$ to 1 degree pitch so that when the bolts are tightened the faces will be pulled together generating a force in the waterway area to improve sealing.

## INSTALLATION TIPS

Once a flange is joined to pipe, the method for joining two flanges together is as follows:

1. Make sure that all the bolt holes of the matching flanges match up. It is not necessary to twist the flange and pipe to achieve this.
2. Insert all bolts.
3. Make sure that the faces of the mating flanges are not separated by excessive distance prior to bolting down the flanges.
4. The bolts on the plastic flanges should be tightened by pulling down the nuts diametrically opposite each other using a torque wrench. Complete tightening should be accomplished in stages and the final torque values in the following table should be followed for the various sizes of flanges. Uniform stress across the flange will eliminate leaky gaskets.

Table 75

| FLANGE SIZE <br> (IN.) | RECOMMENDED <br> TORQUE (FT. LBS.) |
| :---: | :---: |
| $1 / 2-1-1 / 2$ | $10-15$ |
| $2-4$ | $20-30$ |
| $6-8$ | $33-50$ |
| 10 | $53-75$ |
| 12 | $80-110$ |
| $14-24$ | 100 |

*For a well lubricated bolt.

The following tightening pattern is suggested for the flange bolts.

5. If the flange is mated to a rigid and stationary flanged object, or a metal flange, particularly in a buried situation where settling could occur with the plastic pipe, the plastic flange must be supported to eliminate potential stressing.

Note: Flange gasket and low torque gasket sets are available from Harrington Industrial Plastics.

## FIBERGLASS REINFORCED PLASTICS (FRP)

## FIBERGLASS REINFORCED PLASTICS (FRP)

FRP is a special segment of the corrosion-resistant plastics industry. By combining flexible strands of glass with various thermoset resins, a wide range of performance characteristics can be achieved. Unlike thermoplastic resins, thermoset resins do not return to a liquid state with heat.

The glass can be prepared in a variety of forms which determines the final properties of the glass resin combination. As an example, the glass can be chopped strands in a mat or felt type fabric, yarns, woven fabric, continuous strands, unidirectional or bidirectional fabrics and so on. The choices are almost infinite.

The different types of glass all have different rates of resin absorption. For the most part, every mechanical attribute is enhanced by increasing the volume of glass contained in the plastic thermoset resin. Thus, glass versus resin ratio becomes a key criteria in defining a product for a particular application.

Glass fiber and resin are described as a composite or laminate. When combining glass and resin, it is important to "wet the glass" and this is done by eliminating the trapped air which increases the glass to resin interface. The glass used for FRP is treated with silane or other similar chemistry to enhance the resin's affinity to the glass.

Selecting a specific resin will dictate the performance characteristics of the final FRP product. Chemical resistance, temperature range and mechanical properties are determined by the choice of resin and the glass.

Epoxy resins give exceptional mechanical strength and are very chemically resistant. Epoxies are used for caustics, hydrocarbons, and most organic chemicals. Several catalysts can be used in curing the epoxy resin by a crosslinking of the long polymer chain. The choice of catalyst will determine the properties of the finished FRP product. For example, an anhydride catalyst will give an epoxy product with limited chemical resistance and limited temperature capability. An aromatic amines catalyst, on the other hand, will produce a final product with broad chemical resistance and a temperature range of up to $300^{\circ} \mathrm{F}$ in certain services.

Primary disadvantages of epoxies are they require long curing times and are best cured using heat to promote complete reaction for all the epoxy sites. Epoxies are, therefore, stronger when the catalyzation is enhanced by heat.

Polyester resins are available in many forms. The two that are relevant to FRP are orthophthalic and isophthalic resins. The former is a non-corrosion resistant resin used in boats, auto bodies, and structural forms. The latter is the chemically resistant resin that is appropriate to our use in handling corrosive fluids. Isophalic polyester is the most economical of all the resin choices for FRP.

Vinylester is a coined word describing a polyester that has been modified by the addition of epoxide reactive sites. The vinylester resin has broad chemical resistance including most acids and weak bases. It is generally the choice for high purity deionized water storage in an FRP vessel.

FRP piping is available from a few major manufacturers as a standard catalog, off-the-shelf product in diameters up to 16 inches. Face to face dimensions for fittings are based on steel and the requirements of American National Standards Institute ANSI B-16.3. Not all fittings meet ANSI requirements unless specified by agreement. FRP flanges are always thicker than steel, so longer bolts are needed.

There are many fabricators who specialize in made-to-order or custom vessels, as well as special made-to-order piping. For FRP piping larger than 16 inch in diameter, it is also made to order. Large diameter FRP pipe can be custom made in sizes even larger than 12 feet.

FRP pipe products are manufactured by several techniques. Filament winding is done using continuous lengths of fiberglass yarn or tape which are wound onto a polished steel mandrel. The glass is saturated with a catalyzed resin as it is being wound onto the mandrel. This process is continued until the desired wall thickness is achieved. The resin polymerizes usually by an exothermic reaction. Depending on the angle at which the glass is applied and the tension, the mechanical properties of the finished product can be affected. Piping and vessels are produced in this manner.

Centrifugal casting involves applying glass and catalyzed resin to the inside of a rotating polished cylindrical pipe. Curing of the glass resin combination forms a finished pipe. The forces of the centrifugal rotating cylinder forces the resin to wet the glass and gives an inherent resin rich and polished outside diameter to the final product. The resin that is in excess of that required to wet the glass forms a pure resin liner. Pipe, both small and larger diameter, as well as tanks, are manufactured by this process.

Applications for FRP have grown since the introduction almost forty years ago of thermoset resins. The following is a list of some of the general advantages of FRP:

> Corrosion resistant
> Lightweight
> High strength-to-weight ratio
> Low resistance to flow
> Ease of installation
> Low cost of installation
> Very low electrical conductivity
> Excellent thermal insulation
> Long service life
> Dimensional stability

Industrial uses for FRP tanks and piping have developed in oil and gas, chemical processing, mining, nuclear, and almost every other industry you can think of.

## FIBERGLASS REINFORCED PLASTICS (FRP)

FRP piping is very amenable to the addition of specific additives to achieve certain properties. Antimony trioxide or brominated compounds, for example, can be added to provide excellent fire resistant characteristics. Specifically, designed FRP piping systems are produced for internal pressures up to 3000 PSI. Other FRP piping is used for down hole in the oil field, usually for salt water reinjection. FRP products are one of the most easily modified to meet specific needs, thus the broad range of industrial applications.

As with any piping material, good system design, proper fabrication and correct installation techniques are necessary for long and reliable service life.

Selecting the proper joining method is important for controlling installation costs and being compatible with the nature of the installation.

Butt and wrap is used to join FRP pipe by simply butting two sections of pipe together and overwrapping the joint with multiple layers of fiberglass saturated with the appropriate resin.

Threaded connections are often used for rapid and easy joining. There can be an O-ring gasket used to provide the sealing mechanism.

Bell and spigot joints are used usually with a bonding adhesive or with a gasket.

Flanges are most often used to join FRP pipe to metal or other dissimilar piping materials.

Contact molding is a process of applying fiberglass and resin to the surface of a mold that may be a variety of shapes. This process can be done by hand, spraying, or with an automated system. FRP fittings, vessels, and piping are produced by this method.

Compression molding is a process normally used to manufacture FRP fittings. A mixture of glass and resin is placed inside a mold and with heat and other molding techniques a finished part is produced.

Current standards outline the composition, performance requirements, construction method, design criteria testing and quality of workmanship. The modern standards have their origin in the U.S. Dept. of Commerce Voluntary Standard PS1549. Custom Contact Molded Reinforced Polyester Chemical Resistant Equipment. The ASTMC-582-95 takes the place of PS1569.

The following is a partial listing of ASTM standards for FRP Industrial products.

FIBERGLASS PIPE AND FITTINGS
Specification for:

| D 2997-95 | Centrifugally Cast "Fiberglass" Pipe <br> D 5421-93 <br> Contact Molded "Fiberglass" Flanges |
| :--- | :--- |
| D 5677-95 | "Fiberglass" Pipe and Pipe Fittings, <br> Adhesive Bonded Joint Type, for Aviation <br> Jet Turbine Fuel Lines <br> "Fiberglass" Pipe and Pipe Fittings, <br> D 5686-95 |
|  | Adhesive Bonded Joint Type Epoxy Resin, <br> for Condensate Return Lines |
| D 3517-91 "Fiberglass" Pressure Pipe |  |
| D 5685-95 | "Fiberglass" Pressure Pipe Fittings |
| D 2996-95 | Filament-Wound"Fiberglass" Pipe <br> D 40inforced Thermosetting Resin (RTR) <br> Flanges |

## FIBERGLASS TANKS AND EQUIPMENT Specifications for:

D 4097-95a Contact-Molded Glass-Fiber-Reinforced Thermoset Resin Chemical-Resistant Tanks
C 482-95

D 3982-92

D 3299-95a
Filament-Wound Glass-Fiber-Reinforced Thermoset Resin Chemical-Resistant Tanks

There are many special tools used for making field joints. The best policy is to follow the FRP pipe manufacturer's recommendations precisely. Most manufacturers offer the services of a factory person to train or supervise fabrication and installation.

To take maximum advantage of the many advantages of FRP in your corrosive or high purity application, contact your nearest Harrington or Corro-Flo Harrington location, or contact our Technical Services Group in Chino, California, using the number listed on the inside back cover.

## HYDRAULIC FUNDAMENTALS

PRESSURE The basic definition of pressure is force per unit area. As commonly used in hydraulics and in this catalog, it is expressed in pounds per square inch (PSI).


ATMOSPHERIC PRESSURE is the force exerted on a unit area by the weight of the atmosphere. At sea level, the atmospheric standard pressure is 14.7 pounds per square inch.
GAUGE PRESSURE Using atmospheric pressure as a zero reference, gauge pressure is a measure of the force per unit area exerted by a fluid. Units are PSIG.


ABSOLUTE PRESSURE is the total force per unit area exerted by a fluid. It equals atmospheric pressure plus gauge pressure. Units are expressed in PSIA.

OUTLET PRESSURE or discharge pressure is the average pressure at the outlet of a pump during operation, usually expressed as gauge pressure (psig).

INLET PRESSURE is the average pressure measured near the inlet port of a pump during operation. It is expressed either in units of absolute pressure (psig) preferably, or gauge pressure (psig).

DIFFERENTIAL PRESSURE is the difference between the outlet pressure and the inlet pressure. Differential pressure is sometimes called Pump Total Differential pressure.

VACUUM OR SUCTION are terms in common usage to indicate pressures in a pumping system below normal atmospheric pressure and are often measured as the difference between the measured pressure and atmospheric pressure in units of inches of mercury vacuum, etc. It is more convenient to discuss these in absolute terms; that is from a reference of absolute zero pressure in units of psia.


FLUID FUNDAMENTALS Fluids include liquids, gases, and mixtures of liquids, solids, and gases. For the purpose of this catalog, the terms fluid and liquid are used interchangeably to mean pure liquids, or liquids mixed with gases or solids which act essentially as a liquid in a pumping application.
DENSITY OR SPECIFIC WEIGHT of a fluid is its weight per unit volume, often expressed in units of pounds per cubic foot, or grams per cubic centimeter.

Example: If weight is 80 lb .; density is $80 \mathrm{lb} / \mathrm{cu}$. ft . The density of a fluid changes with temperature.
SPECIFIC GRAVITY of a fluid is the ratio of its density to the density of water. As a ratio, it has no units associated with it.

EXAMPLE: Specific gravity is 80 lb or $\mathrm{SG}=1.282$
62.4 lb .


TEMPERATURE is a measure of the internal energy level in a fluid. It is usually measured in units of degrees fahrenheit ( ${ }^{\circ} \mathrm{F}$ ) or degrees centigrade $\left({ }^{\circ} \mathrm{C}\right)$. The temperature of a fluid at the pump inlet is usually of greatest concern. See ${ }^{\circ} \mathrm{F}^{\circ}{ }^{\circ} \mathrm{C}$ conversion chart on page 96 .


VAPOR PRESSURE of a liquid is the absolute pressure (at a given temperature) at which a liquid will change to a vapor. Vapor pressure is best expressed in units of psi absolute (psia). Each liquid has its own vapor pressuretemperature relationship.


For example: If $100^{\circ} \mathrm{F}$ water is exposed to the reduced absolute pressure of .95 psia , it will boil. It will boil, even at $100^{\circ} \mathrm{F}$.

## HYDRAULIC FUNDAMENTALS

VISCOSITY-The viscosity of a fluid is a measure of its tendency to resist a shearing force. High viscosity fluids require a greater force to shear at a given rate than low viscosity fluids.
The CENTIPOISE (cps) is the most convenient unit of absolute viscosity measurement.
Other units of viscosity measurement such as the centistoke (cks) or Staybolt Second Universal (SSU) are measures of Kinematic viscosity where the specific gravity of the fluid influences the viscosity measured. Kinematic viscometers usually use the force of gravity to cause the fluid to flow down a calibrated tube while timing its flow.



The absolute viscosity, measured in units of centipoise ( $1 / 100$ of a poise) is used throughout this catalog as it is a convenient and consistent unit for calculation. Other units of viscosity can easily be converted to centipoise:
Kinematic vicsocity x Specific Gravity = Absolute Viscosity Centistokes $\quad x$ Specific Gravity $=$ Centipoise SSU x . $216 \quad$ x Specific Gravity $=$ Centipoise
See page 100 for detailed conversion charts
Viscosity unfortunately is not a constant, fixed property of a fluid, but is a property which varies with the conditions of the fluid and the system.


In a pumping system, the most important factors are the normal decrease in viscosity with temperature increase.
And the viscous behavior properties of the fluid in which the viscosity can change as shear rate or flow velocity changes.



EFFECTIVE VISCOSITY is a term describing the real effect of the viscosity of the ACTUAL fluid, at the SHEAR RATES which exist in the pump and pumping system at the design conditions.
Centrifugal pumps are generally not suitable for pumping viscous liquids. When pumping more viscous liquids instead of water, the capacity and head of the pump will be reduced and the horsepower required will be increased.
pH value for a fluid is used to define whether the aqueous solution is an acid or base (with values of pH usually between 0 and 14):

1. Acids or acidic solutions have a pH value less than 7.
2. Neutral solutions have pH value of 7 at $25^{\circ} \mathrm{C}$ (example: pH of pure water $=7$ ).
3. Bases or alkaline solutions have a pH value greater than 7.

## RELATION OF PRESSURE TO ELEVATION

In a static liquid (a body of liquid at rest) the pressure difference between any two points is in direct proportion only to the vertical distance between the points.
This pressure difference is due to the weight of the liquid and can be calculated by multiplying the vertical distance by the density (or vertical distance $x$ density of water $x$ specific gravity of the fluid). In commonly used units


P static (in PSI) - Z (in feet) x $62.4 \mathrm{lbs} . / \mathrm{cu} . \mathrm{ft} . \mathrm{x}$ SG 144 sq. in./sq. ft.

PUMP HEAD-PRESSURE-SPECIFIC GRAVITY-in a centrifugal pump the head developed (in feet) is dependent on the velocity of the liquid as it enters the impeller eye and as it leaves the impeller periphery and therefore, is independent of the specific gravity of the liquid. The pressure head developed (in psi) will be directly proportional to the specific gravity.


Pressure-Head relation of identical pumps handling liquids of differing specific gravities.


Pressure-head relation of pumps delivering same pressure handling liquids of differing specific gravity.

## HYDRAULIC FUNDAMENTALS

IMPORTANT PUMP TERMS: The term HEAD is commonly used to express the elevational equivalent of pressure allowing for specific gravity, Generally expressed in feet, head can best be defined by the following equation:

Pounds per square inch $\times 2.31=$ Head in feet Specific Gravity

The following expressions of HEAD terms are generally accepted as standards throughout the industry.

Static Head - The hydraulic pressure at a point in a fluid when the liquid is at rest.
Friction Head
Velocity Head
Pressure Head

- The loss in pressure or energy due to frictional losses in flow.
- The energy in a fluid due to its velocity, expressed as a head unit.

Discharge Head • The output pressure of a pump in operation.
Total Dynamic • The total pressure difference Head between the inlet and outlet of a pump in operation.
Suction Head • The inlet pressure of a pump when above atmospheric.
Suction Lift • The inlet pressure of a pump when below atmospheric.

## FRICTIONAL LOSSES

The nature of frictional losses in a pumping system can be very complex. Losses in the pump itself are determined by actual test and are allowed for in the manufacturers' curves and data. Similarly, manufacturers of processing equipment, heat exchangers, static mixers, etc., usually have data available for friction losses.


## CONVERSION DATA <br> TABLE 76

CONVERSION OF THERMOMETER READINGS
Degrees centigrade to degrees Fahrenheit

| ${ }^{\circ} \mathbf{C}$ | ${ }^{\circ} \mathbf{F}$ | ${ }^{\circ} \mathbf{C}$ | ${ }^{\circ} \mathbf{F}$ | ${ }^{\circ} \mathbf{C}$ | ${ }^{\circ} \mathbf{F}$ | ${ }^{\circ} \mathbf{C}$ | ${ }^{\circ} \mathbf{F}$ |
| ---: | ---: | ---: | ---: | ---: | ---: | ---: | ---: |
| -40 | -40.0 | +5 | +41.0 | +40 | +104.0 | +175 | +347 |
| -38 | -36.4 | 6 | 42.8 | 41 | 105.8 | 180 | 356 |
| -36 | -32.8 | 7 | 44.6 | 42 | 107.6 | 185 | 365 |
| -34 | -29.2 | 8 | 46.4 | 43 | 109.4 | 190 | 374 |
| -32 | -25.6 | 9 | 48.2 | 44 | 111.2 | 195 | 383 |
| -30 | 22.0 | 10 | 50.0 | 45 | 113.0 | 200 | 392 |
| -28 | 18.4 | 11 | 51.8 | 46 | 114.8 | 205 | 401 |
| -26 | 14.8 | 12 | 53.6 | 47 | 116.6 | 210 | 410 |
| -24 | 11.2 | 13 | 55.4 | 48 | 118.4 | 215 | 419 |
| -22 | 7.6 | 14 | 57.2 | 49 | 120.2 | 220 | 428 |
| -20 | -4.0 | 15 | 59.0 | 50 | 122.0 | 225 | 437 |
| -19 | -2.2 | 16 | 60.8 | 55 | 131.0 | 230 | 446 |
| -18 | -0.4 | 17 | 62.6 | 60 | 140.0 | 235 | 455 |
| -17 | +1.4 | 18 | 64.4 | 65 | 149.0 | 240 | 464 |
| -16 | 3.2 | 19 | 66.2 | 70 | 158.0 | 245 | 473 |
| -15 | 5.0 | 20 | 68.0 | 75 | 167.0 | 250 | 482 |
| -14 | 6.8 | 21 | 69.8 | 80 | 176.0 | 255 | 491 |
| -13 | 8.6 | 22 | 71.6 | 85 | 185.0 | 260 | 500 |
| -12 | 10.4 | 23 | 73.4 | 90 | 194.0 | 265 | 509 |
| -11 | 12.2 | 24 | 75.2 | 95 | 203.0 | 270 | 518 |
| -10 | 14.0 | 25 | 77.0 | 100 | 212.0 | 275 | 527 |
| -9 | 15.8 | 26 | 78.8 | 105 | 221.0 | 280 | 536 |
| -8 | 17.6 | 27 | 80.6 | 110 | 230.0 | 285 | 545 |
| -7 | 19.4 | 28 | 82.4 | 115 | 239.0 | 290 | 554 |
| -6 | 21.2 | 29 | 84.2 | 120 | 248.0 | 295 | 563 |
| -5 | 23.0 | 30 | 86.0 | 125 | 257.0 | 300 | 572 |
| -4 | 24.8 | 31 | 87.8 | 130 | 266.0 | 305 | 581 |
| -3 | 26.6 | 32 | 89.6 | 135 | 275.0 | 310 | 590 |
| -2 | 28.4 | 33 | 91.4 | 140 | 284.0 | 315 | 599 |
| -1 | 30.2 | 34 | 93.2 | 145 | 293.0 | 320 | 608 |
| 0 | 32.0 | 35 | 95.0 | 150 | 302.0 | 325 | 617 |
| +1 | 33.8 | 36 | 96.8 | 155 | 311.0 | 330 | 626 |
| 2 | 35.6 | 37 | 98.6 | 160 | 320.0 | 335 | 635 |
| 3 | 37.4 | 38 | 100.4 | 165 | 329.0 | 340 | 644 |
| 4 | 39.2 | 39 | 102.2 | 170 | 338.0 | 345 | 653 |
| -1 |  |  |  |  |  |  |  |
| -1 |  |  |  |  |  |  |  |

VOLUME
Volume of a pipe is computed by:
V= ID2x7rx Lx3
Where: $\quad V=$ volume (in cubic inches)
ID = inside diameter (in inches) $\pi=3.14159$
$\mathrm{L}=$ length of pipe (in feet)
1 U.S. Gallon .
128 fl. oz. (U.S.) 231 cu. in. $0.134 \mathrm{cu} . \mathrm{ft}$. 3.785 litres
.00379 cu. meters 0.833 Imp. gal. 0238 42-gal. barrel


WEIGHT
1 U.S. Gallon @ $50^{\circ} \mathrm{F}$. . . . . . . . . . . . . . . . 8.33 lb. x sp. gr.
1 Cubic Foot
$62.35 \mathrm{lb} . \mathrm{x} \mathrm{sp.gr}$.
7.48 gal. (U.S.)

1 Cubic Ft. of Water @ $50^{\circ} \mathrm{F}$.
62.41 lb .

1 Cubic Ft. of Water @39.2F
( $39.2^{\circ} \mathrm{F}$ is water temperature
at its greatest density).
62.43 lb .

1 Kilogram
. 2.2 lb.
1 Imperial Gallon Water 10.0 lb .

1 Pound
2 U.S. gal. -sp. gr.
016 cu. ft. sp. gr.

## CAPACITY OR FLOW

1 Gallon Per Minute (g.p.m.)
134 c.f.m. 500 lb. per hr. x sp. gr.
500 lb. Per Hour 1 g.p.m. $\div$ sp. gr.
1 Cubic Ft. Per Minute (c.f.m.) 449 g.p.h.
1 Cubic Ft. Per Second (c.f.s.) . . . . . . . . . . . . . 449 g.p.m.
1 Acre Foot Per Day . . . . . . . . . . . . . . . . . . . . 227 g.p.m.
1 Acre Inch Per Hour . . . . . . . . . . . . . . . . . . . . 454 g.p.m.
1 Cubic Meter Per Minute . . . . . . . . . . . . . . . . 264.2 g.p.m.
1,000,000 Gal. Per Day
595 g.p.m.
Brake H.P. = (g.p.m. ) (Total Head in Ft.) (Specific Gravity)
(3960) (Pump Eff.)

## FOR SERVICE, PLEASE CALL 1-800-877-HIPCO

## CONVERSION DATA

TABLE 77

| TO CHANGE | T0 | MULTIPLY BY |
| :---: | :---: | :---: |
| Atmospheres | PSI (Pounds per Sq. Inch) | 14.696 |
| Atmospheres | Feet of Water | 33.9 |
| Atmospheres | Inches of Mercury | 29.92 |
| Barrels (U.S.L.q.) | Gallons (U.S.) | 31.5 |
| Barrels of Oil | Gallons (U.S.) | 42 |
| B.T.U. | H.P.Lr | . 0003929 |
| Centimeters | Feet | . 0328 |
| Centimeters | Inches | . 3937 |
| Centimeters/Sec. | Feet/Min. | 1.9684 |
| Centimeters/Sec. | Feet/Sec. | . 0328 |
| Centipoise | Poises | . 01 |
| Centistokes | Stokes | . 01 |
| Cubic Centimeters | Cubic Feet | $3.5314 \times 10^{-5}$ |
| Cubic Centimeters | Cubic Inches | . 06102 |
| Cubic Centimeters | Gallons (L.Q.) | . 0002642 |
| Cubic Feet | Gallons | 7.4805 |
| Cubic Feet | Cubic Inches | 1728. |
| Cubic Feet | Cubic Yards | . 03703 |
| Cubic Feet/Min. | G.P.M. | 7.4805 |
| Cubic Inches | Gallons | . 004329 |
| Cubic Inches | Cubic Centimeters | 16.387 |
| Cubic Inches | Cubic Feet | . 0005787 |
| Cubic Meters | Gallons (Liq) | 264.17 |
| Cubic Meters | Cubic Feet | 35.31 |
| Cubic Meters | Cubic Inches | 61,023.74 |
| Cubic Meters/Hr. | G.P.M. | 4.403 |
| Cubic Yards | Cubic Feet | 27 |
| Degrees | Revolution | . 00277778 |
| Dynes | Pounds | $2.248009 \times 10^{-6}$ |
| Dynes/Sq. Cm. | PSI | $1.45038 \times 10^{-5}$ |
| Fathom | Feet | 6 |
| Feet | Centimeters | 30.48006 |
| Feet | Meters | . 3048006 |
| Feet | Inches | 12 |
| Feet | Yards | . 3333 |
| Feet of Water | Atmosphere | . 02949 |
| Feet of Water | PSI | . 433 |
| Feet of Water | Inches of Mercury | . 88265 |
| Feet of Water | Pounds per Sq. Ft. | 62.5 |
| Feet/Hr. | Miles/Hour | . 00018939 |
| Feet/Min. | Meters/Min. | . 3048 |
| Feet/Min. | Miles/Hour | . 01136 |
| Feet/Sec. | Miles/Hour | . 681818 |
| Gallons | Cubic Centimeters | 3,785.43 |


| TO CHANGE | T0 | MULTIPLY BY |
| :---: | :---: | :---: |
| Gallons | Gallons (Imp.) | . 83268 |
| Gallons | Cubic Feet | . 13368 |
| Gallons | Cubic Inches | 231 |
| Gallons | Pound of Water | 8.33 |
| Gallons/Min. | Cubic Feet/Min. | . 13368 |
| Horsepower | Ft. Lbs./Min. | 33,000 |
| Horsepower | Ft. Lbs./Sec. | 550 |
| Inches | Feet | . 083333 |
| Inches | Meters | . 0254 |
| Inches | Millimeters | 25.40005 |
| Inches | Mils | 1000 |
| Inches of Mercury | Atmosphere | . 033327 |
| Inches of Mercury | Feet of Water | 1.1309 |
| Inches of Mercury | PSI | . 489 |
| Inches of Mercury | Inches of Water | 13.6 |
| Inches of Water | Inches of Mercury | . 0735 |
| Inches of Water | Pounds per Sq. In. | . 0361 |
| Inches of Water | Ounces per Sq. In. | . 578 |
| Inches of Water | Pounds per Sq. Ft. | 5.2 |
| Kilograms | Pounds (avdp.) | 2.2046 |
| Kilograms/Sq. Cm. | PSI | 14.2233 |
| Kilograms/Sq. mm. | PSI | 1422.33 |
| Liters | Gallons | . 264178 |
| Long Tons | Pounds | 2240 |
| Meters | Feet | 3.2808 |
| Meters | Inches | 39.37 |
| Ounces | Pounds | . 0625 |
| Ounces per Sq. In. | Inches of Mercury | . 127 |
| Ounces per Sq. In. | Inches of Water | 1.733 |
| Poise | Centipoise | 100 |
| Pounds | Ounces | 16 |
| Pounds per Sq. In. | Inches of Water | 27.72 |
| Pounds per Sq. In. | Feet of Water | 2.31 |
| Pounds per Sq. In. | Inches of Mercury | 2.04179 |
| Pounds per Sq. In. | Atmospheres | . 06804 |
| Pounds of Water | Gallon | . 12004 |
| Square Feet | Square Inches | 144 |
| Square Feet | Square Yards | . 11111 |
| Square Inches | Square Centimeters | 6.4516 |
| Square Inches | Square Feet | 006944 |
| Square Inches | Square Millimeters | 645.163 |
| Square Millimeters | Square Inches | . 0015499 |
| Square Yards | Square Feet | 9 |
| Tons Molasses/Hr. | G.P.M. | 2.78 |

## CONVERSION DATA

| Inches | Millimeters |  |  |
| :--- | :---: | :--- | :--- |
| 0 | 0.0000 | Convert 3.7643 meters to |  |
| $1 / 128$ | 0.1984 | feet, inches and fractions |  |
| $1 / 64$ | 0.3969 | 3.7643 meters |  |
| $3 / 128$ | 0.5953 | $\underline{3.6556}$ | $=12 \mathrm{ft}$. |
| $1 / 32$ | 0.7937 | 108.70 | mm |
| $5 / 128$ | 0.9921 | $\underline{107.95}$ | $=41 / 4 \mathrm{in}$. |
| $3 / 64$ | 1.1906 | 3.75 | $=\underline{1 / 32^{\prime \prime}}$ |
| $7 / 128$ | 1.3890 | 3.7643 meters $=\underline{12^{\prime}-4-9 / 32^{\prime \prime}}$ |  |

Convert $15^{\prime}-6-7 / 16^{\prime \prime}$ to meters
$15^{\prime}=4.5720$ meters
$6.7 / 16^{\prime \prime}=.163513$ meters
$15^{\prime}-6-7 / 16^{\prime \prime}=4.735513$ meters

## EQUIVALENT OF COMMON FRACTIONS OF AN INCH

| FRACTION | DECIMALS | MILLIMETERS | FRACTION | DECIMALS | MILLIMETERS |
| :---: | :---: | :---: | :---: | :---: | :---: |
| 1/64 | -. 015625 | -0.397 | 33/64 | -. 515625 | -13.097 |
| 1/32 | . 03125 | -0.794 | 17/32 | -. 53125 | -13.494 |
| 3/64 | -. 046875 | -1.191 | 35/64 | -. 546875 | -13.891 |
| 1/16 | -. 0625 | -1.588 | 9/16 | -. 5625 | -14.288 |
| 5/64 | -. 078125 | -1.984 | 37/64 | -. 578125 | -14.684 |
| 3/32 | -. 09375 | -2.381 | 19/32 | -. 59375 | -15.081 |
| 7/64 | -. 109375 | -2.778 | 39/64 | -. 609375 | -15.478 |
| 1/8 | -. 1250 | -3.175 | 5/8 | -. 625 | -15.875 |
| 9/64 | -. 140625 | -3.572 | 41/64 | -. 640625 | -16.272 |
| 5/32 | -. 15625 | -3.969 | 21/32 | -. 65625 | -16.669 |
| 11/64 | -. 171875 | -4.366 | 43/64 | -. 671875 | -17.066 |
| 3/16 | -. 1875 | -4.762 | 11/16 | -. 6875 | -17.462 |
| 13/64 | -. 203125 | -5.159 | 45/64 | -. 703125 | -17.859 |
| 7/32 | -. 21875 | -5.556 | 23/32 | -. 71875 | -18.256 |
| 15/64 | -. 234375 | -5.953 | 47/64 | -. 734375 | -18.653 |
| 1/4 | -. 25 | -6.350 | 3/4 | -. 7500 | -19.050 |
| 17/64 | -. 265625 | -6.747 | 49/64 | -. 765625 | -19.447 |
| 9/32 | -. 28125 | -7.144 | 25/32 | -. 78125 | -19.844 |
| 19/64 | -. 296875 | -7.541 | 51/64 | -. 796875 | -20.241 |
| 5/16 | -. 3125 | -7.938 | 13/16 | -. 8125 | -20.638 |
| 21/64 | -. 328125 | -8.334 | 53/64 | -. 828125 | -21.034 |
| 11/32 | -. 34375 | -8.731 | 27/32 | -. 84375 | -21.431 |
| 23/64 | -. 359375 | -9.128 | 55/64 | -. 859375 | -21.828 |
| 3/8 | -. 3750 | -9.525 | 7/8 | -. 8750 | -22.225 |
| 25/64 | -. 390625 | -9.922 | 57/64 | -. 890625 | -22.622 |
| 13/32 | -. 40625 | -10.319 | 29/32 | -. 90625 | -23.019 |
| 27/64 | -. 421875 | -10.716 | 59/64 | -. 921875 | -23.416 |
| 7/16 | -. 4375 | -11.112 | 15/16 | -. 9375 | -23.812 |
| 29/64 | -. 453125 | -11.509 | 61/64 | -. 953125 | -24.209 |
| 15/32 | -. 46875 | -11.906 | 31/32 | -. 96875 | -24.606 |
| 31/64 | -. 484375 | -12.303 | 63/63 | -. 984375 | -25.003 |
| 1/2 | -. 5 | -12.700 | 1 | -1.0 | -25.400 |

## TABLES 79, 80, \& 81

WATER PRESSURE TO FEET HEAD

| POUNDS <br> PER <br> SQUARE INCH | FEET <br> HEAD | POUNDS <br> PER <br> SQUARE INCH | FEET <br> HEAD |
| :---: | :---: | :---: | :---: |
| 1 | 2.31 | 100 | 230.90 |
| 2 | 4.62 | 110 | 253.98 |
| 3 | 6.93 | 120 | 277.07 |
| 4 | 9.24 | 130 | 300.16 |
| 5 | 11.54 | 140 | 323.25 |
| 6 | 13.85 | 150 | 346.34 |
| 7 | 16.16 | 160 | 369.43 |
| 8 | 18.47 | 170 | 392.52 |
| 9 | 20.78 | 180 | 415.61 |
| 10 | 23.09 | 200 | 461.78 |
| 15 | 34.63 | 250 | 577.24 |
| 20 | 46.18 | 300 | 692.69 |
| 25 | 57.72 | 350 | 808.13 |
| 30 | 69.27 | 400 | 922.58 |
| 40 | 92.36 | 500 | 1154.48 |
| 50 | 115.45 | 600 | 1385.39 |
| 60 | 138.54 | 700 | 1616.30 |
| 70 | 161.63 | 800 | 1847.20 |
| 80 | 184.72 | 900 | 2078.10 |
| 90 | 207.81 | 1000 | 2309.00 |

NOTE: One pound of pressure per square inch of water equals 2.31 feet of water at $60^{\circ} \mathrm{F}$. Therefore, to find the feet head of water for any pressure not given in the table above, multiply the pressure pounds per square inch by 2.31 .

FEET HEAD OF WATER TO PSI

| FEET <br> HEAD | POUNDS <br> PER <br> SQUARE INCH | FEET <br> HEAD | POUNDS <br> PER <br> SQUARE INCH |
| :---: | :---: | :---: | :---: |
| $\mathbf{1}$ | .43 | 100 | 43.31 |
| 2 | .87 | 110 | 47.64 |
| 3 | 1.30 | 120 | 51.97 |
| 4 | 1.73 | 130 | 56.30 |
| 5 | 2.17 | 140 | 60.63 |
| 6 | 2.60 | 150 | 64.96 |
| 7 | 3.03 | 160 | 69.29 |
| 8 | 3.46 | 170 | 73.63 |
| 9 | 3.90 | 180 | 77.96 |
| 10 | 4.33 | 200 | 86.62 |
| 15 | 6.50 | 250 | 108.27 |
| 20 | 8.66 | 300 | 129.93 |
| 25 | 10.83 | 350 | 151.58 |
| 30 | 12.99 | 400 | 173.24 |
| 40 | 17.32 | 500 | 216.55 |
| 50 | 21.65 | 600 | 259.85 |
| 60 | 25.99 | 700 | 303.16 |
| 70 | 30.32 | 800 | 346.47 |
| 80 | 34.65 | 900 | 389.78 |
| 90 | 38.98 | 1000 | 433.00 |

NOTE: One foot of water at $60^{\circ} \mathrm{F}$ equals .433 pounds pressure per square inch. To find the pressure per square inch for any feet head not given in the table above, multiply the feet head by .433 .

## EQUIVALENTS OF PRESSURE AND HEAD

| TO OBTAIN MULTIPLY BY | lb./in. ${ }^{2}$ | lb. $/ 7 \mathrm{t}^{2}$ | Atmospheres | kg/cm ${ }^{2}$ | kg/m ${ }^{2}$ |  |  | in. Mercury $\left(32^{\circ} \mathrm{F}\right)^{\star *}$ (32 $\left.{ }^{\circ} \mathrm{F}\right)^{*}$ | mm Mercury $\left(32^{\circ} \mathrm{F}\right)^{* *}$ | Bar | $\begin{array}{\|c\|} \hline \text { Megapascal } \\ \text { (MPa)"** } \end{array}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Ib. $/ \mathrm{in} .{ }^{2}$ | 1 | 144 | . 068046 | . 070307 | 703.070 | 27.7276 | 2.3106 | 2.03602 | 51.7150 | 0.06895 | . 006895 |
| lb./ft. ${ }^{2}$ | . 0069445 | 1 | . 000473 | . 000488 | 4.88241 | . 1926 | . 01605 | . 014139 | . 35913 | . 000479 | . 0000479 |
| Atmospheres | 14.696 | 2116.22 | 1 | 1.0332 | 10332.27 | 407.484 | 33.9570 | 29.921 | 760 | 1.01325 | . 101325 |
| kg/cm ${ }^{2}$ | 14.2233 | 2048.155 | . 96784 | 1 | 10000 | 394.38 | 32.8650 | 28.959 | 735.559 | . 98067 | . 098067 |
| $\mathrm{kg} / \mathrm{m}^{2}$ | . 001422 | . 204768 | . 0000968 | . 0001 | 1 | . 03944 | . 003287 | . 002896 | . 073556 | 000098 | . 0000098 |
| in. Water* | . 036092 | 5.1972 | . 002454 | . 00253 | 25.375 | 1 | . 08333 | . 073430 | 1.8651 | . 00249 | . 000249 |
| ft. Water* | . 432781 | 62.3205 | . 029449 | . 03043 | 304.275 | 12 | 1 | . 88115 | 22.3813 | . 029839 | . 0029839 |
| in. Mercury** | . 491154 | 70.7262 | . 033421 | . 03453 | . 345.316 | 13.6185 | 1.1349 | 1 | 25.40005 | 033864 | . 0033864 |
| mm Mercury** | . 0193368 | 2.78450 | . 0013158 | . 0013595 | 13.59509 | . 53616 | . 044680 | . 03937 | 1 | . 001333 | . 0001333 |
| Bar*** | 14.5038 | 2088.55 | . 98692 | 1.01972 | 10197.2 | 402.156 | 33.5130 | 29.5300 | 750.062 | 1 | . 10 |
| MPa*** | 145.038 | 20885.5 | 9.8692 | 10.1972 | 101972 | 4021.56 | 335.130 | 295.300 | 7500.62 | 10 | 1 |

$$
\text { * Water at } \left.68^{\circ} \mathrm{F}\left(20^{\circ} \mathrm{C}\right) \quad * * \text { Mercury at } 32^{\circ} \mathrm{F}\left(0^{\circ} \mathrm{C}\right) \quad * * * 1 \mathrm{MPa}(\text { Megapascal })=10 \mathrm{Bar}=1,000 \mathrm{~N} / \mathrm{m}^{2}\right)
$$

To convert from one set of units to another, locate the given unit in the left hand column, and multiply the numerical value by the factor shown horizontally to the right, under the set of units desired.

## CONVERSION DATA

## TABLES 82 \& 83

Poise = c.g.s. unit of absolute viscosity
Stoke = c.g.s. unit of kinematic viscosity
Centipoise $=0.01$ poise
Centistoke $=0.01$ stoke
Centipoises = centistokes $x$ density (at temperature under consideration)
Reyn ( 1 lb. sec. per sq. in.) $=69 \times 105$ centipoises

## VISCOSITY CONVERSION

| SAYBOLT <br> UNIVERSAL <br> SSU | STOKES | CENTISTOKES | POISES* | CENTIPOISES* | ( | ENGLER <br> SECONDS | REDWOOD <br> NO. 1 <br> SECONDS |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 31 | .010 | 1.00 | .008 | .8 | TYPICAL <br> LIQUIDS <br> AT 70 |  |  |
| 35 | .025 | 2.56 | .020 | 2.05 | 54 | 29 | WATER |
| 50 | .074 | 7.40 | .059 | 5.92 | 89 | 32.1 | KEROSENE |
| 80 | .157 | 15.7 | .126 | 12.6 | 125 | 69.2 | NO. 4FUEL OIL |
| 100 | .202 | 20.2 | .162 | 16.2 | 150 | 85.6 | TRANSFORMER OIL |
| 200 | .432 | 43.2 | .346 | 34.6 | 295 | 170 | HYDRAULICOIL |
| 300 | .654 | 65.4 | .522 | 52.2 | 470 | 254 | SAE 10W OIL |
| 500 | 1.10 | 110 | .88 | 88.0 | 760 | 423 | SAE 10 OIL |
| 1,000 | 2.16 | 220 | 1.73 | 173 | 1,500 | 896 | SAE 20 OIL |
| 2,000 | 4.40 | 440 | 3.52 | 352 | 3,000 | 1,690 | SAE 30 OIL |
| 5,000 | 10.8 | 1,080 | 8.80 | 880 | 7,500 | 4,230 | SAE 50 OIL |
| 10,000 | 21.6 | 2,160 | 17.0 | 1,760 | 15,000 | 8,460 | SAE 60-70 OIL |
| 50,000 | 108 | 10,800 | 88 | 8,800 | 75,000 | 43,660 | MOLASSES B |
| 100,000 | 216 | 21,600 | 173 | 17,300 | 150,000 | 88,160 | MOLASSESC |

Kinematic Viscosity (in centistokes) $=$

## Absolute Viscosity (in centipoise) Density

## REYNOLDS NUMBER, R.

Reynolds Number, R. is a dimensionless number or ratio of velocity in ft. per sec. times the internal diameter of the pipe in feet times the density in slugs per cu.ft. divided by the absolute viscosity in lb. sec. per sq. ft.
This is equivalent to $R=V D / V$ (VD divided by the kinematic viscosity). Reynolds Number is of great significance because

$$
\mathrm{R}=\frac{\mathrm{VD}}{\mathrm{~V}}
$$

it determines the type of flow, either laminar or turbulent, which will occur in any pipe line, the only exception being a critical zone roughly between an $R$ of 2000 to 3500 . Within this zone it is recommended that problems be solved by assuming that turbulent flow is likely to occur. Computation using this assumption gives the greatest value of friction loss and hence the result is on the safe side.
For those who prefer the greater precision of an algebraic equation, Reynolds Number for a pipe line may also be computed from the following formula:

## PUMPING VISCOUS LIQUIDS WITH

## CENTRIFUGAL PUMPS

Centrifugal pumps are generally not suitable for pumping viscous liquids. However, liquids with viscosities up to 2000 SSU can be handled with Centrifugal pumps. The volume and pressure of the pump will be reduced according to the following table.

Percent reduction in flow and head and percent increase in power when pumping viscous liquid instead of water are shown in the table below.

| VISCOSITY <br> SSU | $\mathbf{3 0}$ | $\mathbf{1 0 0}$ | $\mathbf{2 5 0}$ | $\mathbf{5 0 0}$ | $\mathbf{7 5 0}$ | $\mathbf{1 0 0 0}$ | $\mathbf{1 5 0 0}$ | $\mathbf{2 0 0 0}$ |
| :--- | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Flow Reduction <br> GPM \% | - | 3 | 8 | 14 | 19 | 23 | 30 | 40 |
| Head Reduction <br> Feet \% | - | 2 | 5 | 11 | 14 | 18 | 23 | 30 |
| Horsepower <br> increase \% | - | 10 | 20 | 30 | 50 | 65 | 85 | 100 |

$$
\mathrm{R}=\frac{\mathrm{Q}}{29.4 \mathrm{dv}}
$$

where $Q$ is in GPM, $d$ is inside diameter of pipe in inches, and $V$ is kinematic viscosity in $\mathrm{ft}^{2} / \mathrm{sec}$.

## FOR SERVICE, PLEASE CALL 1-800-877-HIPCO

## CONVERSION DATA BAUME

UNITED STATES STANDARD BAUME SCALES
RELATION BETWEEN BAUME DEGREES AND SPECIFIC GRAVITY
LIQUIDS HEAVIER THAN WATER
Formula $-\mathrm{sp} \mathrm{gr}=\frac{145}{145-^{\circ} \text { Baume }}$

## TABLE 84

| BAUME <br> DEGREES | SP GR <br> $60^{\circ}-60^{\circ}$ | BAUME <br> DEGREES | SP GR <br> $60^{\circ}-60^{\circ}$ | BAUME <br> DEGREES | SP GR <br> $60^{\circ}-60^{\circ}$ | BAUME <br> DEGREES | SP GR <br> $60^{\circ}-60^{\circ}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 0 | 1.00000 | 20 | 1.16000 | 40 | 1.38095 | 60 | 1.70588 |
| 1 | 1.00694 | 21 | 1.16935 | 41 | 1.39423 | 61 | 1.72619 |
| 2 | 1.01399 | 22 | 1.17886 | 42 | 1.40777 | 62 | 1.74699 |
| 3 | 1.02113 | 23 | 1.18852 | 43 | 1.42157 | 63 | 1.76829 |
| 4 | 1.02837 | 24 | 1.19835 | 44 | 1.43564 | 64 | 1.79012 |
| 5 | 1.03571 | 25 | 1.20833 | 45 | 1.45000 | 65 | 1.81250 |
| 6 | 1.04317 | 26 | 1.21849 | 46 | 1.46465 | 66 | 1.83544 |
| 7 | 1.05072 | 27 | 1.22881 | 47 | 1.47959 | 67 | 1.85897 |
| 8 | 1.05839 | 28 | 1.23932 | 48 | 1.49485 | 68 | 1.88312 |
| 9 | 1.06618 | 29 | 1.25000 | 49 | 1.51042 | 69 | 1.90789 |
| 10 | 1.07407 | 30 | 1.26087 | 50 | 1.52632 | 70 | 1.93333 |
| 11 | 1.08209 | 31 | 1.27193 | 51 | 1.54255 | 71 | 1.95946 |
| 12 | 1.09023 | 32 | 1.28319 | 52 | 1.55914 | 72 | 1.98630 |
| 13 | 1.09848 | 33 | 1.29464 | 53 | 1.57609 | 73 | 2.01389 |
| 14 | 1.10687 | 34 | 1.30631 | 54 | 1.59341 | 74 | 2.04225 |
| 15 | 1.11538 | 35 | 1.31818 | 55 | 1.61111 | 75 | 2.07143 |
| 16 | 1.12403 | 36 | 1.33028 | 56 | 1.62921 | 76 | 2.10145 |
| 17 | 1.13281 | 37 | 1.34259 | 57 | 1.64773 | 77 | 2.13235 |
| 18 | 1.14173 | 38 | 1.35514 | 58 | 1.66667 | 78 | 2.16418 |
| 19 | 1.15079 | 39 | 1.36792 | 59 | 1.68605 | 79 | 2.19697 |

LIQUIDS LIGHTER THAN WATER Formula- $\mathrm{sp} \mathrm{gr}=\frac{140}{130+{ }^{\circ} \mathrm{Baume}}$

| 10 | 1.00000 | 30 | .87500 | 50 | .77778 | 70 | .70000 |
| :--- | :--- | :--- | :--- | :--- | :--- | :--- | :--- |
| 11 | .99291 | 31 | .86957 | 51 | .77348 | 71 | .69652 |
| 12 | .98592 | 32 | .86420 | 52 | .76923 | 72 | .69307 |
| 13 | .97902 | 33 | .85890 | 53 | .76503 | 73 | .68966 |
| 14 | .97222 | 34 | .85366 | 54 | .76087 | 74 | .68627 |
| 15 | .96552 | 35 | .84848 | 55 | .75676 | 75 | .68293 |
| 16 | .95890 | 36 | .84337 | 56 | .75269 | 76 | .67961 |
| 17 | .95238 | 37 | .83832 | 57 | .74866 | 77 | .67633 |
| 18 | .94595 | 38 | .83333 | 58 | .74468 | 78 | .67308 |
| 19 | .93960 | 39 | .82840 | 59 | .74074 | 79 | .66986 |
| 20 | .93333 | 40 | .82353 | 60 | .73684 | 80 | .66667 |
| 21 | .92715 | 41 | .81871 | 61 | .73298 | 81 | .66351 |
| 22 | .92105 | 42 | .81395 | 62 | .72917 | 82 | .66038 |
| 23 | .91503 | 43 | .80925 | 63 | .72539 | 83 | .65728 |
| 24 | .90909 | 44 | .80460 | 64 | .72165 | 84 | .65421 |
| 25 | .90323 | 45 | .80000 | 65 | .71795 | 85 | .65117 |
| 26 | .89744 | 46 | .79545 | 66 | .71428 | 86 | .64815 |
| 27 | .89172 | 47 | .79096 | 67 | .71066 | 87 | .64516 |
| 28 | .88608 | 48 | .78652 | 68 | .70707 | 88 | .64220 |
| 29 | .88050 | 49 | .78212 | 69 | .70352 | 89 | .63927 |

From Circular No. 59 Bureau of Standards.

## RELATIVE SIZE OF PARTICLES

| US AND ASTM STD. SIEVENO. | ACTUAL OPENING |  | US AND ASTM STD. SIEVE NO. | ACTUAL OPENING |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
|  | INCHES | MICRONS |  | INCHES | MICRONS |
| 10 | . 0787 | 2000 | 170 | . 0035 | 88 |
| 12 | . 0661 | 1680 | 200 | . 0029 | 74 |
| 14 | . 0555 | 1410 |  | . 0026 | 65 |
| 16 | . 0469 | 1190 | 230 | . 0024 | 62 |
| 18 | . 0394 | 1000 | 270 | . 0021 | 53 |
| 20 | . 0331 | 840 |  | . 0020 | 50 |
| 25 | . 0280 | 710 | 325 | . 0017 | 44 |
| 30 | . 0232 | 590 |  | . 0016 | 40 |
| 35 | . 0197 | 500 | 400 | . 00142 | 36 |
| 40 | . 0165 | 420 |  | . 00118 | 30 |
| 45 | . 0138 | 350 | 550 | . 00099 | 25 |
| 50 | . 0117 | 297 | 625 | . 00079 | 20 |
| 60 | . 0098 | 250 |  | . 00059 | 15 |
| 70 | . 0083 | 210 | 1,250 | . 000394 | 10 |
| 80 | . 0070 | 177 | 1,750 | . 000315 | 8 |
| 100 | . 0059 | 149 | 2,500 | . 000197 | 5 |
| 120 | . 0049 | 125 | 5,000 | . 000099 | 2.5 |
| 140 | . 0041 | 105 | 12,000 | . 0000394 |  |

## PUMP SIZING GUIDELINES

The following worksheet is designed to take you step-by-step through the process of selecting the proper pump for most common applications. There are three major decisions to make when choosing the right pump. They are size, type and best buy for the particular application. Each factor must be weighed carefully and a final selection refined through the process of elimination. The following worksheet will help eliminate many common oversights in design selection. This is a combination of many manufacturers specification request, so it may be photocopied and used by any applications engineer.
I. Sketch the layout of the proposed installation. Trying to pick a pump without a sketch of the system is like a miner trying to work without his lamp. You are in the dark from start to finish. When drawing the system, show the piping, fittings, valves and/or other equipment that may affect the system. Mark the lengths of pipe runs. Include all elevation changes.
II. Determine and study what is to be pumped. All of the following criteria will affect the pump selection in terms of materials of construction and basic design.
What is the material to be pumped and its concentration? Is it corrosive? $\qquad$ yes $\qquad$ no $\qquad$ pH value.
Specific Gravity or pounds per gallon $\qquad$ Temperature: Min. $\qquad$ Max. $\qquad$ degrees $C$. or $F$. Viscosity at temperature(s) given above $\qquad$ in Centipoise or $\qquad$ Seconds Saybolt Universal. Is the material abrasive $\qquad$ yes $\qquad$ no. If so, what is the percentage of solid in solution $\qquad$ and their size range $\qquad$ Min. $\qquad$ Max.
Capacity required (constant or variable) $\qquad$ U.S. Gallons per minute (gpm) $\qquad$ ,
U.S. Gallon per hour (gph) $\qquad$ ,U.S. Gallons per day (gpd) $\qquad$ ,Cubic Centimeters per day (ccpd) $\qquad$ _.

## PUMP SIZING GUIDELINES

## (continued)

III. Calculating the total pressure requirements.

## The Inlet side of the pump

1. What is the material of the inlet piping $\qquad$ and size ?
(a) What is the total length of the inlet piping, in feet?
(b) Fittings Qty. Equivalent length (See page 58)
$\qquad$
2. Total length ( $a+b$ above) for calculating friction loss
3. Friction loss per 100 foot of pipe (See pages 50-58)
$\qquad$ -
4. Total inlet friction loss (use answer from \#2 above multiplied by answer in \#3 above, then divide the product by 100)
5. Static suction lift (See important terms under Hydraulic Fundamentals, pages 93-95)
6. Static suction head
7. Total inlet head $=(\overline{4+5-6}$ from above $)$ $\mathrm{NPSH}_{\mathrm{A}}$ (Net Positive Suction Head, available) has been calculated to be $\qquad$ .

## The Discharge side of the pump

8. What is the material of the discharge piping $\qquad$ and the size $\qquad$ ?
(c) What is the total length of the discharge piping, in feet?
(d) Fittings Qty. Equivalent length (See page 58)
$\qquad$
9. Total length ( $\mathrm{c}+\mathrm{d}$ above) for calculating friction loss
10. Friction loss per 100 foot of pipe (See pages 50 to 58 ) $=$ $\qquad$
11. Total discharge friction loss (Use answer from \#9 above multiplied by answer in \#10 above then divide the product by 100)
12. Static discharge head (See sketch) Total elevation difference between centerline of the pumps inlet and the point of discharge.
13. Add any additional pressure requirements on the system: ie, filters, nozzles or equipment. $\qquad$ PSI
14. Total Discharge Head $=(11+12+13$ from above $)$
15. Total System Head $=(7+12+13)$ $\qquad$ in feet.
16. Total Static Head $=(5-6+12+13)$ in feet.
17. Total Friction Loss $=(4+11)$ $\qquad$ in feet.

## IV. Service Cycle

How many hours per day will this pump operate? $\qquad$ How many days per week will it be used? $\qquad$
V. Construction Features

Is a sanitary pump design required? $\qquad$ yes $\qquad$ no.
Will the pump be required to work against a closed discharge? $\qquad$ yes $\qquad$ no.
Is it possible for this pumping system to run dry? $\qquad$ yes $\qquad$ no. Is a water-jacketed seal required to prevent crystallization on the seal faces? no. Can the pump be totally isolated, drained, and flushed? yes $\qquad$
Does this application and environment require a chemically resistant epoxy coating? $\qquad$ no
VI. Drive Requirements

AC $\qquad$ or DC $\qquad$ Motor, Voltage $\qquad$ Cycle (Hz) $\qquad$ Phase $\qquad$
Motor enclosure design $\qquad$ Open, $\qquad$ Totally Enclosed, $\qquad$ Explosion Proof, $\qquad$ Sanitary,
Pneumatic (Air Motor) Plant air pressure available $\qquad$ psig. Volume of air available $\qquad$
VII. What accessories will be required? Foot Valve $\qquad$ , Suction Strainer $\qquad$ ,
Check Valves ,Isolation Valves $\qquad$ Pressure Relief Valve $\qquad$ ,
Pressure Gauges $\qquad$ Flow indicators $\qquad$ , Filter/Lubricator/Regulator $\qquad$ .

## GLOSSARY OF PIPING TERMS

## ABRASION RESISTANCE:

Ability to withstand the effects of repeated wearing, rubbing, scraping, etc.

## ACCEPTANCE TEST:

An investigation performed on an individual lot of a previously qualified product, by, or under the observation of, the purchaser to establish conformity with a purchase agreement.

## ACRYLIC RESINS:

A class of thermoplastic resins produced by polymerization of acrylic acid derivatives.

## ACRYLONITRILE - BUTADIENE • STYRENE (ABS):

Plastics containing polymers and/or blends of polymers, in which the minimum butadiene content is 6 percent, the minimum styrene and/ or substituted styrene content is 15 percent, and the maximum content of all other monomers is not more than 5 percent, and lubricants, stabilizers and colorants.

## ADHESIVE:

A substance capable of holding materials together by surface attachment.

## AGING:

The effect of time on materials.

## ALKYD RESINS:

A class of thermosetting resins produced by condensation of a polybased acid or anhydride and a polyhydric alcohol.

## ANNEAL:

To prevent the formation of or remove stresses in plastic parts by controlled cooling from a suitable elevated temperature.

## BELL END:

The enlarged portion of a pipe that resembles the socket portion of a fitting and that is intended to be used to make a joint by inserting a piece of pipe into it. Joining may be accomplished by solvent cements, adhesives, or mechanical techniques.

## BEAM LOADING:

The application of a load to a pipe between two points of support, usually expressed in pounds and the distance between the centers of the supports.

BLISTER:
Undesirable rounded elevation of the surface of a plastic, whose boundaries may be either more or less sharply defined, somewhat resembling in shape a blister on the human skin. A blister may burst and become flattened.

## BOND:

To attach by means of an adhesive.

## BURNED:

Showing evidence of thermal decomposition through some discoloration, distortion, or destruction of the surface of the plastic.

## BURST STRENGTH:

The internal pressure required to break a pipe or fitting. This pressure will vary with the rate of build-up of the pressure and the time during which the pressure is held.

## BUTYLENE PLASTICS:

Plastics based on resins made by the polymerization of butane or copolymerization of butene with one or more unsaturated compounds, the butene being in greatest amount of weight.

## CELLULOSE:

Chemically a carbohydrate, which is the chief component of the solid structure of plants, wood, cotton, linen, etc. The source of the cellulosic family of plastics.

## CELLULOSE ACETATE BUTYRATE:

A class of resins made from a cellulose base. Either cotton tinters or purified wood pulp, by the action of acetic anhydride, acetic acid, and butyric acid.

## CEMENT:

A dispersion of solutions of a plastic in a volatile solvent. This meaning is peculiar to the plastics and rubber industries and may or may not be an adhesive composition.

CHEMICAL RESISTANCE:
(1) The effect of specific chemicals on the properties of plastic piping with respect to concentration, temperature, and time of exposure. (2) The ability of a specific plastic pipe to render service for a useful period in the transport of a specific chemical at a specified concentration and temperature.

## COALESCENCE:

The union or fusing together of fluid globules or particles to form larger drops or a continuous mass.

## COLD FLOW:

Change in dimensions or shape of some materials when subjected to external weight or pressure at room temperature.

## COMPOUND:

A combination of ingredients before being processed or made into a finished product. Sometimes used as a synonym for material formulation.

## COMPRESSIVE STRENGTH:

The crushing load at failure applied to a specimen per unit area of the resistance surface of the specimen.

## CONDENSATION:

A chemical reaction in which two or more molecules combine with the separation of water. Also, the collection of water droplets from vapor onto a cold surface.

## COPOLYMER:

The product of simultaneous polymerization of two or more polymerizeable chemicals known as monomers.

## CRAZING:

Fine cracks at or under the surface of a plastic.

## CREEP:

The unit elongation of a particular dimension under load for a specific time following the initial elastic elongation caused by load application. It is expressed usually in inches per inch per unit of time.

## CURE:

To change the properties of a polymeric system into a final, more stable, usable condition by the use of heat, radiation or reaction with chemical additives.

## DEFLECTION TEMPERATURE:

The temperature at which a specimen will deflect a given distance at a given load under prescribed conditions of test. See ASTM D648. Formerly called heat distortion.

## DEGRADATION:

A deleterious change in the physical properties of a plastic evidenced by impairment of these properties.

## GLOSSARY OF PIPING TERMS

## DIELECTRIC CONSTANT:

A value that serves as an index of the ability of a substance to resist the transmission of an electrostatic force from one charged body to another, as in a condenser. The lower the value, the greater the resistance. The standard apparatus utilizes a vacuum, whose dielectric constant is 1 ; in reference to the various materials interposed between the charged terminals have the following values at $20^{\circ} \mathrm{C}$ : air, 1.00058; glass, 3; benzene, 2.3; acetic aced, 6.2; ammonia, 15.5; ethyl alcohol, 25: glycerol, 56; and counts for its unique behavior as a solvent and in electrolytic solutions. Most hydrocarbons have high resistance (low conductivity). Dielectric constant values decrease as the temperature rises.

## DIFFUSION:

The migration or wandering of the particles or molecules of a body of fluid matter away from the main body through a medium or into another medium.

## DIMENSION RATIO:

The diameter of a pipe divided by the wall thickness. Each pipe can have two dimension ratios depending upon whether the outside or inside diameter is used. In practice, the outside diameter is used if the standards requirement and manufacturing control are based on this diameter. The inside diameter is used when this measurement is the controlling one.

DRY-BLEND:
A free-flowing compound prepared without fluxing or addition of solvent.

## DUROMETER:

Trade name of the Shore Instrument Company for an instrument that measures hardness. The Durometer determines the "hardness of rubber or plastics by measuring the depth of penetration (without puncturing) of a blunt needle compressed on the surface for a short period of time.

## ELASTICITY:

That property of plastics materials by virtue of which they tend to recover their original size and like properties.

## ELONGATION:

The capacity to take deformation before failure in tension. Expressed as a percentage of the original length.

## EMULSION:

A dispersion of one liquid in another, possible only when they are mutually insoluble.

## ENVIRONMENTAL STRESS CRACKING:

Cracks that develop when the material is subjected to stress in the presence of specific chemicals.

## ESTER:

A compound formed by the reaction between an alcohol and an acid. Many esters are liquids. They are frequently used as plasticizers in rubber and plastic compounds.

## EXTRUSION:

Method of processing plastic in a continuous or extended form by forcing heat-softened plastic through an opening shaped like the cross-section of the finished product. This is the method used to produce thermoplastic (PVC) pipe.

FABRICATE:
Method of forming a plastic into a finished article by machining drawing, cementing, and similar operations.

## FIBER STRESS:

The unit stress, usually in pounds per square inch (psi) in a piece of material that is subjected to an external load.

## FILLER:

A relatively inert material added to a plastic to modify its strength, permanence, working properties or other qualities or to lower costs.

## FLAMMABILITY:

The time a specimen will support a flame after having been exposed to a flame for a given period.

## FLEXURAL STRENGTH:

The pressure in pounds necessary to break a given sample when applied to the center of the sample which has been supported at its end.

## FORMULATION:

A combination of ingredients before being processed or made into a finished product. Sometimes used as a synonym for material or compound.

## FORMING:

A process in which the shape of plastic pieces such as sheets, rods, or tubes is changed to a desired configuration.

## FUSE:

To join two plastic parts by softening the material through heat or solvents.

## GENERIC:

Common names for types of plastic material. They may be either chemical terms or coined names. They contrast with trademarks which are the property of one company.

## GRAVES TEAR STRENGTH:

The force required to rupture a specimen by pulling a prepared notched sample.

## HARDNESS:

A comparative gauge of resistance to indentation.

## HEAT DISTORTION:

The temperature at which a specimen will deflect a given distance at a given load.

## HEAT JOINING:

Making a piper joint by heating the edges of the parts to be joined so that they fuse and become essentially one piece with or without the addition of additional material.

## HEAT RESISTANCE:

The ability to withstand the effects of exposure to high temperature. Care must be exercised in defining precisely what is meant when this term is used. Descriptions pertaining to heat resistance properties include boilable, washable, cigarette-proof, sterilizable, etc.

## HOOP STRESS:

The tensile stress, usually in pounds per square inch (psi) in the circumferential orientation in the wall of the pipe when the pipe contains a gas or liquid under pressure.

## HYDROSTATIC DESIGN STRESS:

The estimated maximum tensile stress in the wall of the pipe in the circumferential orientation due to internal hydrostatic pressure that can be applied continuously with a high degree of certainty that failure of the pipe will not occur.

## GLOSSARY OF PIPING TERMS

## HYDROSTATIC STRENGTH (quick):

The hoop stress calculated by means of the ISO equation at which the pipe breaks due to an internal pressure build-up, usually within 60 to 90 seconds.

## IMPACT STRENGTH:

Resistance or mechanical energy absorbed by a plastic part to such shocks as dropping and hard blows.

## INJECTION MOLDING:

Method of forming a plastic to the desired shape by forcing heat-softened plastic into a relatively cool cavity where it rapidly solidifies (freezes).

## ISO EQUATION:

An equation showing the interrelations between stress, pressure, and dimensions in pipe, namely

$$
\frac{S P(I D+t) \text { or } P(O D)-t)}{2 t}
$$

where $\quad S=$ stress
$\mathrm{P}=$ pressure
ID = average inside diameter
OD = average outside diameter
$t=$ minimum wall thickness

JOINT:
The location at which two pieces of pipe or a pipe and a fitting are connected together. The joint may be made by an adhesive, a solvent cement, or a mechanical device such as threads or a ring seal.

## KETONES:

Compounds containing the carbonyl group (CO) to which is attached two alkyl groups. Ketones, such as methyl ethyl ketone, are commonly used as solvents for resins and plastics.

## LIGHT STABILITY:

Ability of a plastic to retain its original color and physical properties upon exposure to sun or artificial light.

## LONGITUDINAL STRESS:

The stress imposed on the long axis of any shape. It can be either a compressive or tensile stress.

## LONG-TERM HYDROSTATIC STRENGTH:

The estimated tensile stress in the wall of the pipe in the circumferential orientation (hoop stress) that when applied continuously will cause failure of the pipe at 100,000 hours (11.43 years). These strengths are usually obtained by extrapolation of log-log regression equations or plots.

## LUBRICANTS:

A substance used to decrease the friction between solid faces sometimes used to improve processing characteristics of plastic compositions.

## MODULUS:

The load in pounds per square inch (or kilos per square centimeter) of initial cross-sectional area necessary to produce a stated percentage elongation which is used in the physical description of plastics (stiffness).

## MODULUS OF ELASTICITY:

The ratio of the stress per square inch to the elongation per inch due to this stress.

## MOLDING, COMPRESSION:

A method of forming objects from plastics by placing the material in a confining mold cavity and applying pressure and usually heat.

## MONOMER:

The simplest repeating structural unit of a polymer. For additional polymers this presents the original unpolymerized compound.

## OLEFIN PLASTICS:

Plastics based on resins made by the polymerization of olefins or copolymerization of olefins with other unsaturated compounds, the olefins being in greatest amount by weight. Polyethylene, polypropylene, and polybutylene are the most common olefin plastics encountered in pipe.

## ORANGE PEEL:

Uneven surface somewhat resembling an orange peel.

## ORGANIC CHEMICAL:

Originally applied to chemicals derived from living organisms, as distinguished from "inorganic" chemicals found in minerals and inanimate substances; modern chemists define organic chemicals more exactly as those which contain the element carbon.

## PHENOL RESINS:

Resins made by reaction of a phenolic compound or tar acid with an aldehyde; more commonly applied to thermosetting resins made from pure phenol and formaldehyde.

## PLASTIC:

A material that contains as an essential ingredient an organic substance of large molecular weight is solid in its finished state, and at some state in its manufacture or in its processing into finished articles, can be shaped by flow.

## PLASTICITY:

A property of plastics and resins which allows the material to be deformed continuously and permanently without rupture upon the application of a force that exceeds the yield value of the material.

## PLASTIC CONDUIT:

Plastic pipe or tubing used as an enclosure for electrical wiring.

## PLASTIC PIPE:

A hollow cylinder of a plastic material in which the wall thickness is usually small when compared to the diameter and in which the inside and outside walls are essentially concentric.

## PLASTIC TUBING:

A particular size of plastics pipe in which the outside diameter is essentially the same as that of copper tubing.

## POLYBUTYLENE:

A polymer prepared by the polymerization of butene-1 as the sole monomer.

POLYETHYLENE:
A polymer prepared by the polymerization of ethylene as the sole monomer.

## POLYMER:

A product resulting from a chemical change involving the successive addition of a large number of relatively small molecules (monomer) to form the polymer and whose molecular weight is usually a multiple of that of the original substance.

## POLYMERIZATION:

Chemical change resulting in the formation of a new compound whose molecular weight is usually a large multiple of that of the original substance.

## GLOSSARY OF PIPING TERMS

## POLYPROPYLENE:

A polymer prepared by the polymerization of propylene as the sole monomer.

## POLYSTYRENE:

A plastic based on a resin made by polymerization of styrene as the sole monomer.

## POLYVINYL CHLORIDE:

Polymerized vinyl chloride, a synthetic resin which, when plasticized or softened with other chemicals, has some rubber like properties. It is derived from acetylene and hydrochloric acid.

## PRESSURE:

When expressed with reference to pipe the force per unit area exerted by the medium in the pipe.

## STABILIZER:

A chemical substance which is frequently added to plastic compounds to inhibit undesirable changes in the material, such as discoloration due to heat or light.

## STIFFNESS FACTOR:

A physical property of plastic pipe that indicates the degree of flexibility of the pipe when subjected to external loads.

## STRAIN:

The ratio of the amount of deformation to the length being deformed caused by the application of a load on a piece of material.

## STRENGTH:

The mechanical properties of a plastic such as a load or weight carrying ability, and ability to withstand sharp blows. Strength properties include tensile, flexural, and tear strength, toughness, flexibility, etc.

## STRESS:

When expressed with reference to pipe, the force per unit area in the wall of the pipe in the circumferential orientation due to internal hydrostatic pressure.

## STRESS CRACK:

External or internal cracks in a plastic caused by tensile stresses less than that of its short-time mechanical strength.

## STRESS RELAXATION:

The decrease of stress with respect to time in a piece of plastic that is subject to an external load.

## STYRENE PLASTICS:

Plastics based on resins made by the polymerization of styrene or copolymerization of styrene with other unsaturated compounds, the styrene being in greatest amount by weight.

## STYRENE-RUBBER-PLASTICS:

Compositions based on rubbers and styrene plastics, the styrene plastics being in greatest amount by weight.

## SUSTAINED PRESSURE TEST:

A constant internal pressure test for 1000 hours.

## TEAR STRENGTH:

Resistance of a material to tearing.

## TENSILE STRENGTH:

The capacity of a material to resist a force tending to stretch it. Ordinarily the term is used to denote the force required to stretch a material to rupture, and is known variously as "breaking point," "breaking stress," "ultimate tensile strength," and sometimes erroneously as "breaking strain." In plastics testing, it is the load in pounds per square inch or kilos per square centimeter of original cross-sectional area, supported at the moment of rupture by a piece of test sample on being elongated.

## THERMOFORMING:

Forming with the aid of heat.

## THERMAL CONDUCTIVITY:

Capacity of a plastic material to conduct heat.

## THERMAL EXPANSION:

The increase in length of a dimension under the influence of an increase in temperature.

## THERMOPLASTIC:

In a plastic which is thermoplastic in behavior, adj. capable of being repeatedly softened by increase of temperature and hardened by decrease of temperature.

## THERMOSETTING:

Plastic materials which undergo a chemical change and harden permanently when heated in processing. Further heating will not soften these materials.

## TRANSLUCENT:

Permitting the passage of light, but diffusing it so that objects beyond cannot be clearly distinguished.

## TURBULENCE:

Any deviation from parallel flow in a pipe due to rough inner walls, obstructions, or direction changes.

## VINYL PLASTICS:

Plastics based on resins made from vinyl monomers, except those specifically covered by other classification, such as acrylic and styrene plastics. Typical vinyl plastics are polyvinyl chloride, or polyvinyl monomers with unsaturated compounds.

## VIRGIN MATERIAL:

A plastic material in the form of pellets, granules, powder, floc or liquid that has not been subjected to use or processing other than that required for its original manufacture.

## VISCOSITY:

Internal friction of a liquid because of its resistance to shear, agitation or flow.

## VOLATILE:

Property of liquids to pass away by evaporation.

## WATER ABSORPTION:

The percentages by weight or water absorbed by a sample immersed in water. Dependent upon area exposed and time of exposure.

## WELDING:

The joining of two or more pieces of plastic by fusion of the material in the pieces at adjoining or nearby areas either with or without the addition of plastic from another source.

## YIELD STRENGTH:

The stress at which a plastic material exhibits a specified limiting permanent set.

## YIELD POINT:

The point at which a plastic material will continue to elongate at no substantial increase in load during a short test period.

## YIELD STRESS:

The stress at which a plastic material elongates without further increase of stress. Up to this point, the stress/strain relationship is linear (Young's Modules).


[^0]:    Harrington's corporate office in Chino, CA

[^1]:    -- = Data not available at printing; $\mathrm{N} / \mathrm{R}=\mathrm{Not}$ Recommended; $\mathrm{N} / \mathrm{A}=$ Not Available (not manufactured)

    * Threaded Polypropylene is not recommended for pressure applications and Fuseal drainage systems are not pressure rated.
    **For threaded joints properly backwelded.
    NOTE: The pressure ratings in this chart are based on water and are for pipe and fittings only. Systems that include valves, flanges, or other weaker items will require derating the entire system.

